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Señora Jefe de la
DIVISION DE NUEVAS CREACIONES
SUPERINTENDENCIA DE INDUSTRIA Y COMERCIO
E S D

Referencia Expediente No 00 083 187

Solicitante **ORMAT INDUSTRIES LTD**

Asunto Solicitud de patente para **"MÉTODO Y
APARATO PARA PROCESAR SUMINISTROS DE
HIDROCARBUROS PESADOS"**

Fecha de solicitud 01 de noviembre de 2000

TRAMITE 002 - EVENTO: 001 - ACTUACIÓN- 329

1 Yo, Emilio FERRERO, obrando como apoderado de la solicitante en referencia, atentamente presento con este escrito la copia certificada de la solicitud de patente estadounidense No 09/431,159 del 01 de noviembre de 1999, junto con su respectiva traducción de sus reivindicaciones y certificaciones, de la cual se reclama prioridad en esta solicitud de patente

2 Ruego a la Señora Jefe se sirva aceptar este escrito con sus anexos, y se continúe con el trámite de la solicitud

Bogotá, -9 ENE 2001
Señora Jefe,



EMILIO FERRERO
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llr COLO 11802-801-002-3
MRE-15



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United States Patent and Trademark Office

October 20, 2000

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OFFICE OF THOSE PAPERS OF THE BELOW IDENTIFIED PATENT
APPLICATION THAT MET THE REQUIREMENTS TO BE GRANTED A
FILING DATE UNDER 35 USC 111**

APPLICATION NUMBER 09/431,159

FILING DATE November 01, 1999



**By Authority of the
COMMISSIONER OF PATENTS AND TRADEMARKS**

N Williams
N WILLIAMS
Certifying Officer

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BOX PATENT APPLICATION

Attorney Docket No P-15149

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Application of

Yoram BRONICKI

Serial No NOT YET ASSIGNED

Filed November 1, 1999

For METHOD OF AND APPARATUS FOR PROCESSING HEAVY HYDROCARBON FEEDS

U.S. PATENT
09/431159
11/01/99

TRANSMITTAL LETTER

Assistant Commissioner for Patents
Washington, D C 20231

Sir

Submitted herewith for filing in the U S Patent and Trademark Office is the following

- (1) Transmittal Letter
- (2) PTO Form-1082
- (3) 28 page Patent Application consisting of
 - 14 pages of Textual Specification
 - 3 pages of 10 claims
 - 1 Abstract of the Disclosure
 - 10 sheets of drawings
- (4) Unexecuted Inventor's Declaration
- (5) Early Serial Number Notification Postcard

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Patent, Trademark and Copyright Cases
Unfair Competition, Trade Secrets,
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** Registered Patent Agents not Admitted in DC

FORM PTO-1082

TRANSMITTAL FOR NEW U.S. PATENT APPLICATION

Assistant Commissioner for
Patents and Trademarks
Washington, D.C. 20231

Re New U.S. Patent Application
For METHOD OF AND APPARATUS FOR
PROCESSING HEAVY HYDROCARBON FEEDS
Inventor(s) Yoram BRONICKI
Attorney Docket P-15149

Sir

Attached hereto is the application identified above, including

28 Pages Application Consisting of
14 Pages of Textual Specification
3 Pages of 10 Claims
1 Abstract of the Disclosure
10 Sheets of drawings
X Unexecuted Inventor's Declaration

The Government filing fee is calculated as follows

Total Claims	10 - 20 = 0	x \$18.00	= \$0.00
Independent Claims	2 - 3 = 0	x \$78.00	= \$0.00
Base Fee			\$760.00
Multiple Dependent Claim Fee (\$250.00)			\$0.00
Subtotal			\$760.00

TOTAL FILING FEE*

\$760.00

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- Reduced by one-half, as applicant(s) is/are a "small entity"
A Declaration Claiming Small Entity Status
- will be filed at a later date
- is submitted herewith
- Foreign priority is claimed under 35 U S C § 119 from Patent Application(s) No dated ____
- Priority document(s) will be submitted at a later date
- Priority document(s) is/are submitted herewith
- ☒ Executed Declaration(s) will be submitted at a later date pursuant to 37 CFR § 1 41 and § 1 53, with an appropriate surcharge under 37 CFR § 1 16(e)
- ☒ Formal drawing(s) is/are attached
- Formal drawing(s) will be submitted at a later date
- Assignment document(s) is/are submitted herewith, the recordation fee of \$40 00 per document is enclosed herewith
- A Verified Translation will be submitted at a later date
- ☒ No payment is enclosed at this time Full payment will be made when the executed Declaration is submitted
- Submitted herewith is a check in the amount of \$

Respectfully submitted,

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METHOD OF AND APPARATUS FOR PROCESSING HEAVY HYDROCARBON FEEDS
DESCRIPTION

1 Technical Field

This invention relates to processing heavy hydrocarbon feeds containing sulfur, metals, and asphaltenes which may be used in refineries and/or producing power, and more particularly, to a method of and apparatus for upgrading heavy crude oils or fractions thereof

2 Background of the Invention

Many types of heavy crude oils contain high concentrations of sulfur compounds, organo-metallic compounds, and heavy, non-distillable fractions called asphaltenes that are insoluble in light paraffins such as n-pentane. Because most petroleum products used for fuel must have a low sulfur content, the sulfur compounds in the non-distillable fractions reduce their value to petroleum refiners and increase their cost to users of such fractions as fuel or as raw material for producing other products. In order to increase the saleability of these non-distillable fractions, refiners must resort to various expedients for removing sulfur compounds.

A conventional approach to removing sulfur compounds in distillable fractions of crude oil, or its derivatives, is catalytic hydrogenation in the presence of molecular hydrogen at moderate pressure and temperature. While this approach is cost effective in removing sulfur from distillable oils, problems arise when the feed includes metallic-containing asphaltenes. Specifically, the presence of metallic-containing asphaltenes results in catalyst deactivation by reason of the coking tendency of the asphaltenes, and the accumulation of metals on the catalyst, especially nickel and vanadium compounds commonly found in the asphaltenes.

Alternative approaches include coking, high-pressure, desulfurization, and fluidized catalytic cracking of non-distillable oils, and production of asphalt for paving and other uses. All of these processes, however, have disadvantages that are intensified by the presence of high concentrations of metals, sulfur and asphaltenes. In the case of coking non-distillable oils, the cost is high and a disposal market for the resulting high sulfur coke must be found. Furthermore, the products produced from the asphaltene portion of the feed to a coker are almost entirely low valued coke and cracked gases. In the case of residual oil desulfurization, the cost of

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high-pressure equipment, catalyst consumption and long processing times make this alternative undesirably expensive

In U S Patent No 4,191,636, heavy oil is continuously converted into asphaltenes and metal-free oil by hydrotreating the heavy oil to crack asphaltenes selectively and remove heavy metals such as nickel and vanadium simultaneously. The liquid products are separated into a light fraction of an asphaltene-free and metal-free oil and a heavy fraction of an asphaltene and heavy metal-containing oil. The light fraction is recovered as a product and the heavy fraction is recycled to the hydrotreating step.

In U S Patent No 4,528,100, a process for the treatment of residual oil is disclosed, the process comprising the steps of treating the residual oil so as to produce a first extract and a first raffinate using supercritical solvent extraction, and then treating the first raffinate so as to produce a second extract and a second raffinate again by supercritical solvent extraction using a second supercritical solvent and then combining the first extract and the raffinate to a product fuel. In accordance with a particular embodiment of the invention disclosed in the U S '100 patent, the supercritical solvents are particularly selected to concentrate vanadium in the second extract. Thus, even though the amount of vanadium present in the product fuel is low and consequently beneficial for reducing gas turbine maintenance problems as stated in this U S '100 patent, some amount of vanadium does still remain therein.

Another example of a user of the heavier, higher boiling range portion of a hydrocarbon is a refinery with a fluid catalytic cracking unit (a FCC unit). FCC units typically are operated with a feedstock quality constraint of very low metals, asphaltenes, and CCR (i.e., less than 10 wppm metals, less than 0.2 wt% asphaltenes, and less than 2 wt% CCR). Utilization of feedstocks with greater levels of asphaltenes or CCR results in increased coke production and a corresponding reduction in unit capacity. In addition, use of feedstocks with high levels of metals and asphaltenes results in more rapid deactivation of the catalyst, and thus increased catalyst consumption rates and increased catalyst replacement costs.

