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SUPERINDUSTRIA Y COMERCIO

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Dependencia: 2020 DIVISION DE NUEVAS CREACIONES

Señor
SUPERINTENDENTE DE INDUSTRIA Y COMERCIO
DIVISIÓN DE NUEVAS CREACIONES
E. S. D.

REF: Expediente No.: **04-010.426**
Patente de Invención: **"LODO CONDUCTOR BASADO ELÉCTRICAMENTE EN ACEITE"**
Titular: **HALLIBURTON ENERGY SERVICES, INC.**

Publicada en la Gaceta de la Propiedad Industrial No. 555 de 31 de agosto de 2.005

SOLICITUD DE EXAMEN DE PATENTABILIDAD

HUMBERTO RUBIO CAMACHO, mayor de edad, domiciliado en Bogotá, D.C., identificado con la cédula de ciudadanía número 17.192.062 de Bogotá, abogado Titulado con Tarjeta Profesional No. 50.007 del Consejo Superior de la Judicatura, actuando en carácter de APODERADO de la Sociedad **HALLIBURTON ENERGY SERVICES, INC.**; domiciliada en Duncan, Oklahoma, Estados Unidos de América; respetuosamente solicito a esa Dependencia:

- 1.- De conformidad con lo establecido en el Artículo 44 de la Decisión 486 de la Comisión de la Comunidad Andina y estando dentro del termino legal de seis meses contados desde la fecha de publicación en la Gaceta No. 555 de 31 de agosto de 2.005, de la solicitud de la patente de la referencia, solicito se sirvan proceder a efectuar el examen de patentabilidad de la Invención.
- 2.- Para que la presente petición sea viable, estoy anexando el siguiente documento:
 - 2.1. Recibo de pago No. 05-76,781 de 05 de octubre de 2.005; por un valor de \$ 186.000,00, de acuerdo con la Resolución No. 31980 de 24 de diciembre de 2.004.
- 3.- Por lo anterior solicito se continúe con el trámite correspondiente.

Del Señor Superintendente,


HUMBERTO RUBIO CAMACHO
C.C. 17.192.062 de Bogotá
T.P. 50.007 Consejo Superior
de la Judicatura.
COD. 4134

04/448-013/pi

cpfm.-

SUPERINTENDENCIA DE INDUSTRIA Y COMERCIO

NIT : 800176089-2

EXAMEN DE PATENTABILIDAD
PATENTE DE INVENCION: LODO
CONDUCTOR BASADO ELÉCTRICAMENTE
EN ACEITE

RECIBO OFICIAL DE CAJA : 05 - 76,781
FECHA : OCTUBRE 5 DE 2005

SUPERINTENDENCIA Y COMERCIO
Radicación : 84610426 000000003 Folios: 2
Fecha (AMD): 2005-10-06 14:23:59
Trámite : 011 PCT-PATENT 379 FASE MARC 538 PETICION
Dependencia: 2020 DIVISION DE NUEVAS CREACIONES

***** C O N S I G N A C I O N *****

DEPOSITANTE	TIPO PAGO	BANCO	CUENTA	No. PAGO	FECHA PGO	Vr. PAGO
HUMBERTO RUBIO ABOGADOS	LCONSIGNACION	BANCO POPULAR	050-00110-6	41400445	05/10/2005	10,313,000.00

***** C O N C E P T O *****

CANT.	RENTISTICO	CONCEPTO	TOTAL CONCEPTO
1	50005-01-01 SOLICITUDES	114 PTC CAP-II EXAMEN DE PATENTIBILID	186,000.00
TOTAL :			\$ 186,000.00

SON: CIENTO OCHENTA Y SEIS MIL PESOS

RESPONSABLE : _____

RECIBO DE CAJA APLICADO AL EXPEDIENTE No. _____

DIVISION DE NUEVAS CREACIONES

RADICACIÓN EXPEDIENTE No 04-10426

EL EXTRACTO DE LA PRESENTE SOLICITUD DE PATENTE DE INVENCION

– PCT, FUE PUBLICADO EN LA GACETA DE PROPIEDAD INDUSTRIAL No

555, DE FECHA 31 DE AGOSTO DE 2005, EL TERMINO HABIL SEÑALADO

POR LA LEY EXPIRA EL 28 DE NOVIEMBRE DE 2005

NOTA Dentro del plazo de los seis (6) meses siguientes a partir de la fecha de publicación en la gaceta de Propiedad Industrial, debera solicitar y cancelar el examen de patentabilidad so pena de que la solicitud caiga en abandono, de acuerdo con lo establecido en el Artículo 44 de la Decisión 486/2000

