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) 347-3611
) 310-4995

Señora Jefe de la
DIVISION DE NUEVAS CREACIONES
Superintendencia de Industria y Comercio
E. S. D.

TRÁMITE : 002

EVENTO : 001

ACTUACIÓN : 538

Referencia : Expediente No. 00-052.353

Asunto : Solicitud de patente para: **LECHADAS Y
COMPOSICIONES ALMACENABLES PARA CEMENTAR
POZOS DE PETROLEO Y GAS**

Solicitante : **PETROLEO BRASILEIRO S.A. PETROBRAS**

Fecha de solicitud : 12 de julio de 2000

Publicada en la : Gaceta No. 516 del 30 de Mayo de 2002

1. Yo, Emilio FERRERO, identificado como aparece al pie de mi firma, actuando como apoderado en el asunto de la referencia, atentamente, solicito se efectúe el examen de patentabilidad de la solicitud en referencia según lo establecido en el artículo 44 de la Decisión 486 de la Comisión de la Comunidad Andina. Para tal efecto presento junto con este escrito el recibo No. 02-78,525 por valor de \$318.000.00, que corresponde a la tasa fijada según lo dispuesto en la resolución No. 44691 del 31 de diciembre de 2001.

2. Ruego atentamente a la Señora Jefe se sirva ordenar que se anexe este recibo, para que se efectúe dicho examen y se continúe con el trámite de la solicitud.

Bogotá, 29 NOV 2000
Señora Jefe,


EMILIO FERRERO
T.P.A. No. 31.929

COLO 00795 801 015 4
MRE/JFR/ID-000305/WPCL0795



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Industria y Comercio

SUPERINTENDENCIA

NIT : 000170007-2

Superintendencia de Industria y Comercio
Activación y Concesión de Marcas
Fecha: 2002-11-29 17:17:52
Tramite: 1 QUE PATE-NEG 1 1 PLAZA-NEG 019 PAT-NEG
Dependencia: SUB-DIVISION DE NUEVAS CREACIONES

RECIBO OFICIAL DE CASH : 02 - 70,525
FECHA : NOVIEMBRE 15 DE 2002

***** DONATION *****

DEPOSITANTE	TIPO PAGO	BANCO	CUENTA	Nº. PAGO	FECHA PGO	VAL. PAGO
CANELIER ABOGADOS	DONATION	BANCO POPULAR	050-00110-6	3133962	25/11/2002	20,104,000.00

***** D O N C E T O *****

CANT. CONTABILITICO	CONCEPTO	TOTAL CONCEPTO
1 50005-01-01 SOLICITUDES	112 PTC CAP-I EXAMEN DE PATENTIBILIDA	310,000.00
	TOTAL :	310,000.00

CON: TRESCIENTOS DIEZ Y CINCO MIL PESOS

RESPONSABLE : 

RECIBO DE CASH APLICADO AL EXPEDIENTE N°.

Colo 00795-801-015-4

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Bogotá, D.C., Colombia

SUPERINTENDENCIA DE INDUSTRIA Y COMERCIO
DIVISIÓN DE NUEVAS CREACIONES

2005-06-16
375

2020

Bogotá, D. C., 10 de Junio de 2005

Doctor

EMILIO FERRERO

Representante **PETROLEO BRASILEIRO S.A. - PETROBRAS**

ASUNTO	Radicación No.	00-52353
	Trámite	002
	Evento	001
	Actuación	430
	Oficio	
	Folios	024

10607

Como resultado del examen de fondo, realizado con fundamento en el artículo 45 de la Decisión 486 de la Comisión de la Comunidad Andina, se le comunica

1) Documentos estudiados:

- a) Para el presente estudio se tendrán en cuenta el capítulo descriptivo, comprendido en los folios 108 a 142 de la solicitud en estudio.
- b) Para el presente estudio se tendrá en cuenta el capítulo reivindicatorio que comprende 23 reivindicaciones en los folios 143 a 149 de la solicitud en estudio.
- c) Conforme lo establece los artículos 9, 10 y 11 de la decisión 486 de la Comisión de la Comunidad Andina, la presente solicitud en estudio fue presentada el 12 de julio de 2000, y en el momento de la radicación **SI** se reclamo prioridad de la primera solicitud presentada en Brasil BRPI9902726-7.

2) Objeto de la invención

- a) Las reivindicaciones 1 a 23 de la solicitud en estudio se refieren a composiciones "almacenables" (sic) para cementación de pozos de petróleo y gas que contienen escoria de alto horno como material hidráulico, activadores, aditivos y una fase acuosa continua que forma una lechada de cementación, en donde la cantidad de activadores en dichas composiciones con base en la cantidad de escoria es insuficiente para efectuar el fraguado de la composición durante por lo menos 72 horas
- b) El anterior producto y su procedimiento de fabricación buscan mejores formulas de cementar pozos de petróleo y gas.
- c) Según la Clasificación Internacional de Patentes, la codificación para esta solicitud corresponde a C 04 B 07/14

3) Claridad de la Solicitud

- a) El artículo 30 de la Decisión 486 de la Comisión de la Comunidad Andina establece que

"Las reivindicaciones definirán la materia que se desea proteger mediante la patente. Deben ser claras y concisas y estar enteramente sustentadas por la descripción. Las reivindicaciones podrán ser independientes o dependientes. Una reivindicación será independiente cuando defina la materia que se desea proteger sin referencia a otra reivindicación anterior. Una reivindicación será dependiente cuando defina la materia que se desea proteger refiriéndose a una reivindicación anterior. Una reivindicación será dependiente cuando defina la materia que se desea proteger refiriéndose a una reivindicación anterior.- Una reivindicación que se refiera a dos o más reivindicaciones anteriores se considerará reivindicación dependiente múltiple."

El capítulo reivindicatorio no es claro toda vez que:

- i) No se precisa la materia sobre la cual se solicita protección. Cómo se explicará en el punto 4), la presente solicitud no posee unidad de invención, por lo que no está definida la materia sobre la cual se solicita protección.
- ii) La reivindicación 22 se encuentra mal redactada. El solicitante describe un proceso pero la encabeza como un producto. El solicitante debería comenzar la reivindicación como "proceso para fabricar composiciones para cementación de pozos de petróleo y gas como las de las reivindicaciones *** caracterizado porque se preparan..."
- iii) La reivindicación 23 debe eliminarse. Aquí el solicitante quiere caracterizar el mismo objetivo a lograr. De acuerdo a lo contemplado en toda la solicitud, se quiere proteger unas composiciones que sirven para la cementación de pozos de petróleo o gas. Por tanto, no puede caracterizar como nuevo el mismo objetivo a lograr. Debe eliminarse dicha reivindicación.

De acuerdo a lo anterior, el capítulo reivindicatorio no cumple con el requisito de claridad de acuerdo a lo establecido en el Art. 30 de la Decisión 486.

4) Evaluación de la Unidad de Invención

El artículo 25 de la Decisión 486 de la Comisión de la Comunidad Andina establece

"La solicitud de patente sólo podrá comprender una invención o un grupo de invenciones relacionadas entre sí, de manera que conformen un único concepto inventivo"

La presente solicitud carece de unidad de invención toda vez que configura **TRES** diferentes objetos. Aunque se dirigen a **COMPOSICIONES PARA**

CEMENTACIÓN DE POZOS la definición de la materia que caracteriza a cada una de las reivindicaciones independientes 1, 3, y 5 es muy diferente entre sí. Esto permite afirmar que no se trata del mismo producto. Todo el problema radica en configurar varias reivindicaciones independientes con materia diferente. El solicitante debe establecer una sola reivindicación independiente dirigida al **producto** en la forma más simple de la solicitud de invención. Partiendo de allí establecer reivindicaciones dependientes que amplíen esa forma más simple hasta su forma más compleja.

De acuerdo a lo anterior, la presente solicitud no cumple con el requisito de unidad de invención de acuerdo al Art. 25 de la Decisión 486.

5) Determinación del Estado de la Técnica

El artículo 16 de la Decisión 486 de la Comisión establece:

“El estado de la técnica comprenderá todo lo que haya sido accesible al público por una descripción escrita u oral, utilización, comercialización o cualquier otro medio antes de la fecha de presentación de la solicitud de patente o, en su caso, de la prioridad reconocida.”

“Sólo para el efecto de la determinación de la novedad, también se considerará dentro del estado de la técnica, el contenido de una solicitud de patente en trámite ante la oficina nacional competente cuya fecha de presentación o de prioridad fuese anterior a la fecha de presentación o de prioridad de la solicitud de patente que se estuviese examinando, siempre que dicho contenido este incluido en la solicitud de fecha anterior cuando ella se publique o hubiese transcurrido el plazo previsto en el artículo 40.”

Consultadas las bases de datos y los archivos con que cuenta la entidad, especialmente bajo las clasificaciones **C 04 B 28/08** y las más cercanas a ellas, se encontró que antes del 13 de julio de 1999 (fecha para determinar el estado de la técnica) habían sido publicados los documentos que se enumeran en la siguiente tabla los cuales se relacionan con composiciones para cementación de pozos.

De acuerdo con lo establecido en el artículo 16 se determinó el estado de la técnica y se encontró el siguiente antecedente:

Nº	Documento	Título	Fecha de Publicación
D1	US 5547506	Storable liquid cementitious slurries for cementing oil and gas wells	20.08.1996
D2	US 5409064	Optimizing blast furnace slag cements	25.04.1995
D3	US 5058679	Solidification of water based muds	22.10.1991

6) Evaluación de los requisitos de patentabilidad

El artículo 14 de la Decisión 486 de la Comisión de la Comunidad Andina establece:

“Los Países Miembros otorgarán patentes para las invenciones, sean de producto o procedimiento, en todos los campos de la tecnología, siempre que sean nuevas tengan nivel inventivo y sean susceptibles de aplicación industrial”.

En cumplimiento con este artículo, se procedió a evaluar los requisitos de novedad, nivel inventivo y aplicación industrial con el fin de establecer la patentabilidad de la invención reivindicada en la solicitud en estudio.

a) Evaluación del Nivel Inventivo

El art. 18 de la Decisión 486 de la Comisión de la Comunidad Andina establece:

“Se considerará que una invención tiene nivel inventivo, si para una persona del oficio normalmente versada en el arte en la materia técnica correspondiente, esa invención no hubiese resultado obvia ni se hubiese derivado de manera evidente del estado de la técnica”.

Los documentos D1 (US 5547506), D2 (US 5409064) y D3 (US5058679) muestran composiciones muy similares a las esbozadas por la presente solicitud. Nótese en D1 las columnas 3 y 5 especialmente. En D2 las tablas, ejemplos y en general toda la solicitud. En D3 las tablas 6 y 8. Para un técnico sería obvio llegar a lo encontrado en la presente solicitud partiendo de uno cualquiera de los documentos anteriores o de combinaciones de dos de ellos.

b) Resumen

En conclusión los requisitos de patentabilidad de la presente solicitud se podrían ver afectados así:

Nº	Documento	Reivindicaciones afectadas	Requisito que afecta
D1	US 5547506	1 - 23	Nivel inventivo
D2	US 5409064	1 - 23	Nivel inventivo
D3	US 5058679	1 - 23	Nivel inventivo

7) Notificación

En cumplimiento del artículo 45 de la Decisión 486 de la Comisión de la Comunidad Andina, se le indica que dentro del término de sesenta días contados a partir de la fecha de la notificación de la presente comunicación debe responder a la notificación. En caso de no dar respuesta al presente requerimiento, o si a pesar de la respuesta subsistieran los impedimentos para la concesión, se denegará la patente.