In U S Patent No 5,192,421, a process for the treatment of whole crude oil is disclosed, the process comprising the steps of deasphalting the crude by first mixing the crude with an aromatic solvent, and then mixing the crude-aromatic solvent mixture with an aliphatic solvent. The U S '421 patent (at page 9, lines 43-45) identifies that certain modifications must be made to prior art solvent deasphalting technologies, such as that described in U S Patent Nos 2,940,920, 3,005,769, and 3,053,751 in order to accommodate the process described in the

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U S '421 patent, in particular since the prior art solvent deasphalting technologies have no means to remove that portion of the charge oil that will vaporize concurrently with the solvent and thus contaminate the solvent used in the process. In addition to being burdened by the complexity and cost resulting from the use of two solvents, the U S '421 process results in a deasphalted product that still contains a non-distilled portion with levels of CCR and metals that exceed the desired levels of such contaminants.

In U S Patent No 4,686,028 a process for the treatment of whole crude oil is disclosed, the process comprising the steps of deasphalting a high boiling range hydrocarbon in a two-stage deasphalting process to separate asphaltene, resin, and deasphalted fractions, followed by upgrading only the resin fraction by hydrogenation or visbreaking. The U S '028 patent is burdened by the complexity and cost of a two-stage solvent deasphalting system used to separate the resin fraction from the deasphalted oil. In addition, like the U S '421 patent, the '028 process results in an upgraded product that still contains a non-distilled fraction - the DAO - that is contaminated with CCR and metals.

Metals contained in heavy oils contaminate and spoil the performance of catalysts in fluidized catalytic cracking units. Asphaltenes present in such oils are converted to high yields of coke and gas which burden an operator with high coke burning requirements.

Another alternative available to a refiner or heavy crude user is to dispose of the non-distillable heavy oil fractions as fuel for industrial power generation or as bunker fuel for ships. Disposal of such fractions as fuel is not particularly profitable to a refiner because more valuable distillate oils must be added in order to reduce viscosity sufficiently (e.g. producing heavy fuel oil, etc.) to allow handling and shipping. Furthermore, the presence of high sulfur and metals contaminants lessens the value to users. In addition, this does not solve the problem of the non-distillable heavy oil fractions in a global sense since environmental regulations restrict the use of high sulfur fuel oil. Refiners frequently use a thermal conversion process, e.g., visbreaking, for reducing the heavy fuel oil yield. This process converts a limited amount of the heavy oil to lower viscosity light oil, but has the disadvantage of using some of the higher value distillate oils to reduce the viscosity of the heavy oil sufficiently to allow handling and shipping. Moreover, the asphaltene content of the heavy oil restricts severely the degree of visbreaking conversion possible due to the tendency of the asphaltene to condense into heavier materials, even coke, and cause instability in the resulting

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fuel oil. Furthermore, this process reduces the amount of heavy fuel oil that the refiner has to sell and is not useful in a refinery processing heavy crudes.

Many proposals thus have been for dealing with crude and metals. And while many are technically viable, they appear to have achieved little or no commercialization, due, in large measure, to the high cost of the technology involved. Usually such cost takes the form of increased catalyst contamination by the metals and/or the carbon deposition resulting from the attempted conversion of the asphaltene fractions.

An example of the processes proposed in order to cope with high metals and asphaltenes is disclosed in U.S. Patent No. 4,500,416. In one embodiment, an asphaltene-containing hydrocarbon feed is solvent deasphalted in a deasphalting zone to produce a deasphalted oil (DAO) fraction, and an asphaltene fraction which is catalytically hydrotreated in a hydrotreating zone to produce a reduced asphaltene stream that is fractionated to produce light distillate fractions and a first heavy distillate fraction. Both the first heavy distillate fraction and the DAO fraction are thermally cracked into a product stream that is then fractionated into light distillate fractions and a second heavy distillate fraction which is routed to the hydrotreating zone.

In an alternative embodiment, an asphaltene-containing hydrocarbon feed is solvent deasphalted in a deasphalting zone to produce a deasphalted oil (DAO) fraction, and an asphaltene fraction which is catalytically hydrotreated in a hydrotreating zone to produce a reduced asphaltene stream that is fractionated to produce light distillate fractions and a first heavy distillate fraction. The first heavy distillate fraction is routed to the deasphalting zone for deasphalting, and the DAO fraction is thermally cracked into a product stream that is then fractionated into light fractions and a second heavy distillate fraction which is routed to the hydrotreating zone.

In each embodiment in the 416 patent, asphaltenes are routed to a hydrotreating zone wherein heavy metals present in the asphaltenes cause a number of problems. Primarily, the presence of the heavy metals in the hydrotreater causes deactivation of the catalyst that increases the cost of the operation. In addition, such heavy metals also result in having to employ higher pressures in the hydrotreater which complicates its design and operation and hence its cost.

It is therefore an object of the present invention to provide a new and improved method of and apparatus for processing and upgrading heavy hydrocarbon feeds containing sulfur, metals, and asphaltenes, wherein the disadvantages as outlined are reduced or substantially overcome.

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SUMMARY OF THE INVENTION

Apparatus for processing a heavy hydrocarbon feed, in accordance with the present invention, comprises firstly a heater for heating the heavy hydrocarbon feed. The heated heavy hydrocarbon feed produced is fed to an atmospheric fractionating tower for fractionating the heated heavy hydrocarbon feed fed to the inlet of the atmospheric fractionating tower producing light atmospheric fractions and atmospheric bottoms. In addition, the apparatus includes a vacuum fractionating tower for fractionating heated atmospheric bottoms, heated by a further heater, and producing lighter vacuum fractions and vacuum residue. Furthermore, the apparatus includes a solvent deasphalting (SDA) unit for producing deasphalted oil (DAO) and asphaltenes from the vacuum residue as well as a thermal cracker for thermally cracking the deasphalted oil and producing a thermally cracked product which is recycled to the inlet of the atmospheric fractionating tower. Moreover, the apparatus can include a further thermal cracker for thermally cracking the lighter vacuum fractions for producing a further thermally cracked product which is recycled to the inlet of the atmospheric fractionating tower. If preferred, the lighter vacuum fractions can be supplied to the thermal cracker in addition to the deasphalted oil. In such a case, the further thermal cracker previously mentioned is not used.

Furthermore, the present invention includes a method for processing a heavy hydrocarbon feed comprising the steps of heating a heavy hydrocarbon feed and fractionating the heated heavy hydrocarbon feed in an atmospheric fractionating tower for producing light atmospheric fractions and atmospheric bottoms. Heated atmospheric bottoms, heated by a further heater, are fractionated in a vacuum fractionating tower for producing lighter vacuum fractions and vacuum residue while the vacuum residue are solvent deasphalted in a solvent deasphalting (SDA) unit for producing deasphalted oil (DAO) and asphaltenes. The deasphalted oil is then thermally cracked in a thermal cracker for producing a thermally cracked product that is recycled to the inlet of the atmospheric fractionating tower. In addition, the lighter vacuum fractions can be thermally cracked for producing a further thermally cracked product that is recycled to the inlet of the atmospheric fractionating tower. Thermal cracking of the lighter vacuum fractions can be carried out in a separate thermal cracker or in the same thermal cracker in which the deasphalted oil is thermally cracked. Similar apparatus and methods are disclosed in U. S. Patent Application Serial No. 08/910,102, the disclosure of which is hereby incorporated by reference.

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BRIEF DESCRIPTION OF THE DRAWINGS

Embodiments of the present invention are described by way of example, and with reference to the accompanying drawings wherein

Fig 1 is a block diagram of a first embodiment of the present invention for processing a hydrocarbon feed;

Fig 1a is a block diagram of a modification of the first embodiment of the present invention mentioned above for processing a hydrocarbon feed

Fig 2 is a block diagram of a second embodiment of the present invention for processing a hydrocarbon feed;

Fig 3 is a block diagram of a third embodiment of the present invention for processing a hydrocarbon feed;

Fig 4 is a block diagram of a further embodiment of the present invention for processing a hydrocarbon feed,

Fig 5 is a block diagram of a still further embodiment of the present invention for processing a hydrocarbon feed,

Fig 6 is a block diagram of another embodiment of the present invention for processing a hydrocarbon feed;

Fig 7 is a block diagram of another embodiment of the present invention for processing a hydrocarbon feed,

Fig 8 is a block diagram of another embodiment of the present invention for processing a hydrocarbon feed; and

Fig 9 is a block diagram of another embodiment of the present invention for processing a hydrocarbon feed

Like reference numerals and designations in the various drawings refer to like elements

DETAILED DESCRIPTION

Turning to the drawings, numeral 10 in Fig 1 designates apparatus for processing heavy hydrocarbons in accordance with the present invention wherein heavy hydrocarbon feed is supplied to heater 11 and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12. Atmospheric fractionating tower 12 produces light atmospheric fractions in line 14 and atmospheric bottoms in line 15. The atmospheric bottoms in line 15 are then supplied to heater 16 and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18 which produces light vacuum fractions in line 20 and vacuum residue in line 22. The vacuum residue in line 22 is then supplied to solvent deasphalting unit 24 which produces deasphalted oil in line 26 and asphaltenes in line 28. Deasphalted oil in line 26 is supplied to thermal cracker 30 that produces thermally cracked product in line 32 that is recycled to inlet 13 of atmospheric fractionating tower 12. Moreover, the light vacuum fractions in line 20 are supplied to further thermal cracker 35 for thermally cracking the lighter vacuum fractions and a further thermally cracked product is produced in line 37 that is