SE PRESENTARON OPOSICIONES POR PARTE DE TERCEROS

SI

NO **X**

2,739,120
Patented Mar 20, 1956

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2,729,128

ELECTRICALLY CONDUCTIVE DRILLING FLUIDS

Paul W. Fletcher, Whittier, Calif., assigned to Union Oil Company of California, Los Angeles, Calif., a corporation of California.

No Drawing. Application May 18, 1952,
Serial No. 287,399

18 Clinton (CL 252-49)

This invention relates to oil-bore drilling fluids, and in particular concerns oil-bore drilling fluids which are electrically conductive. It further relates to means for rendering a nonconductive oil-bore drilling fluid electrically conductive, and to means for conducting electric well logging operations.

In drilling operations, the drill pipe by means of rotary drilling tools, a hollow drill pipe having a bit attached to the lower end, is lowered and extended downwardly through the well bore and is rotated while the bit is pressed against the working face of the rock to be drilled. The rotation of the drill pipe causes the rotation of the bit and the bit of the hole. The action of the rotating bit grinds away the rock of the hole. The drilling progresses. During the drilling a fluid body known as a drilling fluid is continuously circulated down through the drill pipe, around the bit and against the working face of the hole, and then back up the annular space between the drill pipe and the wall of the hole. The drilling fluid serves a number of purposes. It keeps the drill pipe cool and lubricates the drill bit, suspending and removing the rock particles from the hole, preventing the flow of liquids from the formations traversed by the bore into the same by carrying a certain percentage on each formation, and fulfilling other purposes.

In instances where the underground formations traversed and/or penetrated by the bore contain materials such as hydrocarbon clays which swell and/or disintegrate in the presence of water it has become customary to employ a drilling fluid which is derived from oil at water in the form of an emulsion. This emulsion is usually a 5:1 fluids which contain less than 20% water. The water is added in order to preclude or minimize the introduction of water into the bore by means of the drilling fluid. The emulsion is usually a "water-in-oil" fluids since they are almost invariably comprised of water dispersed in an oil or suspended therein. Some properties of various agents adopted to impart the requisite physical properties to the emulsion are shown. The most important of such agents are: weighting agents, which are used to impart the emulsion with sufficient density to maintain the bore hole; and thickeners adapted to increase the apparent viscosity of the emulsion and thus increase the hydrostatic head provided by the emulsion fluid within the bore; wall-inhibiting agents, which are used to inhibit the bore hole from being eroded to cost; and dispersants, which are used to disperse the solids in the slurry, thus preventing escape of the drilling fluid into permeable formations, and dispersing agents, which serve to maintain solid components of the fluid uniformly dispersed therein.

Among the various methods for investigating and determining the nature of the subsurface formations traversed by a well bore, i. e., well logging, those involving the measurement of one or more of the electrical characteristics of such formations enjoy wide application.

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Most of such studies require that the bore have less than a fluid with a liquid capable of conducting relatively low leakage electric currents, and it is hence highly desirable that the drilling fluid employed in drilling the well be adapted for such use, i. e., the drilling fluid should have relatively good electrical conductivity. In general, however, the drilling fluids used are not sufficiently conductive to permit their use during the drilling operation, and to depth then for use during the logging operation, and this deficiency has greatly restricted their general applicability despite their other highly desirable properties and characteristics. Typically oil-based drilling fluids have electrical resistivities of the order of 1×10^{10} ohm-cm, which is high to permit their use in the logging operation, but is high to prevent their use in electric logging operations with the exception of those cases that the bore hole fluid have a resistivity not greater than about 50×10^{10} ohm-cm, and preferably below about

[illegible]

It is shown which contains synthetic oil-soluble drilling fluids, and a process which contains a solution of alkali-metal and alkaline-earth metal soaps. Heat-treated soda acids can be rendered curative by incorporating in the field curatively controlled amounts of sodium silicate. However in order to gain the benefits of the use of sodium silicate in this manner it is necessary that the use of alkaline-earth metal soap employed and the water content of the field be likewise very carefully controlled. For best results it is necessary to employ a homogeneous to insure adequate dispersion of the sodium silicate in the form fluid. As will be apparent to those skilled in the art, such careful control of proportions and amounts

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vertical mixing procedure is very difficult to achieve under field conditions where inadequate raising facilities render almost impossible the preparation of completely uniform emulsions and where the fluid is continuously

It is accordingly an object of the present invention to provide improved 7 base drill 3 fl id a stabl for use electric well-lining operations.