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Notifíquese el presente oficio conforme a lo dispuesto por el numeral 5.2, literal e) del capítulo quinto del título primero de la Circular Única N° 10 de 2001

ALIX CARMENZA CÉSPEDES DE VERGEL
Jefe División de Nuevas Creaciones

El anterior requerimiento fue notificado por fijación en la lista, de fecha

16 de 2001

Concepto Técnico N°	EXAMINADOR TÉCNICO Código No.	EXAMINADOR JURÍDICO Código No.
835	202003	



US005547506A

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United States Patent [19]
Rae et al.

[11] **Patent Number:** **5,547,506**
[45] **Date of Patent:** **Aug. 20, 1996**

[54] **STORABLE LIQUID CEMENTITIOUS
SLURRIES FOR CEMENTING OIL AND GAS
WELLS**

[75] **Inventors:** **Philip Rae, Aberdeen; Neil Johnston,**
Westhill, both of Scotland

[73] **Assignee:** **BJ Services Company, Tomball, Tex.**

[21] **Appl. No.:** **447,002**

[22] **Filed:** **May 22, 1995**

Related U.S. Application Data

[62] **Division of Ser. No. 186,719, Jan. 25, 1994, Pat. No.**
5,447,197.

[51] **Int. Cl.⁶** **C04B 24/00**

[52] **U.S. Cl.** **106/730; 106/714; 106/719;**
106/724; 106/728; 106/726; 106/790; 106/803;
106/805; 106/809; 106/810; 106/DIG. 4;
166/285; 166/292; 166/293

[58] **Field of Search** **106/714, 724,**
106/729, 730, 789, 790, 802, 804, 805,
809, 810, 718, 720, 803, 823, 285, 292,
293, DIG. 4, 719, 803, 726, 728

[56] **References Cited**

U.S. PATENT DOCUMENTS

3,955,992 5/1976 Roberts 106/730

4,043,827 8/1977 Bennett 106/730
4,188,231 2/1980 Valore 106/823
4,230,502 10/1980 Lustig et al. 106/823
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5,314,022 5/1994 Cowen et al. 166/293
5,340,397 8/1994 Brothers 106/823
5,379,840 1/1995 Cowen et al. 106/789

Primary Examiner—Karl Group

Assistant Examiner—Michael Marcheschi

Attorney, Agent, or Firm—Arnold, White & Durkee

[57]

ABSTRACT

In the method of the invention, a storable hydraulically-active cementitious slurry is made and used to cement within subterranean foundations for oil and gas wells. The slurry is made from hydraulically-active, cementitious material suitable for oil field purposes and can be stored until needed. During storage, the slurry remains liquid. The slurry is activated when needed for cementing. After pumping the activated slurry into the wellbore, the set cement has properties acceptable for well cementing.

17 Claims, No Drawings

STORABLE LIQUID CEMENTITIOUS SLURRIES FOR CEMENTING OIL AND GAS WELLS

This application is a division of application Ser. No. 08/186,719, filed Jan. 25, 1994, U.S. Pat. No. 5,447,197.

BACKGROUND OF THE INVENTION

1. Field of the Invention

The present invention relates to storable cementitious slurries used for oil and gas well cementing, as well as a method of cementing an oil or gas well using the storable slurry.

2. Description of the Prior Art

Hydraulic cements are cements that set and develop compressive strength due to a hydration reaction, not drying. Thus, hydraulic cements can set under water. This setting property serves a variety of purposes. Hydraulic cements are often used for cementing pipes or casings within a well bore of a subterranean formation for the construction of oil, gas and water wells, as well as other purposes, such as squeeze cementing. In the oil and gas industry, successful cementing of well pipe and casing during oil and gas well completion requires cement slurries having several important properties. The cement slurry must have a pumpable viscosity, fluid loss control, minimized settling of particles and the ability to set within a practical time.

In a typical completion operation, the cement slurry is pumped down the inside of the pipe or casing and back up the outside of the pipe or casing through the annular space. This seals the subterranean zones in the formation and supports the casing. The amount of water used in forming the cement slurry depends upon the type of hydraulic cement selected and the job conditions at hand. The amount of water used can vary over a wide range, depending upon such factors as the required consistency of the slurry and upon the strength requirement for a particular job.

Conventional mixing equipment is relatively complex and expensive. The equipment must wet dry cement powder, homogenize the mix, measure its density and, if necessary, recirculate it, such that additional solids or mixwater can be added to achieve the desired density. These varied requirements dictate the equipment's configuration and complexity.

Bulk equipment is usually pressurized so that solids can be transferred pneumatically at the relatively high rates required. Once at the drilling site, the pneumatically conveyed cementing solids must be correctly proportioned and mixed with the water, as well as other additives to form a pumpable slurry. The slurry must then be tested for the appropriate density, with the density adjusted to fall within the appropriate range. If cementing solids are not correctly proportioned, the quality of the cement diminishes.

Because conventional cementing slurries set quickly, they cannot be made in advance of their use. Thus, conventional cementing slurries for cementing well bores cannot be made in advance, such as during the drilling operation. A delay in the drilling operation delays the cementing job. If personnel and equipment for cementing idly wait onsite until the drilling ends, a delay can increase the cost of the cementing job. A slurry made in advance and stored until needed would allow the personnel and equipment to make the storable slurry, regardless of whether drilling had ceased.

One object of the invention is to provide a liquid, storable, cementitious slurry that remains liquid over an extended

period of time but can be activated at the time of use to meet specific job requirements.

Another object of the invention is to provide a storable cement slurry that can be made at a different location from the job site. This storable slurry can then be transported to the job site before cementing.

Another object of the invention is to provide a storable cement slurry that can be stored in nonpressurized tanks and easily transferred. In addition, the mixing equipment used on the job site need only homogenize the slurry with any additional water and additives as required en route to the down hole pumps.

Still another object of the invention is to provide an economical method of cementing a well bore that enhances the quality control of the cementing job.

Another object of the invention is to provide a liquid, storable cementitious slurry that can be used by adding liquid activators to the liquid slurry and proportioning any additional mix water and additives to further control the slurry's properties.

Another object of the invention is to provide such a liquid, storable cementitious slurry that can be used in a well cementing operation by simply metering and controlling liquids rather than by mixing dry bulk products with liquids.

Another object of the invention is to continuously formulate a liquid, storable cementitious slurry on one site, transfer the slurry to the site of application where it is activated and its density adjusted, then pumped into the subterranean formation for cementing.

Another object of the invention is to enhance wellsite efficiency by reducing the time required for the cementing operation. Current practices face rate limitations due to the inherent problems of bulk supply, particle wetting and dispersion, etc. Use of a pre-mixed, storable slurry removes these restrictions, permitting the operation to be carried out consistently at high rates.

SUMMARY OF THE INVENTION

The storable, hydraulically-active, cementitious slurry of the invention is suitable for cementing within subterranean formations for oil or gas wells. The storable slurry comprises a hydraulically-active cementitious material of a type suitable for cementing within subterranean formations for oil or gas wells; an effective amount of a set retarder to allow the storage of the slurry with a minimal change of the slurry's set characteristics after activation and to allow the reversal of the retardation after adding an effective amount of an activator to the slurry prior to cementing; a suspending agent for maintaining the slurry with minimal separation of the cementitious material, an effective amount of water to form a pumpable slurry and optionally, a dispersant to maintain the fluidity of the mix.

In one method of the invention, a subterranean formation for an oil or gas well is cemented with the storable, hydraulically-active, cementitious slurry formulated by mixing together a hydraulically-active cementitious material, a set retarder, a suspending agent, water, and optionally a dispersant, wherein the storable slurry's characteristics minimally change during storage. The storable slurry is stored until required for cementing, at which time it is activated by mixing together an activator and the storable slurry, pumped into the subterranean formation and allowed to set.

In another method of the invention, the density of the slurry is measured and adjusted to the desired density for a particular cementing application by metering and control-

ling liquids rather than by mixing dry bulk products and liquids.

In still another method of the invention the steps of the method are performed at two different locations. In this method, the stable, hydraulically-active, cementitious slurry is formulated at one location, transferred to a second location, activated at the second location, then pumped into the subterranean formation for cementing.

Additional effects, features and advantages will be apparent in the written description that follows.

DETAILED DESCRIPTION OF THE INVENTION

A storable, hydraulically-active, cementitious slurry of the invention is made from a hydraulically-active cementitious material. Hydraulically-active cementitious materials include materials with hydraulic properties, such as hydraulic cement, slag and blends of hydraulic cement and slag (slagment) which are well known in the art. The term "hydraulic cement" refers to any inorganic cement that hardens or sets due to hydration. In this disclosure, the term "hydraulically-active" refers to properties of a cementitious material that allow the material to set in a manner like hydraulic cement, either with or without additional activation. Hydraulically-active cementitious materials may also have minor amounts of extenders such as bentonite, gilsonite, and cementitious materials used either without any appreciable sand or aggregate material or admixed with a granular filling material such as sand, ground limestone, the like. Strength enhancers such as silica powder or silica flour can be employed as well. Hydraulic cements, for instance, include portland cements, aluminous cements, pozzolan cements, fly ash cements, and the like. Thus, for example, any of the oilwell type cements of the class "A-H" and "J" as listed in the API Spec 10, (1st ed., 1982), are suitable hydraulic cements.

The type of slag used for the invention has hydraulic properties. The slag is preferably ground-granulated blast furnace slag with a minimum glass count of about 95% and a fine particle size of about 1 to about 100 μm , preferably less than about 45 μm , most preferably less than 10 μm or a fineness of about 310 to about 540 m^2/kg . See, e.g., U.S. Pat. Nos. 5,125,455 and 5,106,423. A slag slurry develops little strength without increasing the alkalinity of the slurry to initiate hydration. Slag alone can also produce a brittle set product and fluid loss from the slag slurry can be difficult to control.

Slagments are preferably blends of slag and portland cement. Examples of suitable slagments include blends ranging from about 90% cement with 10% slag to 10% cement with 90% slag, with a particularly preferred blend of 60% slag with 40% cement with all percentages based on the dry weight of each component.

Slagment and hydraulic cement are preferred cementitious materials. However, both of these materials react quickly with water and set at room temperature unless modified, and they are, therefore, much more difficult to control. The interstitial water of both cement and slagment slurries is also very aggressive, for example, having a high pH. Yet, storable slurries formed from hydraulic cement, especially portland cement, or slagment have the best overall performance characteristics for well cementing applications.