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recycled to inlet 13 of atmospheric fractionating tower 12. If preferred, rather than using further thermal cracker 35, the light vacuum fractions in line 20 can be thermally cracked in thermal cracker 30 together with the deasphalted oil supplied in line 26, see Fig 1a

Numeral 10A in Fig 2 designates another embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention wherein heavy hydrocarbon feed is supplied to heater 11A and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12A. Atmospheric fractionating tower 12A produces light atmospheric fractions in lines 14A and atmospheric bottoms in line 16A. The atmospheric bottoms in line 16A are then supplied to heater 17A and heated atmospheric bottoms are supplied vacuum fractionating tower 18A which produces light vacuum fractions in lines 20A, heavier vacuum fractions in line 21 and vacuum residue in line 22A. The vacuum residue in line 22A are then supplied to solvent deasphalting unit 24A which produces deasphalted oil in line 26A and asphaltenes in line 28A. Deasphalted oil in line 26A is supplied to thermal cracker 30A that produces thermally cracked product in line 32A that is recycled to inlet 13A of atmospheric fractionating tower 12A. Moreover, the heavier vacuum fractions in line 21 are supplied to further thermal cracker 35A for thermally cracking the heavier vacuum fractions and a further thermally cracked product is produced in line 37A which is recycled to inlet 13A of atmospheric fractionating tower 12A.

Turning now to the embodiment described with reference to Fig 3, numeral 10B designates a further embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11B and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12B. Atmospheric fractionating tower 12B produces light atmospheric fractions in lines 14B and atmospheric bottoms in line 16B. The atmospheric bottoms in line 16B are then supplied to heater 17B and the heated, atmospheric bottoms are supplied to vacuum fractionating tower 18B which produces light vacuum fractions in lines 20B, heavier vacuum fractions in line 21B as well as vacuum residue in line 22B. The vacuum residue in line 22B is then supplied to solvent deasphalting unit 24B which produces deasphalted oil in line 26B and asphaltenes in line 28B. Deasphalted oil in line 26B is supplied to thermal cracker 30B that produces thermally cracked product in line 32B that is recycled to inlet 13B of atmospheric fractionating tower 12B. Moreover, the heavier vacuum fractions in line 21B are supplied to line 26B to form a combined product that is supplied to thermal cracker 30B.

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In another embodiment of the present invention, described with reference to Fig. 4, numeral 10C designates a still further embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11C and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12C. Atmospheric fractionating tower 12C produces lighter atmospheric fractions in line 14C, light atmospheric fractions in line 15C and atmospheric bottoms in line 16C. The atmospheric bottoms in line 16C are then supplied to heater 17C and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18C which produces light vacuum fractions in line 20C, heavier vacuum fractions in line 21C and vacuum residue in line 22C. The vacuum residue in line 22C are then supplied to solvent deasphalting unit 24C which produces deasphalted oil in line 26C and asphaltenes in line 28C. Deasphalted oil in line 26C is supplied to thermal cracker 30C that produces thermally cracked product in line 32C that is recycled to inlet 13C of atmospheric fractionating tower 12C. Moreover, the heavier vacuum fractions in line 21C are supplied to further thermal cracker 35C for thermally cracking the heavier vacuum fractions and a further thermally cracked product is produced in line 37C which is recycled to inlet 13C of atmospheric fractionating tower 12C. Furthermore, this embodiment includes hydrogen donor apparatus 40C having hydrotreater 45C to which light fraction product in line 39C is supplied and which produces treated hydrocarbon feed in line 41C. Treated hydrocarbon feed in line 41C is supplied to heater 43C and the heated, treated hydrocarbon feed is then fed to further atmospheric fractionating tower 42C. Further atmospheric fractionating tower 42C produces further light atmospheric fractions in lines 44C and further atmospheric bottoms in line 46C. The further atmospheric bottoms in line 46C are then supplied to heater 47C and the heated, further atmospheric bottoms are supplied to further vacuum fractionating tower 48C that produces further light vacuum fractions in lines 50C, further heavier vacuum fractions in line 51C and further vacuum residue in line 52C. In this embodiment, portion of further heavier vacuum fractions or hydrogen donor stream present in line 51C is fed via line 60 to line 26C for input into thermal cracker 30C. A further portion of the hydrogen donor stream is fed to line 21C using line 61 for input into thermal cracker 35C.

Preferably, the ratio of the deasphalted oil present in line 26C to the amount of hydrogen donor stream present in line feed 60 is 0.25 to 4. Also, preferably, the ratio of the heavier vacuum fraction present in line 21C to the amount of hydrogen donor stream present in line 61 is also 0.25 to 4.

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In a further embodiment of the present invention described with reference to Fig 5, numeral 10D designates an even further embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11D and the heated, heavy hydrocarbon feed is fed to atmospheric fractionating tower 12D. Atmospheric fractionating tower 12D produces lighter atmospheric fractions in line 14D, light fractions in line 15D and atmospheric bottoms in line 16D. The atmospheric bottoms in line 16D are then supplied to heater 17D and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18D that produces light vacuum fractions in lines 20D, heavier vacuum fractions in line 21D and vacuum residue in line 22D. The vacuum residue in line 22D are then supplied to solvent deasphalting unit 24D that produces deasphalted oil in line 26D and asphaltenes in line 28D. Deasphalted oil in line 26D is supplied to thermal cracker 30D that produces thermally cracked product in line 32D that is recycled to inlet 13D of atmospheric fractionating tower 12D. Moreover, the heavier vacuum fractions in line 21D are also supplied to line 26D for input into thermal cracker 30D. Furthermore, this embodiment includes hydrogen donor apparatus 40D including hydrotreater 45D to which light fraction product in line 39D is supplied and that produces treated hydrocarbon in line 41D. Treated hydrocarbon feed in line 41D is supplied to heater 43D and the heated, treated hydrocarbon feed is fed to further atmospheric fractionating tower 42D. Further atmospheric fractionating tower 42D produces further light atmospheric fractions in lines 44D and further atmospheric bottoms in line 46D. The further atmospheric bottoms in line 46D are then supplied to heater 47D and the heated, further atmospheric bottoms are supplied to further vacuum fractionating tower 48D that produces further light vacuum fractions in lines 50D, further heavier vacuum fractions in line 51D and further vacuum residue in line 52D. In this embodiment, further heavier vacuum fractions or hydrogen donor stream present in line 51D are fed via line 60D to line 26D for input into thermal cracker 30D.

Preferably, the ratio of the hydrocarbon feed present in line 26D to the amount of hydrogen donor stream present in line feed 60D is 0.25 to 4.

As far as the embodiment of the present invention is concerned, described with reference to Fig 6, numeral 10E designates another embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11E and the heated, heavy hydrocarbon feed is fed to atmospheric fractionating tower 12E. Atmospheric fractionating tower 12E

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produces lighter atmospheric fractions in line 14E, light fractions in line 15E and atmospheric bottoms in line 16E. The lighter atmospheric fractions in line 14E and light fractions in line 15E are combined and the combined product is supplied to hydrotreater 19E that produces a hydrotreated product. The atmospheric bottoms in line 16E are then supplied to heater 17E and the heated, atmospheric bottoms are supplied to vacuum fractionating tower 18E which produces light vacuum fractions in lines 20E, heavier vacuum fractions in line 21E and vacuum residue in line 22E. The vacuum residue in line 22E is then supplied to deasphalting unit 24E which produces deasphalted oil in line 26E and asphaltene in line 28E. Deasphalted oil in line 26E is supplied to thermal cracker 30E that produces thermally cracked product in line 32E that is recycled to inlet 13E of atmospheric fractionating tower 12E. Moreover, the light vacuum fractions in lines 20E, and heavier vacuum fractions in line 21E are supplied to line 39E. Portion of those fractions is supplied to further thermal cracker 35E for thermally cracking these vacuum fractions and a further thermally cracked product is produced in line 37E that is recycled to inlet 13E of atmospheric fractionating tower 12E. Furthermore, this embodiment includes a further hydrotreater 40E to which a further portion of fractions present in line 39E is supplied and that produces treated hydrocarbon feed in line 41E. In this embodiment, portion of treated hydrocarbon feed in line 41E is supplied via line 60E to line 26E for input into thermal cracker 30E. Preferably, the ratio of the deasphalted oil present in line 26E to the amount of treated hydrocarbon feed present in line 60E is 0.25 to 4. A further portion of the treated hydrocarbon feed in 41E is supplied to line 42E via line 62 for input into thermal cracker 35E.

Preferably, the ratio of the vacuum fractions present in line 42E to the amount of treated hydrocarbon feed present in line feed 62 is also 0.25 to 4.