Another object is to provide oil-base drilling fluids having good electrical conductivity.

A further object is to provide a composition of matter adapted to imparting the property of electrical conductivity to all-base drilling fluids which are normally sub-

A still further object is to provide an improved method for conducting electric well logging operations.

Other objects will be apparent from the following detailed description of the invention and various advantages not specifically referred to herein will occur to those skilled in the art upon employment of the invention in practice.

I have now found that the above noted relative objects may be realized by transposition an electrolytic cell with an oil-base electrolyte. In this case, particularly, I have found that the efficient electrolysis of oil-base drilling fluids may be reduced to values within the range required for electric logging operations by adding to the fluid relatively small amounts (about 1%) of a substance such as sodium acetate, sodium chloride, or acrylate, or curable types of surface active agents. Such substances increase the normal water content of the oil-base fluid will be sufficient to dissolve the added electrolyte, but in other cases a small amount of water is added for this purpose. In order to remain in the soluble range, the amount of electrolyte added must be limited. In addition, the water content should be maintained below about 10, preferably between about 4 and 8 percent by weight.

The water-soluble formable metallic compounds as stated are employed in accordance with the invention to form a part electrical conductivity to oil base drilling fluid and are used for the most part water-soluble salts of the alkali, alkaline-earth metals and alkali-metal hydroxides. In accordance with customary nomenclature the sum of such radicals is herein included within the term "alkali-metal." Water-soluble salts of the heavy metals are not inoperable insofar as initially imparting electrical conductivity to the fluid is concerned, but because of the tendency of

the field is concerned, but because of the tendency of such salts to hydrolyze in aqueous solution to form insoluble hydroxides, their effect on electrical conductivity is not usually permanent. Specific examples of the foregoing class of water-soluble ionizable metal compounds employed in practice of the invention include the hydroxides of sodium, potassium and lithium, sodium chloride, barium chloride, cesarium iodide, ammonium chloride.

[illegible]

acids. The alkali-metal hydrides, alkoxides, and phosphates are particularly preferred.

salts are particularly preferred. These compounds are capable of interacting with the microheterogeneous electrolytes in accordance with the convention are of the non-ionic type, i.e., they are compounds in which the polar and non-polar groups are separated by a hydrophobic barrier and are not substantially capable of ionization. This type of compound forms a well-recognized class of surface active agents (see Berlin, "Introduction to Emulsions," Chem. and Technol. Publishing Co., Moscow, 1966). This class includes such compounds as there are members of the class consisting of (1) partial esters of polyhydric alcohol with long-chain carboxylic acids and (2) esters of hydroxyalkyl esters of polyhydric alcohols with long-chain carboxylic acids. The term "long-chain carboxylic acids" refers to aliphatic carboxylic acids containing at least 12, preferably 12 to 18 carbon atoms. The term "polyhydric alcohol" refers to aliphatic compounds containing at least two hydroxyl groups. As a rule, the surface active compounds of this class of non-ionic surface active agents comprise polyhydric ester alcohols such as are obtained by con-

[illegible][illegible]

Many further examples of non ionic surface active agents, together with their respective trade names and manufacturers, are listed in *Industrial and Engineering Chemistry* vol. 35 pp. 107-117 and 126-130 (1943). A preferred group of such agents comprises the hydroxy-polyoxyethylene ethers of long-chain fatty acid partial esters of sorbitan which are available commercially under

1 Esterification of one or more, but not all of the hydroxy groups of the sorbita molecule with a long-chain fatty acid, e. g. oleic acid, stearic acid, palmitic acid, lauric acid and other fatty acids containing at least 12 carbon atoms, to form sorbitan partial ester