A set retarder is necessary to prevent the setting of the slurry during storage. The characteristics of these set retard-

ers are diverse and important. An effective amount of set retarder allows the storage of the slurries with minimal changes in the characteristics of both the stored and activated slurry. It is equally important that this effect is reversible after adding an effective amount or low concentration of activator to the slurry, even at low well circulating temperatures. In addition, the set retarder should preferably provide some dispersion of the slurry without overdispersion, and little effect on the compressive strength after activation and setting.

Suitable set retarders include glucoheptonates, such as sodium glucoheptonate, calcium glucoheptonate and magnesium glucoheptonate; lignin sulfonates, such as sodium lignosulfonate and calcium sodium lignosulfonate; gluconates, such as sodium gluconate, calcium gluconate and calcium sodium gluconate; phosphonates, such as the sodium salt of EDTA phosphonic acid; sugars, such as sucrose; hydroxycarboxylic acids, such as citric acid; and the like, as well as their blends. Calcium gluconate for hydraulic cement and slagment slurries and sodium glucoheptonate for slag slurries are especially preferred.

The amount of set retarder can vary, depending on the type of cementitious material, the type of set retarder selected and the desired storage time. Since this disclosure refers to both slags and hydraulic cements, the term "BWOC" refers to by weight of the cementitious material. For slagments and hydraulic cements, typical amounts of gluconates and glucoheptonates range from about 0.1% to about 5% BWOC, preferably from about 0.2% to about 1% BWOC, with about 0.5% BWOC of calcium gluconate especially preferred. For slags, typical amounts of gluconates and glucoheptonates range from 0% to about 3% BWOC, with about 0.1% to about 0.4% BWOC of sodium glucoheptonate especially preferred.

Because the cementitious material may separate during storage due to reduced interparticle interactions when compared with normal cement slurries, adding a suspending agent maintains the slurry with minimal separation of the cementitious material. Certain types of suspending agents of the type used in the drilling mud industry can be used for the purposes of the present invention. These suspending agents include polymers, clays, emulsions, transition metal oxides and hydroxides, and the like. Because more than one suspending agent can be used in the storable slurry, in this disclosure, the term "suspending agent" refers to one or more suspending agents. While some particle separation can still occur over time, routine agitation redisperses the separated particles and rehomogenizes the slurry during storage.

However, the long term suspension of storable cementitious slurries can be somewhat problematic. Both hydraulic cement and slagment slurries pose more difficulties due to the aggressive nature of the interstitial water. This aggressive nature of the interstitial water hydrolyzes some polymers, initiates gelation or crosslinking of other polymers and impairs the long-term support properties of clays by ion-exchange, for example. Suitable suspending agents for hydraulic cements and slagments, therefore, should not gel, crosslink or hydrolyze polymers, nor impair the long-term support of clays. Specific examples of suspending agents useful for the purposes of the present invention include polysaccharides, such as welan gums "BIOZAN", Kelco, San Diego, Calif.), xanthan gums, cellulose and its derivatives like carboxymethyl cellulose, polyanionic cellulose "DRISPAC", Drilling Specialties, Bartlesville, Okla.), carboxymethylhydroxyethyl cellulose, guar and its derivatives, starch, succinoglycan "SHELLFLO-S", Shell International Chemical Co., Ltd., London, England); polyethylene oxide

"POLYOX PEO", Union Carbide, Danbury, Conn.); clays such as bentonite and attapulgite; mixed metal hydroxides "POLYVIS", SKW, Trostberg, Germany); as well as their combinations, and oil-in-water emulsions created with paraffin oils and stabilized with ethoxylated surfactants. "SHELLFLO-S.", polyethylene oxide and bentonite are especially preferred for portland cements and slagments. Slag slurries are preferably suspended using xanthan gums with or without bentonite clay.

The amount of suspending agent used in the storable slurry depends on the type of hydraulically-active cementitious material and selected suspending agent. For slag, the amount of xanthan gum preferably ranges from 0 to about 2 ppb with the bentonite ranging from 0 to about 8 ppb, with about 0.66 of xanthan gum and 0 to about 3 ppb of bentonite especially preferred. For hydraulic cement and slagment, the amount of "SHELLFLO-S." preferably ranges from 0 to about 0.4 gpb based on the amount of the mixwater, with about 0.1 gpb to about 0.2 gpb preferred, and bentonite ranges from 0 to about 10 ppb, with 0 to about 3 ppb preferred. If polyethylene oxide is used alone, the amount preferably ranges from 0 to about 5 ppb with about 0.5 ppb to about 2 ppb especially preferred. Polyethylene oxide may be combined with any of the other suspending agents.

An optional dispersing agent may be used in the storable slurry to control the fluidity of the slurry. The amount of dispersing agent depends of the type of hydraulically-active cementitious material used, selected suspending agent and desired density of the storable slurry. Specific examples of dispersing agents include melamine sulfonic acid polymer condensation product "SP5", "CORMIX", Warrington, England), sodium polyacrylate "BEVALOID 6770", Rhône-Poulenc, Watford, England), naphthalene sulfonic acid polymer "LOMARD", Diamond Shamrock Chemicals Co., Morristown, N.J.), and sulfonated-styrene maleic anhydride polymer "SSMA", (Miltemp, Milpark, Houston, Tex.). The preferred dispersing agent is SSMA and the amount preferably ranges from 0 to about 5 pounds per barrel of mix water, with about 1 to about 3 pounds per barrel especially preferred.

Mixing water containing the above-mentioned additives with the dry hydraulically-active cementitious materials produces the storable slurry. A sufficient amount of water, preferably fresh water, should be added to the hydraulically-active cementitious material to form a liquid storable slurry of suitable consistency. A storable slurry with portland cement should have a density measuring in the range from about 11 to 17.5 lbm/gal and preferably in the range of about 14 to 17.5 lbm/gal, more preferably about 15-16.5 lbm/gal. Storable portland cement slurries at densities about 17.5 lbm/gal and greater have a tendency to gel or undergo a type of "pack-setting" when stored for prolonged periods. Slurry densities for slag slurries of about 15 lbm/gal are preferable.

Depending upon the particular storable slurry, the amount of mixing water in the slurry of the present invention ranges from about 30 to 150 weight percent based upon the dry weight of cement and preferably is in the range of about 35 to 90 weight percent.

Under normal conditions, the storable slurries of the invention have considerable longevity. The storable slurry of the invention should remain stable as a liquid, preferably for about a week and more preferably about two to three months without setting. In some cases, storage times in excess of six months will be achieved. Changes in thickening time of the activated hydraulic cement slurries, even after prolonged storage of the nonactivated slurry, are not excessive and such

changes are readily determined using techniques known in the art.

At the time of cementing, the stored slurry is activated, pumped into the well and allowed to set. Activation occurs by adding an activator. The activator initiates hydration and allows the slurry to set after a predetermined pumping time.

The activator must counteract the set retarder while having a minimal effect on final slurry properties or set characteristics, such as rheology and fluid loss when used in an effective amount. In addition, the activator should be easy to pump and handle, such as a liquid; economical; widely available at reasonable purity; safe to ship and handle and environmentally acceptable.

Activators for a storable slurry include solutions of Group IA and IIA hydroxides, such as sodium hydroxide, magnesium hydroxide and calcium hydroxide; sulfates, such as sodium sulfate; aluminates, such as sodium aluminate and potassium aluminate; carbonates, such as sodium carbonate and silicates. Preferred activators are sodium silicates. Sodium silicate has a large number of industrial uses which include drilling fluids and waterproofing mortars and cements. For slag slurries a sodium silicate "Crystal 120H", Crosfield, Warrington, England) with a particular silica/soda ratio is especially preferred. Sodium silicate ("Crystal 100S", Crosfield) with a different silica/soda ratio is especially preferred for hydraulic cement and slagment slurries. Typical concentrations of activator range from about 0 to about 8 gpb of slurry, preferably about 1 to about 3 gpb of slurry and are preferably added with additional mixwater.

There are two approaches for controlling the thickening time of the activated storable slurries. The first approach is to accurately meter or measure out the activator based on a dose-response curve so the stored slurry becomes "less retarded" and provides the desired thickening time. Because the slope of the dose-response curve may be steep, the slurries may be too sensitive to permit the accurate control of thickening at the wellsite.

The second approach is to "over-activate" the slurry and add additional or secondary set retarders, such as lignin sulfonates, tartrates, gluconates, glucoheptonates, and the like, to achieve the desired thickening time. The "over-activated" slurries respond normally to conventional levels of retarder and exhibit far less sensitivity. In addition, "over-activation" might boost the early compressive strength of the set slurries. A typical concentration of additional set retarder sodium lignosulfonate "R12-1", 40% active, Boregard, Sarpsborg, Norway) ranges from 0 to about 1 gpb.

Extra water is preferably added to the storable slurry during activation. This extra water may be fresh water, sea water or brine. The extra water may contain activator and additional additives, for instance, potassium chloride, dispersants, viscosifiers, secondary retarders, liquid suspensions of weighting agents and chemical extending agents.

The activated slurry can be adjusted to the desired density for a particular cementing application. The slurry density can be increased by the addition of a liquid suspension of a weighting agent, such as trimanganese tetraoxide. Lower density slurries can be prepared by adding more water and modifying activator concentrations, if required. Thus, storable slurry "concentrates" can be made in advance and diluted when activated. For example, a 12.5 lbm/gal portland cement slurry can be prepared by adding 2-3 gallons sodium silicate activator per bbl of slurry and around 38 gallons of additional water per bbl to a storable slurry having the initial density around 15.8 to 16.5 lbm/gal.

Preferably, a pumpable slurry is formed with a measured density ranging from about 11 to about 20 lbm/gal, more preferably in the range of about 14 to about 16 lbm/gal and most preferably about 15 lbm/gal. Although the latter is a lower density than conventional "neat cement", the mechanical properties of the set cement are appropriate for well cementing applications. Furthermore, the volume yield increases and the rheology improves by this slight density reduction.

Once set, the storable slurries of the invention have normal levels of compressive strength.

In the preferred method of the invention, a storable cementitious slurry is made using an oilwell type portland cement, for example, "Dyckerhoff Class G" (Dyckerhoff Zementwerke, Wiesbaden, Germany). The cement is mixed together with a calcium gluconate (0.5–0.75% BWOC) set retarder, 3 ppb of bentonite and about 0.1 gpb "SHELLFLO-S" suspending agent (or alternatively with 2 ppb "POLYOX PEO" alone) and sufficient water to reach a density of about 15.8 to 16.5 lbm/gal. Dispersants, such as polyacrylate, sulfonated styrene maleic anhydride, naphthalene sulfonic acid polymer, and the like, are well known in the art and can be added to the above mixture as needed. The resultant slurry can be kept with occasional agitation for periods of time exceeding twelve weeks under normal storage conditions.

The storable slurry is activated by adding the necessary amount of activator, in this case sodium silicate (100S) is preferably added in an amount of 1 to 3 gpb of slurry before pumping into the well bore. The activator is preferably added with a small volume of additional water to adjust the final density of the activated slurry to 15 lbm/gal.