Turning to the embodiment of the present invention described with reference to Fig. 7 similar apparatus to that described with reference to Fig. 6 is shown wherein numeral 10F designates a further embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11F and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12F. Atmospheric fractionating tower 12F produces lighter atmospheric fractions in line 14F, light fractions in line 15F and atmospheric bottoms in line 16F. The lighter atmospheric fractions in line 14F and light fractions in line 15F are combined and the combined product is supplied to hydrotreater 19F that produces a hydrotreated product. The

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atmospheric bottoms in line 16F are then supplied to heater 17F and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18F which produces light vacuum fractions in lines 20F, heavier vacuum fractions in line 21F and vacuum residue in line 22F. The vacuum residue in line 22F is then supplied to deasphalting unit 24F which produces deasphalted oil in line 26F and asphaltenes in line 28F. Deasphalted oil in line 26F is supplied to thermal cracker 30F that produces thermally cracked product in line 32F that is recycled to inlet 13F of atmospheric fractionating tower 12F. Moreover, the light vacuum fractions in lines 20F, and heavier vacuum fractions in line 21F are supplied to line 39F. Portion of these fractions is supplied to line 26F for input into thermal cracker 30F. Furthermore, this embodiment includes a further hydrotreater 40F to which a further portion of fractions present in line 39F is supplied and which produces treated hydrocarbon feed in line 60F. All of treated hydrocarbon feed in line 60F, in this embodiment, is supplied to line 26F for input into thermal cracker 30F.

Preferably, the ratio of the hydrocarbon feed present in line 26F to the amount of treated hydrocarbon feed present in line feed 60F is 0.25 to 4.

Numerical 10G in Fig. 8 designates an additional embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11G and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12G. Atmospheric fractionating tower 12G produces lighter atmospheric fractions in line 14G, light fractions in line 15G and atmospheric bottoms in line 16G. The lighter atmospheric fractions in line 14G and light fractions in line 15G are combined and the combined product is supplied to hydrotreater 19G that produces a hydrotreated product. The atmospheric bottoms in line 16G are then supplied to heater 17G and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18G that produces light vacuum fractions in lines 20G, heavier vacuum fractions in line 21G and vacuum residue in line 22G. The vacuum residue in line 22G is then supplied to solvent deasphalting unit 24G which produces deasphalted oil in line 26G and asphaltenes in line 28G. Deasphalted oil in line 26G is supplied to thermal cracker 30G that produces thermally cracked product in line 32G that is recycled to inlet 13G of atmospheric fractionating tower 12G. Moreover, the light vacuum fractions in lines 20G are supplied to line 39G. Portion of these fractions is supplied to further thermal cracker 35G for thermally cracking these vacuum fractions and a further thermally cracked product is produced in line 37G which is recycled to inlet 13G of atmospheric fractionating tower 12G. In addition, heavier

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vacuum fractions in line 21G are supplied to this portion of fractions supplied to further thermal cracker 35G. Furthermore, this embodiment includes a further hydrotreater 40G to which a further portion of fractions present in line 39G is supplied and which produces treated hydrocarbon feed in line 41G. In this embodiment, portion of treated hydrocarbon feed in line 41G is supplied via line 60G to line 26G for input into thermal cracker 30G. A further portion of the treated hydrocarbon feed in line 41G is supplied via line 62G to line 42G for input into further thermal cracker 35G. Preferably, the ratio of the vacuum fractions present in line 42G to the amount of treated hydrocarbon feed present in line feed 62G is 0.25 to 4. Also in this embodiment, portion for the hydrotreated product exiting hydrotreater 19G is supplied via line 64G to treated hydrocarbon feed in line 41G exiting further hydrotreater 40G. Consequently, portion of the hydrotreated product supplied to line 41G is supplied to line 26G for input into thermal cracker 30G while another portion of the hydrotreated product supplied to line 41G is supplied to further thermal cracker 35G.

Preferably, the ratio of the deasphalted oil present in line 26G to the amount of treated hydrocarbon feed present in line feed 60G is 0.25 to 4.

As far as the embodiment of the present invention described with reference to Fig. 9 is concerned, similar apparatus to that described with reference to Fig. 8 is shown wherein numeral 10H designates a further embodiment of apparatus for processing heavy hydrocarbons in accordance with the present invention. In this embodiment, heavy hydrocarbon feed is supplied to heater 11H and the heated heavy hydrocarbon feed is fed to atmospheric fractionating tower 12H. Atmospheric fractionating tower 12H produces lighter atmospheric fractions in line 14H, light fractions in line 15H and atmospheric bottoms in line 16H. The lighter atmospheric fractions in line 14H and light fractions in line 15H are combined and the combined product is supplied to hydrotreater 19H that produces a hydrotreated product. The atmospheric bottoms in line 16H are then supplied to heater 17H and the heated atmospheric bottoms are supplied to vacuum fractionating tower 18H which produces light vacuum fractions in lines 20H, heavier vacuum fractions in line 21H and vacuum residue in line 22H. The vacuum residue in line 22H is then supplied to solvent deasphalting unit 24H which produces deasphalted oil in line 26H and asphaltenes in line 28H. Deasphalted oil in line 26H is supplied to thermal cracker 30H that produces thermally cracked product in line 32H that is recycled to inlet 13H of atmospheric fractionating tower 12H. Moreover, the light vacuum fractions in lines 20H are supplied to line 39H for input into further hydrotreater 40H which

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produces treated hydrocarbon feed in line 41H that is supplied via line 60H to line 26H for input into thermal cracker 30H. Heavier vacuum fractions in line 21H are also supplied to line 26H for input into thermal cracker 30H. In this embodiment, portion for the hydrotreated product exiting hydrotreater 19H is supplied via line 64H to treated hydrocarbon feed in line 41H exiting further hydrotreater 40H. Consequently, the portion of the hydrotreated product supplied to line 41H is supplied to line 26H for input into thermal cracker 30H.

Preferably, the ratio of the hydrocarbon feed present in line 26H to the amount of treated hydrocarbon feed present in line feed 60H is 0.25 to 4.

The present invention permits the efficient control of the final boiling point of the product stream. This has importance since the value of the upgraded product produced in accordance with the present invention changes for each specific refinery configuration. Refineries are sensitive to the final boiling point of this upgraded product and material that has high value for one may be valued at the value of vacuum residue by another. Thus, the value of the product or synthetic crude produced in accordance with the present invention and supplied to the refinery can be different for a different balance of the different fractions produced. Refineries are differentiated one from another by the products and fractions they are willing to accept. Consequently, sometimes, the value of a product in the boiling point range between 650 - 1050°F is low even if its quality is high. Here, refineries may prefer different divisions of boiling point ranges of the improved products in accordance with the processing units or apparatus downstream. As a result, if e.g. a refinery is the client of the product or the user of the process, there is an advantage of flexibility of the final boiling point in general and in the actual balance between the vacuum gas oil and the atmospheric product fractions. Furthermore, often a diluent needs to be added to the crude oil in order to meet the pipeline specifications for conveying the heavy oil. Thus, the present invention permits conversion of part of the crude oil into diluent that can be used in the transportation of more viscous oil.

Moreover, as far as combustion turbines are concerned, it is important to control the viscosity and density of the product thus permitting substantially avoiding potential risks from occurring in the fuel system and injectors of the turbine.

In addition, it should be noted that supply means or lines mentioned in this specification refer to suitable conduits, etc.

Furthermore, it should be pointed out that the present invention includes as well the method for operating the

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apparatus disclosed with reference to the above-described figures

It is believed that the advantages and improved results furnished by the method and apparatus of the present invention are apparent from the foregoing description of the invention. Various changes and modifications may be made without departing from the spirit and scope of the invention as described in the claims that follow.