2. Etherification of the remaining hydroxyl group on groups of said partial ester with ethylene oxide to form a hydroxypolyoxyethylene ether thereof. The quantity of ethylene oxide employed should be such that the ether content ranges from 15 to 30 moles/mole _____

Means for carrying out these reactions are well known in the art, and further details concerning the preparation of the products in question are set forth in that prior

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tion of U. S. Patent No. 2,340,466 which relates to the preparation of the so-called "Type B emulsifiers. These products are for the most part oily yellow liquids which are soluble in water, acetone, alcohol and other common organic solvents. They vary in viscosity from about 250 to about 600 cps. at 25° C., depending upon the nature of the long-chain fatty acid medium, the number of such residues in the molecule, and the length of the hydrocarbon chain. As examples of the surface active agents of this group there may be mentioned hydroxypolyoxyethylene sorbitan monolaurate (Tween 20), hydroxypolyoxyethylene sorbitan monopalmitate (Tween 40), hydroxypolyoxyethylene sorbitan monostearate (Tween 60), hydroxypolyoxyethylene sorbitan trioleate (Tween 85) etc. Further information concerning these materials and the so-called partial soaps (Spans) is set forth in "Atlas Surface Active Agents" Atlas Powder Co., Wilmington, Delaware, 1950.

The properties in which the water-soluble metal salt or hydroxide and the surface active agent are incorporated in the drilling fluid are to a certain extent interdependent, i. e., with increasing amounts of the metal component the amount of surface active agent may be decreased, and vice versa. Also, certain particular metal compounds require the presence of more of a particular surface active agent than others, and certain types of surface active agents as such are more effective than others. In general, however, the water-soluble metal salt or alkali-metal hydroxide is provided in an amount representing between about 0.1 and about 5 per cent, preferably between about 0.1 and about 2 per cent, by weight of the entire composition, and the surface active agent is employed in an amount representing between about 0.1 and about 8 per cent, preferably between about 0.4 and about 4 per cent, by weight of the entire composition.

As previously stated, it is necessary that the drilling fluid contain sufficient water to dissolve the water-soluble metal salt or hydroxide so that the latter becomes dispersed in the fluid in the form of a relatively dilute solution. In many instances the drilling fluid will normally contain sufficient water for this purpose, in which case no water need be added along with the metal salt or hydroxide. In some instances, however, it will be necessary to add a small amount of water. In general, it is desirable that the drilling fluid contain at least about 5 per cent, preferably at least about 5 per cent, by weight of water. The upper limit on the water content of the fluid is established at about 10 per cent by weight since those fluids which contain substantial amounts of water lose the desirable characteristics of oil-base drilling fluids in general, and are more properly classifiable as emulsion-base fluids.

The use of a water-soluble metal salt or alkali-metal hydroxide in combination with a surface active agent of the above-defined class in accordance with the invention is applicable to oil-base drilling fluids in general, regardless of their exact formulation. In general, all oil-base drilling fluids essentially comprise a mineral oil dispersion of solids and a dispersing agent which serves to maintain the solids in suspension or to disperse them in the oil. When a hydroxide is included as a well-building agent the fluid usually also contains a small quantity of water. Almost invariably the base oil is a mineral oil, and may be crude oil, a distillate, or a residual fraction. Very often blends of distillate and residual fractions are employed, e. g., a blend of light distillate such as kerosene or Diesel fuel and a light residual fraction such as furnace oil or a light fuel oil. The dispersed solids may usually take the form of finely-divided inert metallic compounds such as lead dust, barium, iron oxide, calcium silicate, mica, or the like, or they may serve as well-building agents to coat or plaster the walls of the bore with an impermeable layer which prevents escape of the