Table 4 shows rheological properties for three storable slurries and demonstrates that the rheological properties are changed minimally when kept for prolonged periods. The slurries have some viscosification upon activation. If such viscosification is undesirable, it can be substantially eliminated by adding dispersants to the slurry. Table 5 shows the rheological properties for three activated slurries and demonstrates that the rheological properties are minimally changed.

Fluid loss control is essential for many conventional cementing applications, for example, squeeze cementing and the cementing of liners and production strings. The addition of conventional cementing fluid-loss additives, such as polyvinyl alcohol, styrene-butadiene latex, co- and ter-polymers of acrylamidomethylpropanesulfonic acid, hydroxyethyl cellulose, carboxymethyl hydroxyethyl cellulose, carboxymethyl cellulose and starch, to storable hydraulic cement and slagment slurries, at the time of activation, provides acceptable levels of control.

A number of additional factors may affect the performance of the storable slurries of the invention. Conventional cement slurries, under certain circumstances, are sensitive to shear and exhibit changes in rheology and thickening time, for example, that depend on the mixing energy or pipe shear to which they are exposed. The storable slurries of the invention do not exhibit undue shear sensitivity and, therefore, should be mixable with a variety of field equipment.

The storable slurry of the invention offers the option of adding material either to the slurry itself or to extra mixwater used to dilute the slurry to the final design density. It is well known that the response of cements to certain additives, for example, dispersants, retarders and gelling agents depends on how the additives are introduced to the slurry. Dry blended additives often elicit qualitatively different perfor-

mance characteristics than those added to mixwater. Even greater differences are sometimes seen if additives are added to an already-mixed slurry. The order of addition of activator and additional additives to the slurry has little effect on the rheology of the activated slurry when mixed at normal API shear rates.

The following example is provided to increase the understanding of the invention, without limiting the scope of the invention.

EXAMPLE 1

All of the experiments using slag were run with slag having a fineness of 420 m²/kg. All experiments with portland cement used "Dyckerhoff Class G" or "Cemol Class G" cement. Slagments were 70/30 blends ordinary portland cement (Castle Cement, Coatbridge, Strathclyde, Scotland) and 420 m²/kg fineness slag.

The experimental protocols followed standard laboratory testing procedures outlined in the API Specification 10. Where necessary, these procedures were modified, such as when the order of addition and mixing energy variables were being studied.

Mixwater was placed in a plastic beaker and stirred with a paddle mixer while adding the suspending agent until the suspending agent was dispersed or hydrated. Next, the set retarder was added while stirring until dissolved. Finally the optional dispersant was added while stirring until dissolved.

The mixwater prepared above was transferred to a Waring blender fitted with an electronic speed control with the speed adjusted until forming a good vortex. While maintaining the vortex by controlling the blender speed, the hydraulically-active cementitious material was added and the time of addition recorded. After 60 s of stirring the slurry, the blender was stopped.

The slurry was transferred to a Fann 35 viscometer cup while noting the slurry's physical characteristics. The initial slurry rheology was measured, and optionally at 10 s and 10 min., using standard rotor 1, spring 1 and bob 1 viscometer configuration at room temperature.

Next, the slurry was transferred to a wide-mouthed plastic bottle fitted with a screw top lid and tightly sealed. The bottle was stored for extended periods of time.

At regular intervals during storage, the slurry's condition was checked. Using a small spatula, free water, gel strengths, the separation of cementitious material particulates, gelation, setting and the general appearance of the slurry were noted. Then, the slurry was remixed thoroughly by stirring and shaking. When desired, the rheology was checked as described above. The storage and testing continued until the slurry set hard. The hard set was usually preceded by a period of high slurry viscosity and gelation, rendering the material unusable before it actually set.

The activation and testing of the final slurry was done with either freshly prepared slurry or stored slurry. A similar mixing energy as described in API Spec 10, §5 for conventional cements was used. The slurry was placed in an electronically controlled Waring blender and stirred at 4,000 rpm for 60 s. The activator plus dilution water and any additional additives were then introduced at 4,000 rpm within a 15 s interval. The mixture was next blended at 12,000 rpm for 35 s.

After final activation and blending, the slurry was tested like a conventional cement slurry. Conventional antifoams could be used to reduce air entrainment as required.

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TABLE 1

STORABLE SLURRY STABILITY TESTING						
No.	SLURRY DENSITY	CEMENT TYPE	SUSPENDING AND DISPERSING AGENTS ¹	RETARDER % BWOC	TIME WEEKS	COMMENTS
1	15	Slag	0.33 ppb welan gum ²	0.1 NaGH ³	1	stable
2	15	Slag	0.9 ppb xanthan ⁴	0.1 NaGH	4	stable
					7	acceptable/ settling
3	15	Slag	0.66 ppb xanthan	0.1 NaGH	7	stable
					14	acceptable/ settling
4	16	Slag	0.9 ppb xanthan	0.1 NaGH	2	mod. gel
5	15	Slagment	0.9 ppb xanthan	0.5 NaGH	1	sedimented
6	15	Slagment	0.2 gpb SS ⁵	0.5 NaGH	1	stable, fluid
					7	stable
7	15.8	Portland	0.7 ppb xanthan	0.5 NaGH	1	stable
					2	settling
8	15.8	Portland	0.9 ppb xanthan + 1 gpb NSAP ⁶	0.5 NaGH	1	settling
9	15.8	Portland	0.7 ppb welan gum	0.5 NaGH	1	stable/gel
					3	gel/thick
10	15.8	Portland	0.5 ppb welan gum	0.5 NaGH	2	settling
11	15.8	Portland	0.3 ppb welan gum	0.5 NaGH	1	settling
12	15.8	Portland	1 ppb CMC ⁷ + 0.8 gpb NSAP	0.5 NaGH	1	bad gel
13	15.8	Portland	0.4 ppb CMC + 0.1 gpb PA ⁸	0.5 NaGH	7	stable
					9	set
14	15.8	Portland	1 ppb PAC ⁹	0.5 NaGH	1	bad gel
15	15.8	Portland	1 ppb CMHEC ¹⁰	0.5 NaGH	1	thixotropic gel
16	15.8	Portland	1 ppb Starch	0.5 NaGH	1	bad gel
17	15.8	Portland	5 ppb Attapulgate	0.5 NaGH	1	settling
18	15.8	Portland	5 ppb Attapulgate + 0.4 ppb xanthan	0.5 NaGH	1	bad gel
19	15.8	Portland	5 ppb BC ¹¹	0.5 NaGH	1	thick
20	15.8	Portland	3 ppb BC	0.5 NaGH	4	stable
					5	some settling
21	15.8	Portland	3 ppb BC + 0.03 gpb ppb AlCH ¹²	0.5 NaGH	1	stable
					2	bad gel
22	15.8	Portland	2 ppb BC + 8.3 ppb microsilica ¹³	0.5 NaGH	1	stable
					2	bad gel
23	17	Portland	5 ppb BC + 0.8 gpb NSAP	0.5 NaGH	1	sediment
24	15.8	Portland	5 ppb BC + 0.2 xanthan	0.5 NaGH	2	stable
					4	mod gel
					5	set
25	16.5	Portland	3 ppb BC + 0.2 xanthan	0.5 NaGH	3	stable
					4	thick
					5	set
26	16.5	Portland	0.2 ppb welan gum	0.5 NaGH	1	bad gel
27	16.5	Portland	0.1% PVP ¹⁴	0.5 NaGH	1	gel/sediment
28	15.8	Portland	oil emulsion ¹⁵	0.5 NaGH	1	compact
29	16.5	Portland	0.2 gpb SS	0.5 NaGH	1	settling
					3	compact
30	16.5	Portland	20 ppt XL- guar ¹⁶	0.5 NaGH	1	gelled
31	16.5	Portland	5% BWOC Fe ₂ O ₃ , orange ¹⁷	0.5 NaGH	1	stable
					3	thick/compact

TABLE 1-continued

STORABLE SLURRY STABILITY TESTING						
No.	SLURRY DENSITY	CEMENT TYPE	SUSPENDING AND DISPERSING AGENTS ¹	RETARDER % BWOC	TIME WEEKS	COMMENTS
32	16.5	Portland	3% BWOC Magneplus ¹⁸	0.5 NaGH	1	gelled
33	16.5	Portland	0.2 ppb welan gum	0.5 CaG ¹⁹	2	stable
34	15.8	Portland	4 ppb BC	0.4 CaG	3	compacted
					3	stable
35	15.8	Portland	0.27 gpb SS + 0.27 gpb PA	0.5 CaG	4	stable >
					4	T. Time test
36	15.8	Portland	0.7 ppb xanthan + 0.32 gpb PA	0.5 CaG	1	slightly gelled
					7	slightly sedimented
37	16.5	Portland	0.2 gpb SS + 0.4 PA	0.5 CaG	4	settled
					4	
38	15.8	Portland	3 ppb BC + 0.1 gpb SS + 0.3 gpb PA	0.5 CaG	5	stable
					6	gel
39	15.8	Portland	3 ppb BC	0.5 CaG	7	thick
					7	stable
40	15.8	Portland	2 ppb PEO ²⁰	0.5 CaG	7	stable
41	16.5	Portland	1.6 ppb PEO	0.5 CaG	6	stable
42	15.8	Portland	0.5 ppb SSMA ²¹	0.5 CaG	8	stable
			1.5 ppb PEO			
			1.5 ppb SSMA			

¹All concentrations of suspending and dispersing agents are based on the quantity of mix water.
²Welan gum biopolymer, "BIOZAN"
³Sodium glucoheptonate
⁴Xanthan gum
⁵Succinoglycan, "SHELLFLO-S"
⁶Naphthalene sulfonic acid polymer
⁷Carboxymethyl cellulose
⁸Soidum polyacrylate
⁹Polyanionic cellulose, "DRISPAC"
¹⁰Carboxymethylhydroxyethyl cellulose
¹¹Bentonite clay
¹²Aluminum chlorohydroxide
¹³Microsilica, Elkem Chemical, Kristiansand, Norway
¹⁴Polyvinylpyrrolidone
¹⁵5% bvol Lotox oil/95% bvol fresh water stabilized with sulfonated nonyl phenol ethoxylate surfactant
¹⁶Crosslinked guar
¹⁷Ferric oxide, fine (±0.5 micron) pigment grade, Bayer AG, Germany
¹⁸Magnesia cement
¹⁹Calcium gluconate
²⁰Polyethylene oxide, "POLYOX"
²¹Sulfonated styrene maleic anhydride

TABLE 2

STORABLE SLURRY SET RETARDATION						
SLURRY DENSITY	RETARDER	CONC.		STORAGE TIME (DAYS)		
		% BWOC	SUSPENDING AGENT	CEMENT TYPE ¹	SLAG	PORTLAND
15	NaGH ²	0	0.66 ppb xanthan ³	8		
15	NaGH	0.1	0.66 ppb xanthan	103<		
15	NaGH	0.2	0.66 ppb xanthan	103<		
15	NaGH	0.4	0.66 ppb xanthan	103<		
15	NaGH	0.3	2 ppb BC ⁴	13		

TABLE 2-continued

STORABLE SLURRY SET RETARDATION						
SLURRY DENSITY	RETARDER	CONC.		STORAGE TIME (DAYS) CEMENT TYPE ¹		
		% BWOC	SUSPENDING AGENT	SLAG	SLAG-MENT	PORT-LAND
15	CaG ⁵	0.5	0.12 gpb SS ⁶		54<	
15.8	NaGH	0.2	0.45% BWOC xanthan			9
15.8	NaGH	0.3	0.45% BWOC xanthan			24
15.8	NaGH	0.5	0.45% BWOC xanthan			39
16.5	NaGH	0.7	0.45% BWOC xanthan			38
16.5	NaG ⁷	0.5	3 ppb BC			58<
16.5	CaG	0.2	3 ppb BC			17
16.5	CaG	0.4	3 ppb BC			38<
16.5	CaG	0.5	3 ppb BC			61<
15.8	CaG	0.7	3 ppb BC			54<
16.5	Citric acid	0.5	3 ppb BC			22
16.5	CSLS ⁸	0.5	3 ppb BC			8
16.5	Sucrose	0.5	3 ppb BC			Gel
15.8	CaG	0.5	1.5 ppb PEO ⁹			60<
15.8	CaG	0.5	1.5 pb PEO			60<
			1.5 ppb SSMA ¹⁰			

¹Time in days indicates when the stored slurry hardened. In some cases the slurry would be unsuitable for use prior to this time.