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WHAT IS CLAIMED IS:

- 1 Apparatus of processing heavy hydrocarbon feed comprising
 - a) a heater for heating said heavy hydrocarbon feed
 - b) an atmospheric fractionating tower for fractionating the heated heavy hydrocarbon feed fed to the inlet of the atmospheric fractionating tower producing light atmospheric fractions and atmospheric bottoms;
 - c) a further heater for heating said atmospheric bottoms and producing heated atmospheric bottoms;
 - d) a vacuum fractionating tower for fractionating said heated atmospheric bottoms and producing light vacuum fractions and vacuum residue;
 - e) a solvent deasphalting (SDA) unit for producing deasphalted oil (DAO) and asphaltenes from said vacuum residue
 - f) a thermal cracker for thermally cracking said deasphalted oil and producing a thermally cracked product which is recycled to the inlet of said atmospheric fractionating tower and
 - g) a further thermal cracker for thermally cracking said light vacuum fractions for producing a further thermally cracked product which is recycled to the inlet of said atmospheric fractionating tower
- 2 Apparatus according to claim 1 including means for supplying only the heavy portion of said light vacuum fractions to said further thermal cracker
- 3 Apparatus according to claim 2 including a hydrogen donor system for processing the lighter portion of said light vacuum fractions and producing a hydrogen donor stream, said hydrogen donor system including:
 - a) a hydrotreater for producing a treated hydrocarbon feed from said the lighter portion of said light vacuum fractions
 - b) a still further heater for producing a heated, treated hydrocarbon stream,
 - c) a further atmospheric fractionating tower for fractionating said heated treated hydrocarbon stream for producing further light atmospheric fractions and further atmospheric bottoms,
 - d) an additional heater for heating said further atmospheric bottoms and producing heated, further atmospheric bottoms and
 - e) a further vacuum fractionating tower for fractionating said heated, further atmospheric bottoms and

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producing further lighter vacuum fractions and further vacuum residue such that the heavier portion of said further lighter vacuum fractions or hydrogen donor stream is supplied to said thermal cracker

4 A method for processing heavy hydrocarbon comprising the steps of

- a) heating said heavy hydrocarbon;
- b) fractionating the heated heavy hydrocarbon feed in an atmospheric fractionating tower for producing light atmospheric fractions and atmospheric bottoms;
- c) heating said atmospheric bottoms for producing heated atmospheric bottoms;
- d) fractionating said heated atmospheric bottoms in a vacuum fractionating tower for producing lighter vacuum fractions and vacuum residue;
- e) solvent deasphalting said vacuum residue in a solvent deasphalting (SDA) for producing deasphalted oil (DAO) and asphaltenes
- f) thermally cracking said deasphalted oil in a thermal cracker for producing a thermally cracked product which is recycled to the inlet of said atmospheric fractionating tower, and
- g) thermally cracking said lighter vacuum fractions for producing a further thermally cracked product that is recycled to said atmospheric fractionating tower

5 A method according to claim 4 providing a further, separate thermal cracker for thermally cracking said lighter vacuum fractions

6 A method according to claim 5 including providing means for supplying only the heavy portion of said light vacuum fractions to said further thermal cracker

7 A method according to claim 4 wherein said lighter vacuum fractions are thermally cracked in the same thermal cracker in which said deasphalted oil is thermally cracked

8 A method according to claim 4 including:

- a) providing a hydrotreater for processing said light atmospheric and the lighter portion of said light vacuum fractions and producing a treated, hydrocarbon stream,
- b) heating said treated hydrocarbon stream for producing a heated, treated, hydrocarbon stream;
- c) fractionating said heated, treated, hydrocarbon stream using a further atmospheric fractionating tower for producing further light atmospheric fractions and further atmospheric bottoms,
- d) heating said further atmospheric bottoms for producing heated further atmospheric bottoms,

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e) fractionating said heated, further atmospheric bottoms using a further vacuum fractionating tower for producing further lighter vacuum fractions and further vacuum residue, and

f) thermally cracking the heavier portion of said further lighter vacuum fractions

9 A method according to claim 7 including

a) providing a hydrotreater for processing said light atmospheric and the lighter portion of said light vacuum fractions and producing a treated, hydrocarbon stream,

b) heating said treated hydrocarbon stream for producing a heated, treated, hydrocarbon stream;

c) fractionating said heated, treated, hydrocarbon stream using a further atmospheric fractionating tower for producing further light atmospheric fractions and further atmospheric bottoms,

d) heating said further atmospheric bottoms producing heated further atmospheric bottoms,

e) fractionating said heated, further atmospheric bottoms using a further vacuum fractionating tower for producing further lighter vacuum fractions and further vacuum residue; and

f) supplying the heavier portion or hydrogen donor stream of said further lighter vacuum fractions to said thermal cracker

10 Apparatus according to claim 1 including

a) a hydrotreater for processing the lighter portion of said light vacuum fractions and producing a treated, hydrocarbon stream

q) a further heater for heating said treated, hydrocarbon stream for producing a heated, treated, hydrocarbon stream.

b) a further atmospheric fractionating column for producing from said heated, treated, hydrocarbon stream further light atmospheric fractions and further atmospheric bottoms;

c) a still further heater for heating said further atmospheric bottoms producing heated, further atmospheric bottoms; and

d) a further vacuum fractionating column for producing further lighter vacuum fractions and further vacuum residue such that the heavier portion of said further light vacuum fractions is supplied together with said deasphalted oil to said thermal cracker

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ABSTRACT

Apparatus for processing a heavy hydrocarbon feed, in accordance with the present invention, includes firstly a heater for heating the heavy hydrocarbon feed. The heated, heavy hydrocarbon feed produced is fed to an atmospheric fractionating tower for fractionating the heated heavy hydrocarbon feed fed to the inlet of the atmospheric fractionating tower producing light atmospheric fractions and atmospheric bottoms. In addition, the apparatus includes a vacuum fractionating tower for fractionating heated atmospheric bottoms heated by a further heater and producing lighter vacuum fractions and vacuum residue. Furthermore, the apparatus includes a solvent deasphalting (SDA) unit for producing deasphalted oil (DAO) and asphaltenes from the vacuum residue as well as a thermal cracker for thermally cracking the deasphalted oil and producing a thermally cracked product which is recycled to the inlet of said atmospheric fractionating tower. Moreover, the apparatus includes a further thermal cracker for thermally cracking the lighter vacuum fractions for producing a further thermally cracked product that is recycled to said atmospheric fractionating tower.

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DECLARATION FOR PATENT APPLICATION	Attorney Docket P-15149 Page 1 of 2
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As a below-named inventor(s) I/we hereby declare that

My/Our residence(s), post office address(es) and citizenship(s) is/are as stated below next to my/our name(s)

I/We believe I/we am/are the original inventor, first and sole (if only one name is listed below) or the original, first and joint inventors (if plural names are listed below) of the subject matter which is claimed, and for which a patent is sought on the invention entitled

METHOD OF AND APPARATUS FOR PROCESSING HEAVY HYDROCARBON FEEDS

the specification of which (check one)

☒ is attached hereto

☐ was filed on _____, as Serial No _____,

and was amended on _____ (if applicable)

We hereby state that we have reviewed and understand the contents of the above-identified specification including the claims as amended by any amendment referred to above

We acknowledge the duty to disclose information which is material to the patentability of this application as defined by 37 CFR § 1.56

We hereby claim foreign priority benefits under 35 U.S.C. § 119 of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed

Prior Foreign Applications

(Application No)	(Country)	(Day/Month/Year Filed)	Priority Claimed	
			()	()
			Yes	No
(Application No)	(Country)	(Day/Month/Year Filed)	()	()
			Yes	No
(Application No)	(Country)	(Day/Month/Year Filed)	()	()
			Yes	No

We hereby appoint Gary M. Nath, Reg. No. 26,965; Harold L. Novick, Reg. No. 26,011; Suet H. Chong, Reg. No. 38,104; Todd L. Juneau, Reg. No. 40,669; Patricia M. Drost, Reg. No. 29,790; Lee C. Reiman, Reg. No. 41,827; Jerald L. Meyer, Reg. No. 41,194; Joshua B. Goldberg, Reg. No. 44,126; David Milligan, Reg. No. 42,893; David R. Murphy, Reg. No. 22,751; Paul A. Sacher, Reg. No. 43,418; Gregory B. Kang, Reg. No. P-45 273 and Robert G. Lev, Reg. No. 30,280, as my attorneys to prosecute this application and transact all business in the U.S. Patent and Trademark Office connected therewith

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NATH & ASSOCIATES
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Washington, D.C. 20005 U.S.A.

We hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by 35 U.S.C. § 112, first paragraph, I/we acknowledge the duty to disclose material information as defined in 37 CFR § 1.56 which occurred between the filing date of the prior application and the national or PCT international filing date of this application

(U.S. Application Serial No)	(U.S. Filing Date)	(Status--patented, pending, abandoned)
(U.S. Application Serial No)	(U.S. Filing Date)	(Status--patented, pending, abandoned)

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DECLARATION FOR PATENT APPLICATION

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Page 2 of 2

We hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true and further that these statements are made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment or both, under 18 U S C § 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon

Full name of sole or first inventor Yoram BRONICKI

Inventor's Signature _____ Date _____

Residence 23 Karem Kavanat Street, Rehovot, Israel

Country of Citizenship Israel

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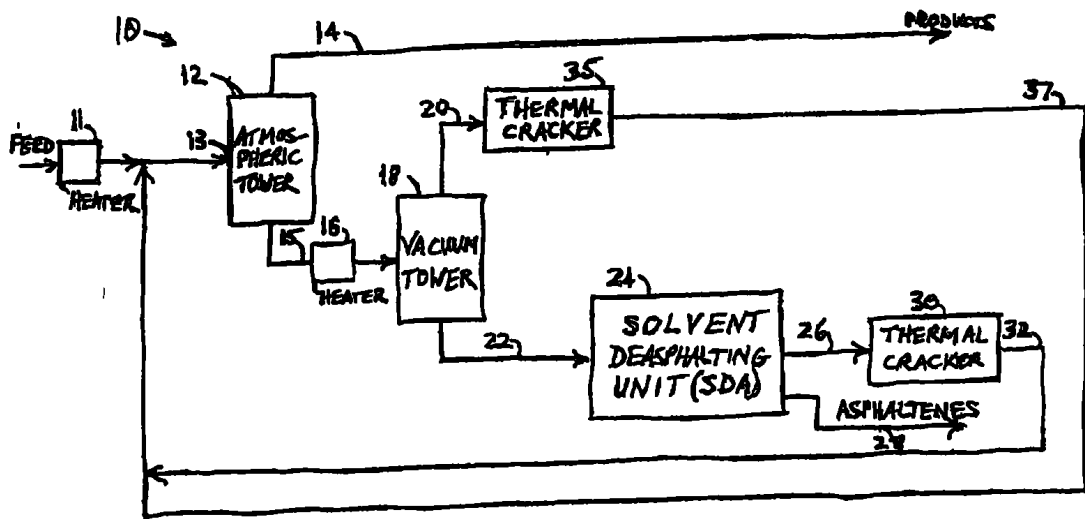


FIG 1

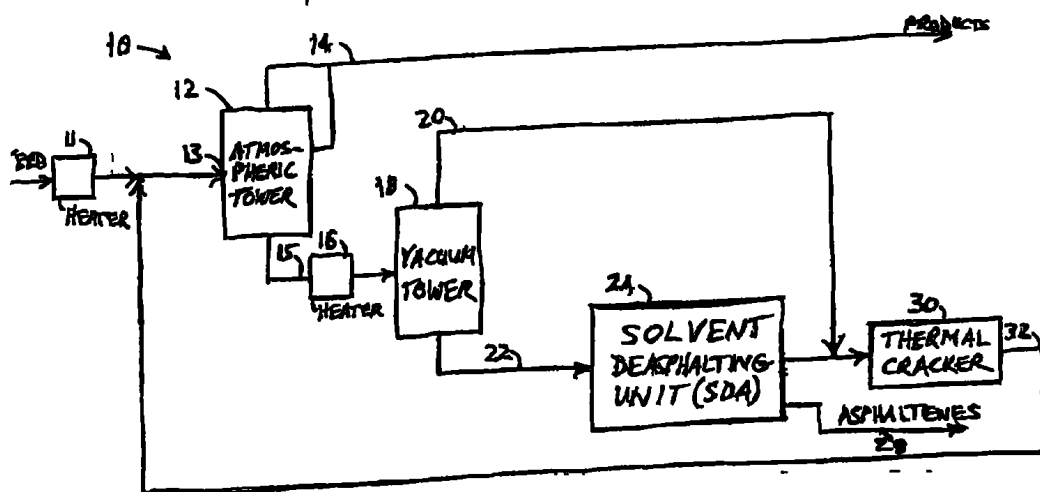


FIG 1A

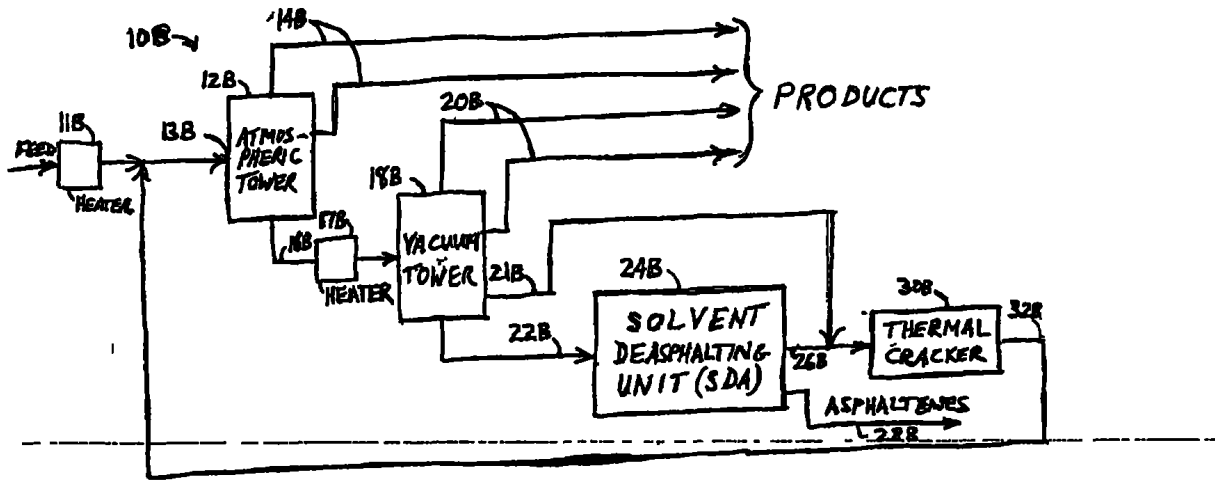
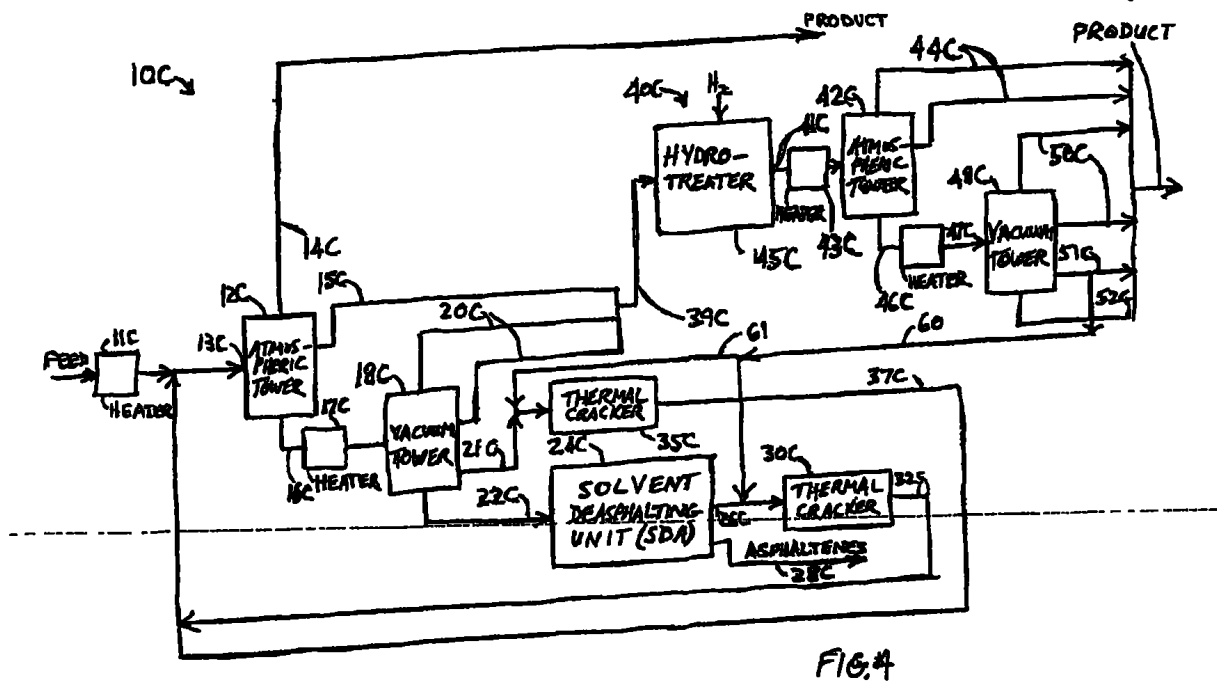
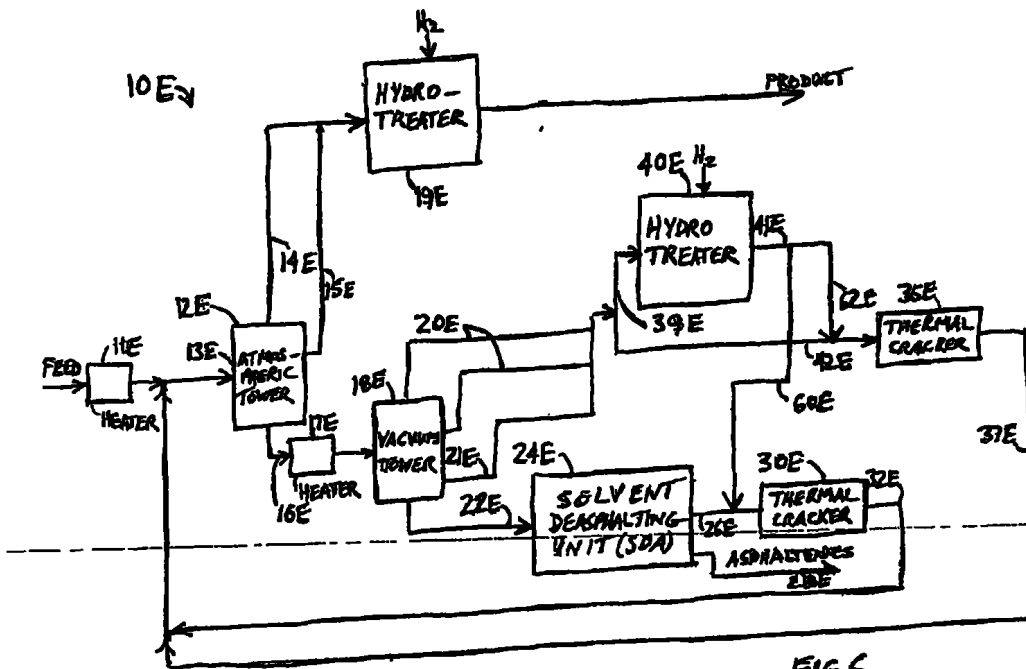