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drilling fluid into permeable formations traversed by the bore. Such well-building agent usually comprises a hydroxide clay such as bentonite, to which case a small amount of water is included in the fluid for the purpose of effecting hydration of the clay. Asphalt is also employed as a well-building agent. In many instances the dispersed solids may comprise both a weighting agent and a well-building agent. A wide variety of materials may be employed as dispersing or suspending agents to maintain the solids uniformly dispersed in the base oil. For the most part, however, the dispersing agent will comprise a metal soap of a fatty acid or sulfonic acid. In some instances such soaps are formed in situ by incorporating into the fluid soap-forming acids, such as tall oil, rosin, oleic acid, stearic acid, lauric acid, linoleic acid, and the like and a basic inorganic compound such as sodium hydroxide, lime, or sodium silicate. In other cases the soap may be formed in situ by incorporating an alkali-metal soap and an alkaline earth metal base into the fluid, whereby saponification occurs to form the corresponding alkaline-earth metal soap. Soap mixtures, including mixtures of water-dispersible and oil-dispersible soaps may also be employed. In addition to the soap-type dispersing agents, such materials as lampblack and diatomaceous earth have been employed for the same purpose.

While the principle of the invention is applicable to all types of oil-base drilling fluids, it is particularly applicable to the so-called "Type B" fluids of the type described in U. S. Patent 2,340,466. Such fluids are prepared by dispersing small amounts each of a hydroxide clay in an alkali-metal metal base and an alkali-metal soap of a heat-treated rosin in suitable base oil. A partial saponification reaction occurs between the rosin soap and the alkaline-earth metal base whereby there is obtained a mixture of the corresponding alkaline-earth metal rosin soap and unreacted alkali-metal rosin soap. The alkali-metal rosin soap employed in preparing this type of drilling fluid is obtained by reacting an alkali-metal alkali, e. g., sodium or potassium hydroxide, with heat-treated wood or gum rosin in such a manner that the reaction is only partially complete and the saponified product contains from about 1 to about 15 per cent of free unneutralized rosin acids.

The heat-treatment of rosin, whereby the rosin acids thereof are isomerized and/or otherwise modified, is well known in the prior art, and may be effected in various ways to obtain modified rosin products which vary somewhat in their physical and chemical properties depending upon the nature and extent of the heat-treatment. Thus, any of the various color grades of refined wood or gum rosin may be heated under non-oxidizing conditions at temperatures between about 250° C. and about 350° C. for a length of time sufficient to raise the specific rotation of the rosin from its original negative value to a value between about +3 and about +15.

The resulting rosin product closely resembles the original rosin in appearance, ease of saponification, etc., but is considerably altered chemically as evidenced by its increased specific rotation, increased dihydroxybutyric acid content, lower iodine number, etc. By carrying out the heat-treatment at somewhat higher temperatures and/or over longer periods of time, the specific rotation may be raised further, e. g., to +25 or even higher, and the degree of olefin unsaturation further decreased. Also, under such conditions decarbonylation takes place with the formation of unsaponifiable bodies which are usually referred to as rosin oil. The heat treatment of rosin to secure the desired modification of the rosin acids as indicated by increase in specific rotation to a value above about +5 may also be effected in the presence of catalysts at relatively low temperatures as described in U. S. Patent 2,114,429. The catalysts employed are of the hydrogenation type, e. g., metallic platinum or palladium, although the treatment is carried out in the

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absence of added hydrogen. The reaction which takes place is termed "disproportionation" since it involves the simultaneous hydrogenation and dehydrogenation of olefin-type acids with the consequent formation of dihydroxybutyric and dihydroxybutyric acids and their esters, and the resulting product is referred to as "disproportionated rosin." Similarly, the product obtained by heat-treating rosin under conditions sufficiently drastic that carbonyl groups are removed from the rosin acids is termed "decarbonylated rosin," and the product obtained by heat-treating rosin under less drastic conditions so that the change effected is substantially only one of molecular rearrangement is referred to as isomerized rosin. All of these modified rosin products are characterized by having been prepared by heat-treating rosin under conditions of time and temperature, and in the presence of absence of a hydrogenation catalyst but in the absence of added hydrogen sufficient to raise the specific rotation of the rosin to a value above about +5.

Any of the above described modified rosin products may be used to obtain the saponification products employed in preparing the preferred drilling fluid composed of the present invention. Procedure for carrying out the saponification reaction is well known in the art and in general consists merely of adding the modified rosin in the solid or molten state to a hot aqueous solution of the desired alkali-metal alkali and thereafter heating the mixture until the reaction is complete and the product contains the desired amount of water. The amount of alkali employed is somewhat less than that required for the complete saponification of the rosin acids other than the saponification product may contain the requisite amount of free unneutralized rosin acids. The concentration of the aqueous alkali is usually as adjusted that the product obtained takes the form of a viscous liquid or thick paste containing 60-85 per cent solids. The physical form of the product may depend somewhat upon the type of modified rosin employed. The saponification product obtained from decarbonylated wood rosin contains a substantial amount of rosin oil, for example, a relatively fluid liquid even though it may contain only 5-10 per cent of water.