²Sodium glucoheptonate

³Xanthan gum

⁴Bentonite clay

⁵Calcium gluconate

⁶"SHELLFLO-S"

⁷Sodium gluconate

⁸Calcium sodium lignosulfonate

⁹Polyethylene oxide

¹⁰Sulfonated styrene maleic anhydride

TABLE 3

ACTIVATION OF STORABLE SLURRIES					
SLURRY		CEMENT	ACTIVATOR	COMMENTS	
DENSITY	RETARDER	TYPE	TYPE	CONC	21° C. (70° F.)
15	0.1% NaGH ¹	Slag ²	Na sulfate	10 ppb	Ineffective
15	0.1% NaGH	Slag	Soda ash	10 ppb	49 hrs set
15	0.1% NaGH	Slag	Sodium silicate 100S	2 gpb	14 hrs set, suitable activator
15	0.1% NaGH	Slag	30% NaOH	0.5 gpb	48 hrs, no set
15	0.5% CaGH ³	Slag-ment ⁴	Sodium silicate 100S	3 gpb	14 hrs set, suitable activator
15.8	0.5% NaGH	Port. ⁵	Dyn 531 ⁶	1.5 gpb	ineffective
15.8	0.5% NaGH	Port.	STC ⁷	1.5 gpb	ineffective
15.8	0.5% NaGH	Port.	STC	3 gpb	slow activation, 4 day
15.8	0.5% NaGH	Port.	Sodium silicate 120H	3 gpb	16 hrs set, suitable activator
15.8	0.5% CaGH	Port.	Sodium silicate 100S	3 ppb	16 hrs. set, suitable activator

¹Sodium glucoheptonate

²The suspending agent for all slag slurries was 0.66 ppb xanthan based on the mix water.

³Calcium glucoheptonate

TABLE 3-continued

ACTIVATION OF STORABLE SLURRIES					
SLURRY		CEMENT		ACTIVATOR	
DENSITY	RETARDER	TYPE	TYPE	CONC	21° C. (70° F.)

⁴The suspending agent for all slagment slurries was 0.2 gpb succinoglycan based on the mix water.
⁵The suspending agent for all portland cement slurries was 3 ppb bentonite clay based on the mix water.
⁶"DYNAGUNIT 531", Sika GmBh, Germany
⁷Sodium thiocyanate

TABLE 4

RHEOLOGY OF STORABLE SLURRIES							
NO.	SLURRY DENSITY	RETARDER	SUSPENDING AGENT ¹	CEMENT TYPE	TIME DAYS	RHEOLOGY PV/YP	COMMENTS, 21° C. (70° F.)
1	15	0.1% NaGH ²	0.66 ppb xanthan ³	Slag	0	150/9	small change in properties
2	15.8	0.5% CaG ⁴	3 ppb BC ⁵	Portland	15 0 14 21	130/2 39/20 42/30 49/32	small change in properties
3	15.8	0.5% CaG	1.5 ppb PEO ⁶ 1.5 ppb SSMA ⁷	Portland	0 33	52/8 54/11	very minor changes in properties

¹All concentration of suspending agent were based on the quantity of mix water.
²Sodium glucoheptonate
³Xanthan gum
⁴Calcium gluconate
⁵Bentonite clay
⁶Polyethylene oxide
⁷Sulfonated styrene maleic anhydride

TABLE 5

RHEOLOGY OF ACTIVATED SLURRIES							
SLURRY DENSITY (>)	SET	ACTIVATOR		RHEOLOGY PV/YP			
DILUTED DENSITY)	RETARDER % BWOC	SUSPENDING AGENT ¹	Sodium Silicate ²	CEMENT TYPE	PRE-ACT	POST-ACT	COMMENTS 21° C. (70° F.)
15	0.1% NaGH ³	.66 ppb xanthan ⁴	1.5 gpb 120H	Slag	147/8	150/5	little change in properties
15.8 > 15	0.5% CaG ⁵	3 ppb BC ⁶	3 gpb 100S	Port.	50/32	24/31	acceptable after dilution
15.8 > 15	0.5% CaG	1.5 ppb PEO ⁷ 1.5 ppb SSMA ⁸	2 gpb 100S	Port.	54/11	36/18	acceptable after dilution

¹The concentration of the suspending agent was based on the quantity of mix water.
²The concentration of activator was based on the quantity of slurry.
³Sodium Glucoheptonate
⁴Xanthan gum
⁵Calcium gluconate
⁶Bentonite clay
⁷Polyethylene oxide
⁸Sulfonated styrene maleic anhydride

TABLE 6

THICKENING TIMES ¹ OF ACTIVATED MIXES							
SLURRY DENSITY	RETARDER % BWOC	Sodium Silicate ²	CEMENT TYPE	SECOND RETARDER	T °C. (°F.)	T. TIME MIN	COMMENT
15	0.1% NaGH ³	1.25 gpb 100S	Slag ⁴		71 (160)	360	
15	0.1% NaGH	.25 gpb 100S	Slag		110 (230)	240	
15	0.1% NaGH	.75 gpb 120H	Slag		110 (230)	93	
15	0.1% NaGH	3 gpb 120H	Slag		71 (160)	200	
15	0.1% NaGH	.75 gpb 120H	Slag		110 (230)	110	
15.8 > 15	0.5% CaG ⁵	1 gpb 100S	Port. ⁶		71 (160)	1037	
15.8 > 15	0.5% CaG	1.5 gpb 100S	Port.		71 (160)	876	
15.8 > 15	0.5% CaG	1.65 gpb 100S	Port.		71 (160)	406	
15.8 > 15	0.5% CaG	1.8 gpb 100S	Port.		71 (160)	100	
15.8 > 15	0.5% CaG	2 gpb 100S	Port.		71 (160)	56	
15.8 > 15	0.5% CaG	2 gpb 100S	Port.	0.1 gpb R12-1 ⁷	71 (160)	110	
15.8 > 15	0.5% CaG	2 gpb 100S	Port.	0.2 gpb R12-1	71 (160)	239	
15.8 > 15	0.5% CaG	2.2 gpb 100S	Port.	0.2 gpob R12-1	71 (160)	125	
15.8 > 12.5	0.5% CaG	2.2 gpb 100S	Port.		71 (160)	90	
15.8 > 12.5	0.5% CaG	2.2 gpb 100S	Port.		49 (120)	225	
15.8 > 15	0.5% CaG	3 gpb 100S	Port.		49 (120)	140	4 week slurry
15.8 > 15	0.5% CaG	3 gpb 100S	Port.		49 (120)	113	
15.8 > 15	0.5% CaG	3 gpb 100S	Port.		49 (120)	101	1.4 ppb SSMA ⁸
15.8 > 15	0.5% CaG	3 gpb 100S	Port.		49 (120)	116	0.35 gpb NSAP ⁹
15.8 > 15	0.5% CaG	3 gpb 100S	Port.		49 (120)	190	0.35 gpb PA ¹⁰
15.8 > 14.5	0.5% CaG	2.5 gpb 100S	Port. ¹¹		71 (160)	77	1.5 ppb SSMA
15 > 14.5	0.5% CaG	2.5 gpb 100S	Slag-ment ¹²		71 (160)	78	1.4 ppb SSMA

¹Thickening time curves generally showed that 100 Bc were reached quickly after thickening had begun. The activator and additional retarder were mixed into dilution water, except for the runs with a density of 12.5 lbm/gal where sea water was added first. Except where noted, tests were done on freshly prepared mixes.

²The concentration of sodium silicate is based on the quantity of slurry.

³Sodium glucoheptonate

⁴0.66 ppb (mix water) welan gum suspending agent for all slag slurries

⁵Calcium gluconate

⁶3 ppb (mix water) bentonite clay suspending agent for cement slurries

⁷Sodium lignosulfonate, 40% active, "Boregard"

⁸Sulfonated styrene maleic anhydride

⁹Naphthalene sulfonic acid polymer

¹⁰Polyacrylate

¹¹1.5 ppb (mixwater) PEO was used as a suspending agent and 1.5 ppb SSMA was used as a dispersant.

¹²The suspending agent for the slagment slurry was 0.2 gpb of succinoglycan based on the amount of mixwater.

EXAMPLE 2

The following results were found when testing the compressive strength using the following formulation. An especially preferred storable slurry was formed as described in Example 1 with portland cement, 0.5% CaG, 1.5 ppb polyethylene oxide and 1.5 ppb sulfonated styrene maleic anhydride. The resulting slurry had a density of 15.8 lbm/gal.

The slurry was activated with 2.2 gpb 100S sodium silicate and diluted to a final density of 15 lbm/gal. At a curing temperature of 88° C. (190° F.), the following compressive strengths were measured.

TEST PERIOD (HRS)	COMPRESSIVE STRENGTH (PSI)
8	1900
24	3250

-continued

TEST PERIOD (HRS)	COMPRESSIVE STRENGTH (PSI)
48	3750

As the above examples show, the slurries of the invention are stable and can be stored for long periods of time while yielding excellent compressive strengths. Because these stable slurries do not set immediately, they can be made at one site and transferred to another site. For example, the slurries can be formulated at one location, such as on land, with the density of the slurry measured and adjusted if desired. Next, the formulated slurry is transferred to a second location, such as an offshore rig. At the second location the transferred slurry may be immediately activated or stored until needed and subsequently activated. At the time of activation, additional mix water and additives are added, while the slurry's density is adjusted to a desired density. The activated slurry is then pumped into the well-

bore for the purpose of supporting the casing and isolating subterranean formations.