FIG 3

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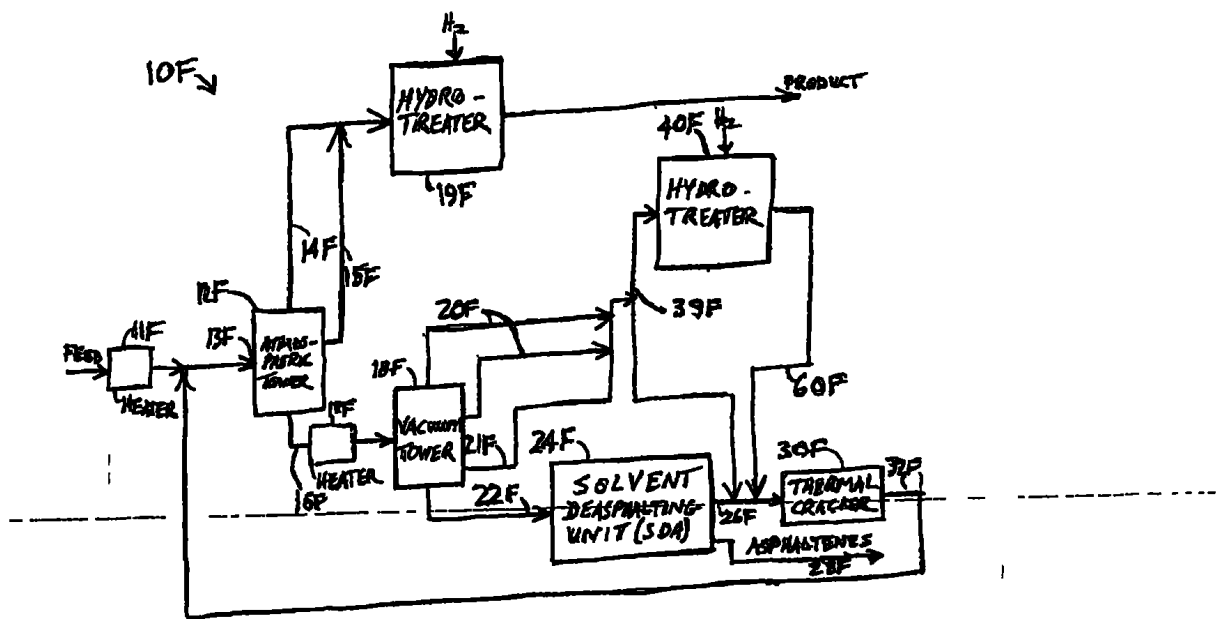
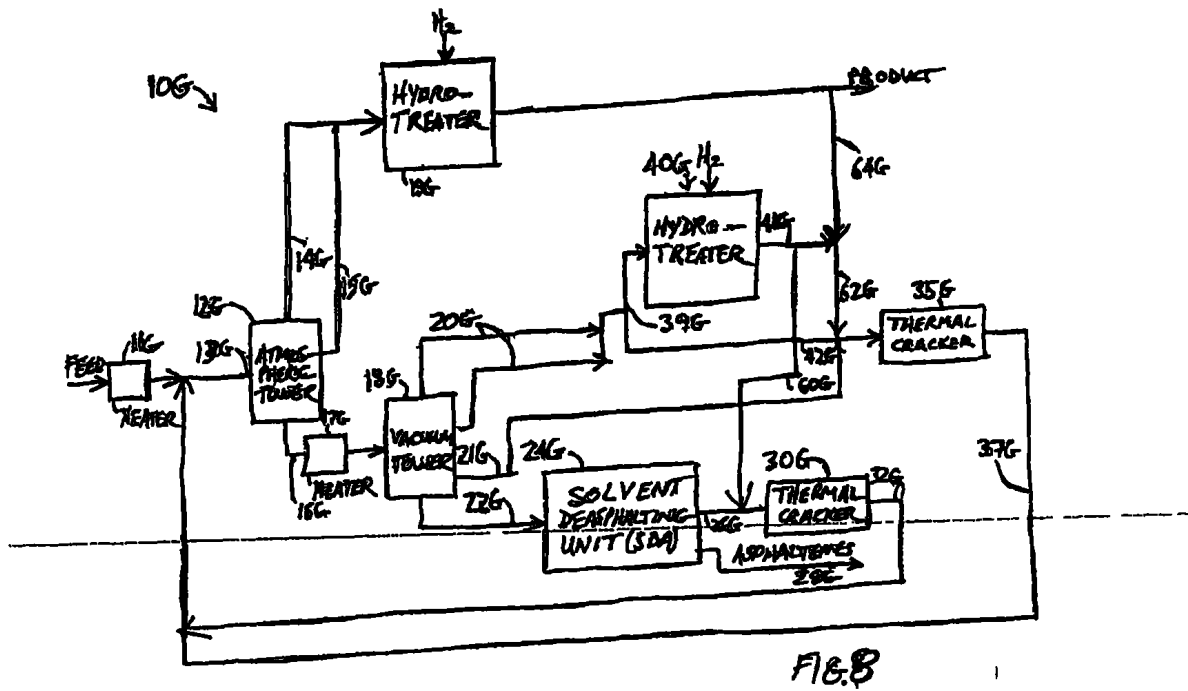


FIG 7



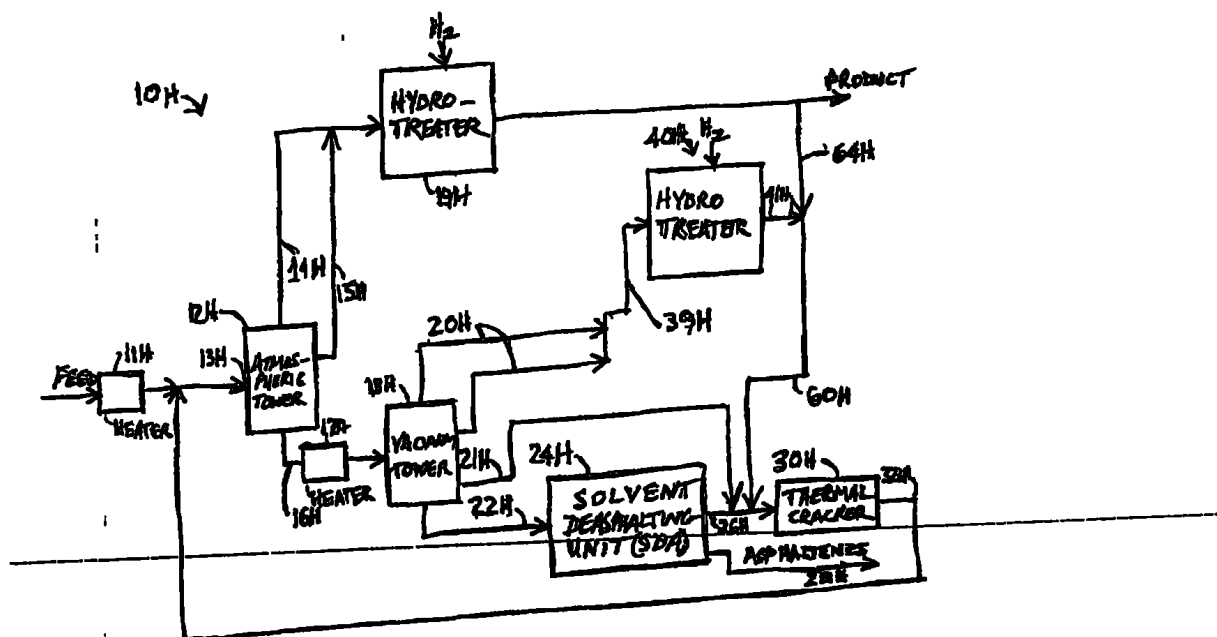
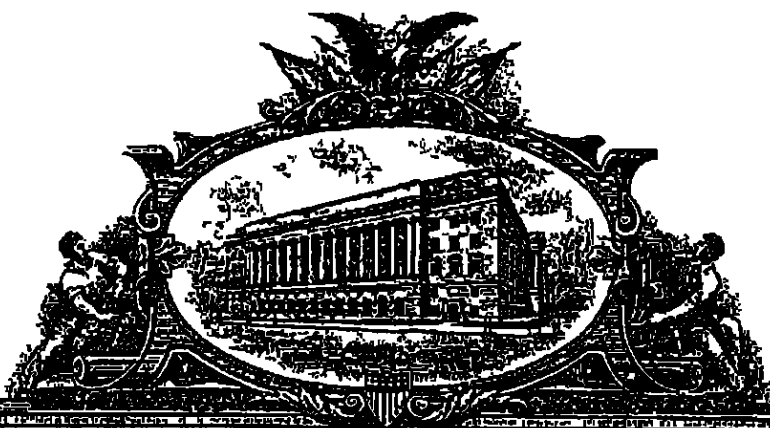