While any of the alkali-metal alkali saponification products of rosin which has been heat-treated to raise its specific rotation to a value above about +5 may be employed in preparing the oil base drilling fluid, I have found that superior results particularly with respect to the fluid loss value of the drilling fluid are attained by employing either of two specific products of this type. The first of such preferred saponification products is an alkali-metal alkali saponification product of rosin which has been heat-treated at temperatures between about 250° C. and about 350° C. in the absence of catalyst to such extent that it contains only about 50-60 per cent of free rosin acids, 30-40 per cent of unneutralized oils, a small amount of phenolic materials, water and products of unknown composition. A particularly preferred product of this type is the potassium hydroxide saponification product of such heat-treated rosin containing about 45-55 per cent potassium rosin acid soaps, about 30-35 per cent unneutralized materials also about 5-10 per cent free rosin acids, and about 5-10 per cent water. The second of the preferred class of saponification products is the product obtained by heating rosin at temperatures of about 225-300° C. for about 15-20 minutes in contact with a hydrogenation catalyst but in the absence of added hydrogen, distilling the resulting product and collecting fraction distilling at about 210-275° C. under about 5-10 mm. pressure, and thereafter saponifying such fraction with aqueous sodium hydroxide in the known manner. Such product is available commercially under the trade name "Deminol 731." Mixtures of these two types of saponified heat-treated rosin products may also be employed.

The proportions in which the components of this type

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of drilling fluid are employed may be varied between certain limits depending on the identity of such components and the specific properties desired in the composition. Ordinarily, however, the saponified heat-treated rosin product is employed in an amount representing between about 1 and about 10, preferably between about 4 and about 6, per cent by weight of the entire composition. The alkaline-earth metal base, which is preferably calcium hydroxide or calcium oxide, is employed in an amount corresponding approximately to that chemically equivalent to the saponified rosin product. When the latter is one of the preferred products hereinbefore described and the alkaline-earth metal base is calcium oxide or hydroxide, the saponification product is provided in the above-stated amount and the base is employed in an amount representing between about 0.1 and about 5, preferably between about 0.4 and about 2 per cent by weight of the entire composition. The hydroxide clay is employed in an amount representing between about 0.1 and about 5, preferably between about 0.4 and about 1.2, per cent by weight of the entire composition, and the water is provided in an amount representing between about 0.2 and about 10, preferably between about 1 and about 5 per cent by weight of the entire composition. These proportions of water include any water which may be contained in the saponified rosin product and/or other components and accordingly the amount of water actually added during preparation of the composition will be adjusted according to the water content of the other components so that the final composition will contain water in the above-stated proportions.

In determining the electrical resistivity of the drilling fluids provided by the invention, an electrode assembly comprising two 1-inch square silver plates spaced about one inch apart is immersed in a sample of the fluid being tested, and the voltage which must be applied across the electrodes to obtain a predetermined current flow through the fluid (usually 400 milliamperes) is ascertained. By calibrating the electrode assembly against a liquid of known resistivity the resistivity of the fluid sample being tested may be determined from such voltage reading. It has been found, however, that many drilling fluids undergo a dielectric breakdown during such testing procedure. Thus, when the fluid is first subjected to the test the voltage across the electrodes may be increased to a relatively high value, e. g., 130 volts before substantial current flow. As soon as the current starts to flow, however, the voltage may be substantially reduced without the flow of current falling below the aforementioned predetermined value. Accordingly, in making the resistivity determination, the electrode assembly is immersed in the fluid and the voltage applied to the electrode plates is gradually raised until the predetermined flow of current is obtained. A so-called "initial resistivity" value is determined from the applied voltage. The voltage is then gradually reduced, and the minimum voltage required to maintain the predetermined current flow is ascertained, and so-called "ultimate resistivity" value is determined from such minimum voltage reading. The dielectric breakdown of the fluid is more or less permanent and the ultimate resistivity value represents the resistivity which the fluid will have during electric logging operations.