An invention has been shown with several advantages. The ability to store a liquid cement slurry eliminates onsite mixing problems, particularly the control of slurry density. Proportioning a liquid slurry with liquids, such as extra water or a weighting agent, is far simpler than proportioning bulk solids with water.

Simpler equipment can be used with the storable slurries of the invention. The slurries can be kept in nonpressurized tanks and loaded and unloaded with conventional fluid pumps. When cementing, the mixing unit need do no more than homogenize the fluid streams of the slurry plus additional mixwater and liquid additives en route to the downhole pumps.

The ability to prepare and control the quality of a storable slurry at the base is obviously advantageous. The slurry is mixed and its initial density measured and adjusted at the base rather than at the wellsite. The slurry need only be homogenized and activated during the cementing operation. The stability of the slurry and longterm fluidity allow the slurry to be prepared, transferred and stored a considerable time before needed for wellsite operations. Thus, the slurry may be prepared at a central facility and stored in liquid form at the facility. From there it is loaded aboard trucks or workboats and transferred to the remote wellsite. At the wellsite, it may be offloaded and stored or used immediately for cementing operations.

The slurry can be transferred with centrifugal pumps between storage tanks, transport tanks and downhole pumps much faster than dry cement can be transferred pneumatically. Similarly, the time to offload cargo to an offshore location would be reduced. For land locations, the slurry could be prepared at the rigsite while drilling is in progress or at a central facility and truck to the wellsite, days before the cementing operation and stored until needed.

The activated slurry can be easily modified to be used for a wide variety of cementing purposes desirable in oil and gas well cementing applications. A few example of these properties include gas control, fluid loss control, turbulent flow rheology and high early strength.

While the invention is shown in only some of its forms, it is not thus limited but is susceptible to various changes and modifications without departing from the spirit and scope of the invention.

What is claimed is:

1. A storable, hydraulically-active, cementitious slurry comprising:
 - a hydraulically-active cementitious material suitable for cementing within subterranean formations for oil or gas wells;
 - an effective amount of a set retarder to allow the storage of the slurry with a minimal change of the slurry's set characteristics upon activation and to allow the reversal of retardation after adding an effective amount of an activator to the slurry prior to cementing;
 - a suspending agent for maintaining the slurry with minimal separation of the cementitious material;
 - an activating agent;
 - an effective amount of water to form a pumpable slurry; wherein an effective amount of activating agent is added which is sufficient to overactivate the slurry and wherein an additional amount of set retarder is added to the slurry to achieve a setting time.
2. The storable, hydraulically-active, cementitious slurry of claim 1, wherein the set retarder additionally disperses the slurry and has little effect on compressive strength of the storable slurry after activation and setting.

3. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the set retarder is selected from the group consisting of:

hydroxycarboxylic acids, glucoheptonates, lignin sulfonates, gluconates, phosphonates, and sugars.

4. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the set retarder is selected from the group consisting of:

sodium glucoheptonate, calcium glucoheptonate, magnesium glucoheptonate, lignin sulfonate, sodium lignosulfonate, calcium sodium lignosulfonate, sodium gluconate, calcium gluconate, calcium sodium gluconate, sodium EDTA phosphonate, sucrose and citric acid.

5. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the set retarder is selected from the group consisting of:

sodium glucoheptonate, sodium gluconate, calcium gluconate, calcium sodium lignosulfonate, sucrose and citric acid.

6. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the set retarder is sodium glucoheptonate present in an amount ranging from 0.1 to about 3% BWOC and the cementitious material is slag.

7. The storable, hydraulically-active, cementitious slurry of claim 5, wherein the set retarder is in an amount ranging from about 0.1% to about 5% BWOC and the cementitious material contains hydraulic cement.

8. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is selected from the group consisting of:

welan gum, xanthan gum, carboxymethyl cellulose, polyanionic cellulose, carboxymethylhydroxyethyl cellulose, guar, starch, polyethylene oxide and succinoglycan.

9. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is bentonite or attapulgite.

10. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is a mixed metal hydroxide.

11. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is a mixture of bentonite and xanthan gum and the cementitious material is slag.

12. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is polyethylene oxide.

13. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the suspending agent is a mixture of bentonite and succinoglycan.

14. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the cementitious material is selected from the group consisting of:

slag, hydraulic cement and mixtures thereof.

15. The storable, hydraulically-active, cementitious slurry of claim 2, wherein the cementitious material contains portland cement.

16. The storable, hydraulically-active, cementitious slurry of claim 14, further comprising a dispersant.

17. The storable, hydraulically-active, cementitious slurry of claim 16, wherein the dispersant is selected from the group consisting of:

melamine sulfonic acid polymer, sodium polyacrylate, naphthalene sulfonic acid polymer, and sulfonated-styrene maleic anhydride polymer.

* * * * *



US005409064A

United States Patent [19]

Cowan

[11] Patent Number: 5,409,064

[45] Date of Patent: Apr. 25, 1995

[54] OPTIMIZING BLAST FURNACE SLAG CEMENTS

[75] Inventor: Kenneth M. Cowan, Sugar Land, Tex.
[73] Assignee: Shell Oil Company, Houston, Tex.
[21] Appl. No.: 176,143
[22] Filed: Dec. 30, 1993

[51] Int. Cl.⁶ E21B 33/13
[52] U.S. Cl. 166/293; 166/292;
106/790
[58] Field of Search 166/292, 293; 106/789,
106/790

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Primary Examiner—George A. Suchfield

[57] ABSTRACT

A method and composition for cementing a well by combining water, blast furnace slag and sodium pyrophosphate to form a cement slurry, displacing the cement slurry into a well and allowing the cement slurry to set.

60 Claims, 12 Drawing Sheets

TABLE 11

Base Slurry: "NEWCEM" Blast Furnace Slag + 0.1% Sodium Gluconate (bwos*) + 50% Distilled Water (bwos) Test Temperature: 150° F.										
	No Activator	0.10% Activator	0.20% Activator	0.40% Activator	0.80% Activator	1% Activator	1.20% Activator	1.40% Activator	1.60% Activator	1.80% Activator
Time to 50 psi	43.15	22.52	15.7	9.68	4.98	4.53	4.2	4	2.95	2.27
Time to 500 psi	53.37	28.9	20.35	12.62	6	5.58	5.28	4.83	3.57	2.63
Time from 50 psi to 500 psi	10.22	6.38	4.65	2.94	1.02	1.05	1.08	0.83	0.62	0.36
Activator:Retarder Ratio	0	1:1	2:1	4:1	8:1	10:1	12:1	14:1	16:1	18:1
	2% Activator	2.20% Activator	2.40% Activator	2.60% Activator	2.80% Activator	3% Activator	4% Activator	5% Activator	6% Activator	7% Activator
Time to 50 psi	2.23	2	2.1	1.82	1.43	1.5	1.2	1.02	1	0.97
Time to 500 psi	2.68	2.38	2.45	2.2	1.62	1.75	1.45	1.15	1.15	1.12
Time from 50 psi to 500 psi	0.45	0.38	0.35	0.38	0.19	0.25	0.25	0.13	0.15	0.15
Activator:Retarder Ratio	20:1	22:1	24:1	26:1	28:1	30:1	40:1	50:1	60:1	70:1

*bwos = by weight of slag

TABLE 12

Base Slurry: "NEWCEM" Blast Furnace Slag + 0.1% Sodium Gluconate (bwos*) + 50% Distilled Water (bwos) Test Temperature: 175° F.										
	No Activator	0.10% Activator	0.20% Activator	0.40% Activator	0.80% Activator	1% Activator	1.20% Activator	1.40% Activator	1.60% Activator	1.80% Activator
Time to 50 psi	17.95	10.3	7.37	4.17	2.58	2.1	1.87	1.38	1.48	1.4
Time to 500 psi	22.27	15.12	9.57	5.68	3.45	2.72	2.38	1.68	1.78	1.73
Time from 50 psi to 500 psi	4.32	4.82	2.2	1.51	0.87	0.62	0.51	0.3	0.3	0.33
Activator:Retarder Ratio	0	1:1	2:1	4:1	8:1	10:1	12:1	14:1	16:1	18:1
	2% Activator	2.20% Activator	2.40% Activator	2.60% Activator	2.80% Activator	3% Activator	4% Activator	5% Activator	6% Activator	7% Activator
Time to 50 psi	1.05	1.17	1.03	1.15	1.22	0.73	0.6	0.62	0.62	0.72
Time to 500 psi	1.22	1.37	1.27	1.33	1.4	0.83	0.73	0.75	0.7	0.83
Time from 50 psi to 500 psi	0.17	0.2	0.24	0.18	0.18	0.1	0.13	0.13	0.08	0.11
Activator:Retarder Ratio	20:1	22:1	24:1	26:1	28:1	30:1	40:1	50:1	60:1	70:1

*bwos = by weight of slag

What is claimed is:

1. A method for cementing a well, comprising:
combining constituents comprising water, blast furnace slag having a particle size within the range of 2,000 to 15,000 cm²/g, and an activator comprising sodium pyrophosphate to form a cement slurry; displacing the cement slurry into the well; and allowing the cement slurry to set.
2. The method of claim 1 wherein the activator includes an oxalate ion-containing compound.
3. The method of claim 1 wherein the activator includes a citrate ion-containing compound.
4. The method of claim 3 wherein the citrate ion-containing compound is selected from the group consisting of sodium citrate, calcium citrate and potassium citrate.
5. The method of claim 1 wherein the weight ratio of activator to slag is adjusted to achieve optimum compressive strength of the cement.
6. The method of claim 5 wherein the weight ratio of activator to slag is further adjusted in accordance with well temperature to achieve optimum compressive strength of the cement.
7. The method of claim 3 wherein the ratio of activator components is adjusted to provide at least one of the following: (a) optimum set time of the cement slurry, (b) optimum compressive strength of the cement, (c) optimum early compressive strength development rate of the cement slurry, and (d) optimum rheological properties for the cement slurry.
8. The method of claim 3 wherein the weight ratio of activator to slag is adjusted to achieve optimum compressive strength of the cement.
9. The method of claim 8 wherein the weight ratio of activator to slag is further adjusted in accordance with well temperature to achieve optimum compressive strength of the cement.

10. The method of claim 5 wherein the activator includes multiple components and wherein the ratio of activator components is adjusted to provide at least one of the following: (a) optimum set time of the cement slurry, (b) optimum compressive strength of the cement, (c) optimum early compressive strength development rate of the cement slurry, and (d) optimum rheological properties for the cement slurry.

11. The method of claim 6 the activator includes multiple components and wherein the ratio of activator components is adjusted to provide at least one of the following: (a) optimum set time of the cement slurry, (b) optimum compressive strength of the cement, (c) optimum early compressive strength development rate of the cement slurry, and (d) optimum rheological properties for the cement slurry.

12. The method of claim 1 including adding a retarder to provide adequate fluidity time of the cement slurry in order to place the cement in the well.