FIG 9

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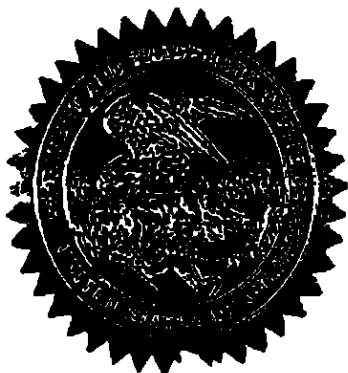
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20 de octubre de 2000

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CUMPLEN LOS REQUISITOS PARA OTORGARLE UNA FECHA DE
PRESENTACION BAJO 35 USC 111**

NÚMERO DE SOLICITUD	09/431 159
FECHA DE PRESENTACIÓN	01 de noviembre de 1999



**Por la Autoridad del
COMISARIO DE PATENTES Y MARCAS**

N WILLIAMS

Oficial certificador

REIVINDICACIONES

Se reivindica lo siguiente

1 Un aparato para procesar un suministro de hidrocarburo pesado que comprende

a) un calentador para calentar el suministro de hidrocarburo pesado,

b) una torre de fraccionamiento atmosférico para fraccionar el suministro de hidrocarburo pesado calentado hacia la entrada de la torre de fraccionamiento atmosférico lo que produce fracciones atmosféricas,

c) otro calentador para calentar los residuos atmosféricos y producir residuos atmosféricos calentados,

d) una torre de fraccionamiento al vacío para fraccionar los residuos atmosféricos calentados y producir fracciones por vacío livianas y residuos por vacío,

e) una unidad de desasfaltado (SDA) para producir crudo desasfaltado (DAO) y asfaltenos a partir del residuo por vacío,

f) una unidad de cracking térmica para producir térmicamente el cracking del crudo desasfaltado y producir un producto de cracking térmico que se recicla hacia la entrada de la torre de fraccionamiento atmosférico, y

g) otra unidad de cracking para producir térmicamente el cracking de las fracciones por vacío livianas para producir otro producto de cracking térmico que se recicla hacia la entrada de la torre de fraccionamiento atmosférico

2 El aparato de acuerdo con la reivindicación 1 que incluye medios para suministrar solamente la porción pesada de las fracciones por vacío livianas a la otra unidad de cracking térmica

3 El aparato de acuerdo con la reivindicación 2 que incluye un sistema donante de hidrógeno para procesar la porción más liviana de las fracciones por vacío livianas y producir una corriente donante de hidrógeno, el sistema donante de hidrógeno incluyendo lo siguiente

a) un hidrotratador para producir un suministro de hidrocarburo tratado a partir de la porción más liviana de las fracciones por vacío livianas,

b) otro calentador para producir una corriente de hidrocarburo tratado calentado,

c) otra torre de fraccionamiento atmosférico para fraccionar la corriente de hidrocarburo tratado calentado para producir otras fracciones atmosféricas livianas y otros residuos atmosféricos,

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d) un calentador adicional para calentar los otros residuos atmosféricos y residuos atmosféricos calentados adicionales, y

e) otra torre de fraccionamiento por vacío para fraccionar los residuos atmosféricos calentados adicionales y producir otras fracciones por vacío más livianas y otros residuos por vacío de manera tal que la porción más pesada de las otras fracciones por vacío más livianas o corriente donante de hidrógeno se suministre a la unidad de cracking térmica

4 Un método para procesar hidrocarburos pesados que comprende los siguientes pasos

a) calentar el hidrocarburo pesado,

b) fraccionar el suministro de hidrocarburo pesado calentado en una torre de fraccionamiento atmosférico para producir fracciones atmosféricas livianas y residuos atmosféricos,

c) calentar los residuos atmosféricos para producir residuos atmosféricos calentados,

d) fraccionar los residuos atmosféricos calentados en una torre de fraccionamiento al vacío para producir fracciones por vacío más livianas y residuos por vacío,

e) desasfaltar por solvente el residuo por vacío en una unidad de desasfaltado por solvente (SDA) para producir crudo desasfaltado (DAO) y asfaltenos,

f) someter térmicamente a cracking el crudo desasfaltado en una unidad de cracking térmica para producir un producto de cracking térmico que se recicla hacia la entrada de la torre de fraccionamiento atmosférico, y

g) someter térmicamente a cracking las fracciones por vacío más livianas para producir otro producto de cracking térmico que se recicla hacia la torre de fraccionamiento atmosférico

5 Un método de acuerdo con la reivindicación 4 que proporciona otra unidad de cracking térmica separada para someter térmicamente a cracking a las fracciones por vacío más livianas

6 Un método de acuerdo con la reivindicación 5 que incluye proporcionar medios para suministrar solamente la porción pesada de las fracciones por vacío livianas a la otra unidad de cracking térmica

7 Un método de acuerdo con la reivindicación 4 en donde las fracciones por vacío más livianas se someten térmicamente a cracking en la misma unidad de cracking térmico en la que se somete a cracking térmico al crudo desasfaltado

8 Un método de acuerdo con la reivindicación 4 que incluye lo siguiente

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- a) proporcionar un hidrotratador para procesar la porción atmosférica liviana y la porción más liviana de las fracciones por vacío livianas y producir una corriente de hidrocarburo tratado,
- b) calentar la corriente de hidrocarburo tratado para producir una corriente de hidrocarburo tratada calentada
- c) fraccionar la corriente de hidrocarburo tratada calentada utilizando otra torre de fraccionamiento atmosférica para producir otras fracciones atmosféricas livianas y otros residuos atmosféricos,
- d) calentar los otros residuos atmosféricos para producir residuos atmosféricos calentados adicionales,
- e) fraccionar los residuos atmosféricos calentados adicionales utilizando otra torre fraccionadora por vacío para producir otras fracciones por vacío más livianas y otros residuos por vacío, y
- f) someter térmicamente a cracking la porción más pesada de las fracciones por vacío más livianas adicionales

9 Un método de acuerdo con la reivindicación 7 que incluye lo siguiente

- a) proporcionar un hidrotratador para procesar la porción atmosférica liviana y la porción más liviana de las fracciones

por vacío livianas y producir una corriente de hidrocarburo tratada

b) calentar la corriente de hidrocarburo tratada para producir una corriente de hidrocarburo tratada calentada,

c) fraccionar la corriente de hidrocarburo tratada calentada utilizando otra torre de fraccionamiento atmosférico para producir fracciones atmosféricas livianas adicionales y otros residuos atmosféricos,

d) calentar los residuos atmosféricos adicionales que producen otros residuos atmosféricos calentados

e) fraccionar los otros residuos atmosféricos calentados utilizando otra torre de fraccionamiento por vacío para producir otras fracciones por vacío más livianas y otros residuos por vacío, y

f) suministrar la porción más pesada o corriente donante de hidrógeno de las otras fracciones por vacío más livianas a la unidad de cracking térmica

10 El aparato de acuerdo con la reivindicación 1 que incluye lo siguiente

a) un hidrotratador para procesar la porción más liviana de las fracciones por vacío livianas y producir una corriente de hidrocarburo tratada

- q) otro calentador para calentar la corriente de hidrocarburo tratada para producir una corriente de hidrocarburo tratada calentada
- b) otra columna de fraccionamiento atmosférico para producir a partir de la corriente de hidrocarburo tratada calentada otras fracciones atmosféricas livianas y otros residuos atmosféricos,
- c) otro calentador para calentar otros residuos atmosféricos que producen residuos atmosféricos calentados, y
- d) otra columna de fraccionamiento por vacío para producir otras fracciones por vacío más livianas y otros residuos por vacío de manera tal que la porción más pesada de las otras fracciones por vacío livianas se suministre junto con el crudo desasfaltado a la unidad de cracking térmico