13. The method of claim 12 wherein the retarder is a salt of a transition metal with an atomic number above iron in the periodic chart.

14. The method of claim 13 wherein the retarder is a copper, zinc or aluminum salt.

15. The method of claim 12 wherein the retarder is a complexing agent.

16. The method of claim 15 wherein the retarder is a lignosulfonate, sulfonated lignin, or lignin amine.

17. The method of claim 15 wherein the retarder is sodium glucoheptonate, sodium gluconate or sodium citrate.

18. The method of claim 12 wherein a ratio of weight of activator to weight of retarder is selected to provide the greatest early compressive strength development and the greatest final strength for a given slag concentration.

19. The method of claim 18 wherein the activator/retarder weight ratio is selected at the static temperature of the well to provide substantially the greatest early compressive strength development and substantially the greatest final strength for a given slag concentration.

20. The method of claim 18 wherein the activator/retarder ratio is selected for a set time of less than about ten hours.

21. The method of claim 18 wherein the activator/retarder ratio is selected for a set time of less than about eight hours.

22. The method of claim 18 wherein the activator/retarder ratio is selected for a set time of between three and six hours.

23. The method of claim 3 including adding a retarder to provide adequate fluidity time of the cement slurry in order to place the cement in the well.

24. The method of claim 23 wherein the retarder is a salt of a transition metal with an atomic number above iron in the periodic chart.

25. The method of claim 24 wherein the retarder is a copper, zinc or aluminum salt.

26. The method of claim 23 wherein the retarder is a complexing agent.

27. The method of claim 26 wherein the retarder is a lignosulfonate, sulfonated lignin, or lignin amine.

28. The method of claim 26 wherein the retarder is sodium glucoheptonate, sodium gluconate or sodium citrate.

29. The method of claim 23 wherein a ratio of weight of activator to weight of retarder is selected to provide the greatest early compressive strength development

and the greatest final strength for a given slag concentration.

30. The method of claim 29 wherein the activator/retarder weight ratio is selected at the static temperature of the well to provide substantially the greatest early compressive strength development and substantially the greatest final strength for a given slag concentration.

31. The method of claim 29 wherein the activator/retarder ratio is selected for a set time of less than about ten hours.

32. The method of claim 29 wherein the activator/retarder ratio is selected for a set time of less than about eight hours.

33. The method of claim 29 wherein the activator/retarder ratio is selected for a set time of between three and six hours.

34. The method of claim 1 including adding a drilling fluid to the cement slurry.

35. The method of claim 5 including adding a retarder to provide adequate fluidity time of the cement slurry in order to place the cement in the well.

36. The method of claim 35 wherein the retarder is a salt of a transition metal with an atomic number above iron in the periodic chart.

37. The method of claim 36 wherein the retarder is a copper, zinc or aluminum salt.

38. The method of claim 35 wherein the retarder is a complexing agent.

39. The method of claim 38 wherein the retarder is a lignosulfonate, sulfonated lignin, or lignin amine.

40. The method of claim 38 wherein the retarder is sodium glucoheptonate, sodium gluconate or sodium citrate.

41. The method of claim 35 wherein a ratio of weight of activator to weight of retarder is selected to provide the greatest early compressive strength development and the greatest final strength for a given slag concentration.

42. The method of claim 41 wherein the activator/retarder weight ratio is selected at the static temperature of the well to provide substantially the greatest early compressive strength development and substantially the greatest final strength for a given slag concentration.

43. The method of claim 41 wherein the activator/retarder ratio is selected for a set time of less than about ten hours.

44. The method of claim 41 wherein the activator/retarder ratio is selected for a set time of less than about eight hours.

45. The method of claim 41 wherein the activator/retarder ratio is selected for a set time of between three and six hours.

46. The method of claim 41 including adding a drilling fluid to the slurry.

47. The method of claim 7 including adding a retarder to provide adequate fluidity time of the cement slurry in order to place the cement in the well.

48. The method of claim 47 wherein the retarder is a salt of a transition metal with an atomic number above iron in the periodic chart.

49. The method of claim 48 wherein the retarder is a copper, zinc or aluminum salt.

50. The method of claim 47 wherein the retarder is a complexing agent.

51. The method of claim 50 wherein the retarder is a lignosulfonate, sulfonated lignin, or lignin amine.

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52. The method of claim 51 wherein the retarder is sodium glucoheptonate, sodium gluconate or sodium citrate.

53. The method of claim 47 wherein a ratio of weight of activator to weight of retarder is selected to provide the greatest early compressive strength development and the greatest final strength for a given slag concentration.

54. The method of claim 53 wherein the activator/retarder weight ratio is selected at the static temperature of the well to provide substantially the greatest early compressive strength development and substantially the greatest final strength for a given slag concentration.

55. The method of claim 53 wherein the activator/retarder ratio is selected for a set time of less than about ten hours.

56. The method of claim 53 wherein the activator/retarder ratio is selected for a set time of less than about eight hours.

57. The method of claim 53 wherein the activator/retarder ratio is selected for a set time of between three and six hours.

58. The method of claim 53 including adding a drilling fluid to the slurry.

59. The method of claim 1 including selecting an activator which also functions as a good dispersing agent, whereby dispersion will favor better compressive strength development after setting of the cement slurry.

60. The method of claim 1 including adding a sulfide scavenging compound to the cement slurry, said scavenging compound being selected from the group consisting of zinc oxide and zinc carbonate.

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United States Patent [19]

Hale et al.

[11] Patent Number: 5,058,679

[45] Date of Patent: Oct. 22, 1991

[54] SOLIDIFICATION OF WATER BASED MUDS

[75] Inventors: Arthur H. Hale, Houston; Kenneth M. Cowan, Sugarland, both of Tex.

[73] Assignee: Shell Oil Company, Houston, Tex.

[21] Appl. No.: 671,627

[22] Filed: Mar. 19, 1991

Related U.S. Application Data

[63] Continuation-in-part of Ser. No. 641,794, Jan. 16, 1991, abandoned, which is a continuation of Ser. No. 457,429, Dec. 27, 1989, abandoned.

[51] Int. Cl.⁵ E21B 33/13; E21B 33/14

[52] U.S. Cl. 166/293; 166/292

[58] Field of Search 166/292, 293; 175/65, 175/66; 252/8.51, 8.514

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Primary Examiner—George A. Suchfield

[57] ABSTRACT

A drilling mud is converted in-situ to a cement by addition of blast furnace slag.

14 Claims, 3 Drawing Sheets

PROCESS FLOW SCHEMES

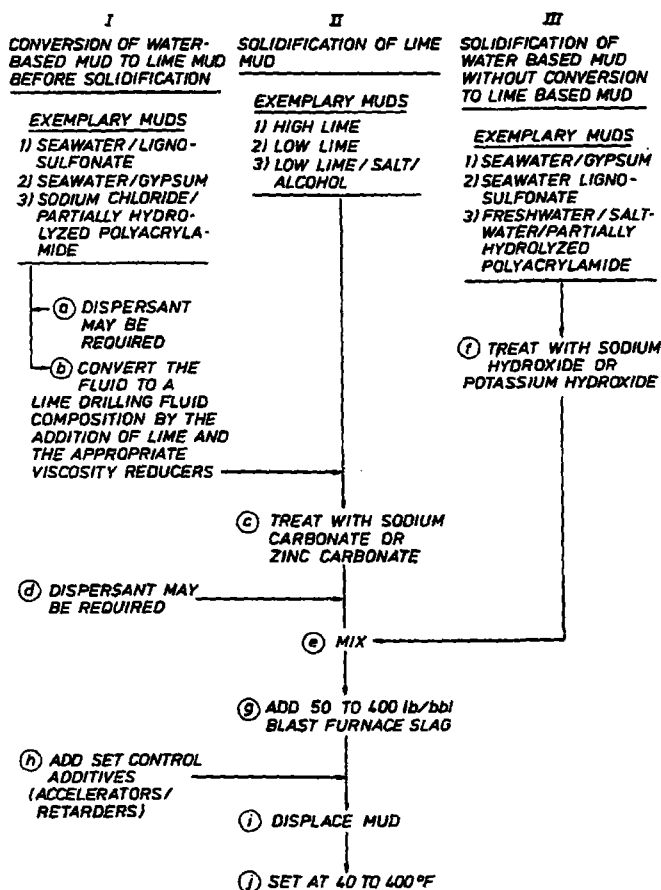


TABLE 5-continued

Initial Setting Times of Salt/Lime/Polyalcohol Drilling Fluid Containing NewCem ¹⁰ Blast Furnace Slag at 150° F. Curing Pressure: 3000 psi				
Drilling Fluid Formulation Number	Drilling Fluid Composition	Test Number	Additives used for Solidification ⁹	Time Required to Reach 50 psi Compression Strength
	296.00 lbs/bbl Barite ¹²			

¹Water phase composed of seawater with 10% NaCl (w/w) added.²Bentonite is a clay or colloidal clay thickening agent.³Rev Dust drill solids is a trade name for clay/quartz solid dust manufactured by MilWhite and is added to simulate drilled solids which would be present in a drilling fluid under actual drilling operations.⁴Morex is a trade name for water-soluble carbohydrate polymer manufactured by Grain Processing Company.⁵Biozan is a trade name for biopolymer manufactured by Kelco Oil Field Group, Inc.⁶Permalose is a trade name for starch manufactured by Milpark.⁷Polydrill is a trade name for synthetic polymer manufactured by SKW Chemicals.⁸See definition supra of POLS.⁹Additives for solidification were added to one barrel of the drilling fluid. The final volume and density increased as a result of the addition of these materials. See Table 7 for density changes.¹⁰NewCem is a trade name for blast furnace slag manufactured by Blue Circle Atlantic, Inc.¹¹MilTemp is a trade name for sulfonated styrene maleic anhydride manufactured by Milpark.¹²Barite is BaSO₄, a drilling fluid weighting agent.

TABLE 6

Compressive Strength Development of Salt/Lime/Polyalcohol Containing NewCem ¹⁰ Blast Furnace Slag at 150° F.					Compressive Strength After Indicated Elapsed Time at 150° F.				
Drilling Fluid Formulation Number	Drilling Fluid Composition	Test Number	Additives Used for Solidification ⁹		24 Hours	48 Hours	72 Hours	96 Hours	120 Hours
1	0.77 bbl/Water ¹		200 lbs/bbl NewCem ¹⁰		0	0	0	0	750
	20.00 lbs/bbl Bentonite ²								
	25.00 lbs/bbl Rev Dust ³								
	4.00 lbs/bbl Lime		200 lbs/bbls NewCem ¹⁰ + 10 lbs/bbl KOH		0	0	260	500	525
	3.00 lbs/bbl Morex ⁴								
	2.00 lbs/bbl Biozan ⁵								
	6.00 lbs/bbl Permalose ⁶								
	6.00 lbs/bbl Polydrill ⁷		200 lbs/bbl NewCem ¹⁰ + 10 lbs/bbl + 10 lbs/bbl Soda Ash		725	810	850	875	910
	36.90 lbs/bbl POLS ⁸								
	158.60 lbs/bbl Barite ¹²								
2	0.77 bbl/Water ¹	1	200 lbs/bbl NewCem ¹⁰		0	0	525	630	670
	20.00 lbs/bbl Bentonite ²								
	25.00 lbs/bbl Rev Dust ³								
	4.00 lbs/bbl Lime	6	200 lbs/bbl NewCem ¹⁰ + 10 lbs/bbl KOH		270	975	—	—	—
	1.50 lbs/bbl Morex ⁴								
	1.50 lbs/bbl Biozan ⁵								
	6.00 lbs/bbl Permalose ⁶								
	6.00 lbs/bbl Polydrill ⁷	2	200 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl Soda Ash		775	865	940	1000	—
	36.90 lbs/bbl POLS ⁸								
	158.60 lbs/bbl Barite ¹²								
		3	200 lbs/bbl NewCem ¹⁰ + 10 lbs/bbl Soda Ash		910	1010	1080	1150	—
		4	200 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl KOH + 5 lbs/bbl Soda Ash		800	880	950	990	—
		5	200 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl KOH + 10 lbs/bbl Soda Ash		1150	1290	1380	1440	—
		7	200 lbs/bbl NewCem ¹⁰ + 10 lbs/bbl KOH + 10 lbs/bbl Soda Ash		890	1020	—	—	—
		8	300 lbs/bbl NewCem ¹⁰ +		1180	—	—	—	—
		10	300 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl Soda Ash 6 lbs/bbl MilTemp ¹¹ (All MilTemp ¹¹ was added to drilling fluid prior to addition of NewCem ¹⁰ .)		0	1300	—	—	—
		9	300 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl Soda Ash 6 lbs/bbl MilTemp ¹¹ (1 lb/bbl of MilTemp ¹¹ was added to the drilling fluid prior to the addition of the NewCem ¹⁰ . The remaining amount was added after the NewCem ¹⁰ addition.)		0	650	—	—	—

TABLE 6-continued

Drilling Fluid Formulation Number	Drilling Fluid Composition	Test Number	Additives Used for Solidification ⁹	Compressive Strength After Indicated Elapsed Time at 150° F.				
				24	48	72	96	120
				Hours	Hours	Hours	Hours	Hours
3	0.67 bbl/Water ¹ 20.00 lbs/bbl Bentonite ² 25.00 lbs/bbl Rev Dust ³ 4.00 lbs/bbl Lime 3.00 lbs/bbl Morex ⁴ 1.50 lbs/bbl Biozan ⁵ 6.00 lbs/bbl Permalose ⁶ 6.00 lbs/bbl Polydrill ⁷ 73.90 lbs/bbl POLS ⁸ 151.00 lbs/bbl Barite ¹²	16	200 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl Soda Ash	1360	1640	—	—	—
4	0.67 bbl/Water ¹ 20.00 lbs/bbl Bentonite ² 25.00 lbs/bbl Rev Dust ³ 4.00 lbs/bbl Lime 1.00 lbs/bbl Morex ⁴ 1.00 lbs/bbl Biozan ⁵ 6.00 lbs/bbl Permalose ⁶ 6.00 lbs/bbl Polydrill ⁷ 36.90 lbs/bbl POLS ⁸ 296.00 lbs/bbl Barite ¹²	12	200 lbs/bbl NewCem ¹⁰ + 5 lbs/bbl Soda Ash	1960	2120	—	—	—

¹Water phase composed of seawater with 10% NaCl (w/w) added.

²Bentonite is a clay or colloidal clay thickening agent.

³Rev Dust drill solids is a trade name for clay/quartz solid dust manufactured by MilWhite and is added to simulate drilled solids which would be present in a drilling fluid under actual drilling operations.

⁴Morex is a trade name for water-soluble carbohydrate polymer manufactured by Grain Processing Company.

⁵Biozan is a trade name for biopolymer manufactured by Kelco Oil Field Group, Inc.

⁶Permalose is a trade name for starch manufactured by Milpark.

⁷Polydrill is a trade name for synthetic polymer manufactured by SKW Chemicals.

⁸See definition supra of POLS.

⁹Additives for solidification were added to one barrel of the drilling fluid. The final volume and density increased as a result of the addition of these materials. See Table 7 for density changes.

¹⁰NewCem is a trade name for blast furnace slag manufactured by Blue Circle Atlantic, Inc.

¹¹MilTemp is a trade name for sulfonated styrene maleic anhydride manufactured by Milpark.

¹²Barite is BaSO₄, a drilling fluid weighting agent.

TABLE 7

Original Drilling Fluid Density	Effect of Solidification Materials on Final Density of Fluid	
	Final Density of Fluid After Addition of: 200 lbs/bbl NewCem	300 lbs/bbl NewCem
12.5 lbs/gal	14.5 lbs/gal	15.2 lbs/gal
15.0 lbs/gal	17.1 lbs/gal	—

TABLE 7-continued

Original Drilling Fluid Density	Effect of Solidification Materials on Final Density of Fluid	
	Final Density of Fluid After Addition of: 200 lbs/bbl NewCem	300 lbs/bbl NewCem
17.0 lbs/gal	19.0 lbs/gal	—

TABLE 8

Solidification of Seawater Systems						
Test Number	Drilling Fluid Composition Number	Additives for Solidification ¹	Compressive Strength		Total Curing Time at 150° F.	
			Non-Destructive Test ²	Destructive Test ³		
3	2	200 lbs/bbl NewCem ⁴ + 10 lbs/bbl Soda Ash	1144 psi	1868 psi	94 hours, 11 minutes	
4	2	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl KOH + 5 lbs/bbl Soda Ash	972 psi	1635 psi	94 hours, 16 minutes	
5	2	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl KOH + 10 lbs/bbl Soda Ash	1422 psi	2146 psi	94 hours, 20 minutes	
2	2	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl Soda Ash	985 psi	1376 psi	94 hours, 24 minutes	
18	2A	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl Soda Ash	—	1556 psi ⁵	48 hours	
19	2A	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl Soda Ash	—	1485 psi ⁵	48 hours	
20	2A	200 lbs/bbl NewCem ⁴ + 5 lbs/bbl Soda Ash	—	1655 psi ⁵	48 hours	
21	2A	300 lbs/bbl NewCem ⁴ +	—	2252 psi ⁵	48 hours	

TABLE 8-continued

Solidification of Seawater Systems					
Test Number	Drilling Fluid Composition Number	Additives for Solidification ¹	Compressive Strength		Total Curing Time at 150° F.
			Non-Destructive Test ²	Destructive Test ³	

5 lbs/bbl Soda Ash

¹Additives for solidification were added to one barrel of the drilling fluid. The final volume and density increased as a result of the addition of these materials. See Table 7 for density changes.

²Performed on the Halliburton Ultrasonic Cement Analyzer at 150° F. and under 3000 psi confining pressure.

³Performed at atmospheric pressure and ambient (75° F.) temperature on the samples taken from the Halliburton Ultrasonic Cement Analyzer.

⁴NewCem is a trade name for blast furnace slag manufactured by Blue Circle Atlantic Inc.

⁵Cured for 48 hours at 159° F. and tested.

TABLE 9

Solidification of Seawater Systems				
Drilling Fluid Composition	Test Number	Additives Used for Solidification ¹	Compressive Strength After Indicated Elapsed Time at 150° F.	
			24 Hours	48 Hours

Seawater/Lignosulfonate	24	200 lbs/bbl NewCem ² + 5 lbs/bbl Soda Ash	1360	1640
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Bullwinkle Field Mud	27	200 lbs/bbl NewCem ² + 5 lbs/bbl Soda Ash	1960	2120
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¹Additives for solidification were added to one barrel of the drilling fluid. The final volume and density increased as a result of the addition of these materials. See Table 7 for density changes.

²NewCem is a trade name for blast furnace slag manufactured by Blue Circle Atlantic Inc.

TABLE 10

KCl-Partially Hydrolyzed Polyacrylamide (PHPA) Mud and Bullwinkle Field Mud				
Additive	KCl/PHPA Mud Amount (lb/bbl)		Field Mud Amount (lb/bbl)	
Lime	4		4	
Sodium Carbonate	5		5	
NaOH		4		4
NewCem	200	200	200	200

Time (Hours)	KCl/PHPA Mud Compressive Strength (psi)		Field Mud Compressive Strength (psi)	
24	735	738	2429	—
48	807	801	2620	—
72	919	956	2673	1765
96				2133
120				2341

Destructive test performed at atmospheric pressure and ambient temperature. KCl-PHPA mud had the following formulation: water 0.834 bbl, bentonite 6 lbs/bbl, partially hydrolyzed polyacrylamide (PHPA) 0.6 lb/bbl, KCl 18 lbs/bbl, KOH 0.3 lb/bbl, carboxymethyl cellulose low viscosity 2 lbs/bbl, drill solids 30 lb/bbl and barite 86.1 lbs/bbl.

2. The method of claim 1 wherein the drilling fluid is a lime mud.

30 3. The method of claim 1 wherein the drilling fluid is a non-lime mud.

4. The method of claim 1 wherein the drilling fluid is a non-lime mud which has been converted to a lime mud.

35 5. The method of claim 4 the non-lime mud is converted to a lime mud by addition of lime and a viscosity reducer prior to the addition of said blast furnace slag.

6. The method of claim 2 or 5 wherein the lime mud is treated with at least one of (1) sodium carbonate, and (2) zinc carbonate prior to the addition of said blast furnace slag.

40 7. The method of claim 3 wherein the non-lime mud is treated with at least one of (1) sodium hydroxide, and (2) potassium hydroxide prior to the addition of said blast furnace slag.

45 8. The method of claim 2 wherein the mud comprises lime, salt, and alcohol.

9. The method of claim 8 wherein the alcohol is an

TABLE 11

Solidification With Portland Cement					
Drilling Fluid Composition	Test Number	Additives Used for Solidification ¹	Compressive Strength After Indicated Elapsed Time at 150° F.		
			24 Hours	48 Hours	72 Hours

II	28	200 lbs/bbl Portland Cement Class H + 5 lbs/bbl Soda Ash	0	0	360
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Bullwinkle Field Mud	29	200 lbs/bbl Portland Cement Class H + 5 lbs/bbl Soda Ash	0	0	0
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¹Additives for solidification were added to one barrel of the drilling fluid. The final volume and density increased as a result of the addition of these materials. See Table 7 for density changes.

What is claimed is:

1. A method for solidifying an aqueous drilling fluid in a borehole comprising:

admixing blast furnace slag with the drilling fluid; 65
displacing the drilling fluid to a preselected location in the borehole; and
allowing the drilling fluid to solidify in-situ.

acyclic polyol.

10. The method of claim 8 wherein the alcohol is a cyclicetherpolyol.

11. The method of claim 8 wherein the alcohol is a monocyclicdietherdiol.

12. The method of claim 8 wherein the alcohol is a polycyclicpolyetherpolyol.