The following examples will illustrate a number of ways in which the principles of the invention have been applied, but are not to be construed as limiting the same.

EXAMPLE 1

The following concentrate composition was prepared

Parts by weight	
Diesel fuel	2500
Saponified decarbonylated rosin	1400
Saponified disproportionated rosin	1400
Bentonite	540
Water	540

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Table II

Expt. No.	Surface Active Agent	Resistivity, Ohm-cm./ft.	
		Initial	Ultimate
10	Alkylated aryl polyether alcohol (10 parts)	100	100
11	Alkylated aryl polyether alcohol (10 parts)	100	100
12	Alkylated aryl polyether alcohol (10 parts)	100	100
13	Alkylated aryl polyether alcohol (10 parts)	100	100
14	Alkylated aryl polyether alcohol (10 parts)	100	100
15	Alkylated aryl polyether alcohol (10 parts)	100	100
16	Alkylated aryl polyether alcohol (10 parts)	100	100
17	Alkylated aryl polyether alcohol (10 parts)	100	100
18	Alkylated aryl polyether alcohol (10 parts)	100	100
19	Alkylated aryl polyether alcohol (10 parts)	100	100
20	Alkylated aryl polyether alcohol (10 parts)	100	100

EXAMPLE III

Approximately 90 parts of salt oil, 45 parts of sodium chloride (10 parts) 150 parts of air-blown asphalt and 45 parts of 70% aqueous sodium hydroxide were stirred into about 500 parts of light diesel fuel, and the resulting composition was diluted with about 340 parts of light diesel fuel oil. The resulting oil-base drilling fluid was stirred for one hour after which it was divided into 1500 part portions. To each portion there was then added 100 parts of water and 40 parts of hydroxypropyl-oxymethylene carbonyl succinate (Tween 80). Approximately 10 parts of the salt indicated in the following Table III were then added to each of the portions of the drilling fluid and the resistivities of the resulting compositions were determined.

Table III

Expt. No.	Salt	Resistivity, Ohm-cm./ft.	
		Initial	Ultimate
21	Sodium chloride	100	100
22	Sodium chloride	100	100
23	Sodium chloride	100	100
24	Sodium chloride	100	100
25	Sodium chloride	100	100
26	Sodium chloride	100	100
27	Sodium chloride	100	100
28	Sodium chloride	100	100
29	Sodium chloride	100	100
30	Sodium chloride	100	100

* A sodium chloride solution was used.

Table I

Expt. No.	Electrolyte		Water, percent	Surface Active Agent		Resistivity, Ohm-cm./ft.	
	Identity	Percent		Identity	Percent	Initial	Ultimate
1	None	0.0	0.0	None	0.0	100	100
2	None	0.0	0.0	None	0.0	100	100
3	None	0.0	0.0	None	0.0	100	100
4	None	0.0	0.0	None	0.0	100	100
5	None	0.0	0.0	None	0.0	100	100
6	None	0.0	0.0	None	0.0	100	100
7	None	0.0	0.0	None	0.0	100	100
8	None	0.0	0.0	None	0.0	100	100
9	None	0.0	0.0	None	0.0	100	100
10	None	0.0	0.0	None	0.0	100	100
11	None	0.0	0.0	None	0.0	100	100
12	None	0.0	0.0	None	0.0	100	100
13	None	0.0	0.0	None	0.0	100	100
14	None	0.0	0.0	None	0.0	100	100
15	None	0.0	0.0	None	0.0	100	100
16	None	0.0	0.0	None	0.0	100	100
17	None	0.0	0.0	None	0.0	100	100
18	None	0.0	0.0	None	0.0	100	100
19	None	0.0	0.0	None	0.0	100	100
20	None	0.0	0.0	None	0.0	100	100

Based on weight of entire composition

EXAMPLE II

The data presented in the following Table II, illustrate the use of a number of different emulsifying agents of the present class in accordance with the principle of the invention. In each experiment, approximately 100 parts of water, 10 parts of eriodon phosphate and 40 parts of the indicated emulsifying agent were added to 1500 parts of the oil-base drilling fluid prepared in Example I. The resulting fluid had the following approximate composition

Oil-base drilling fluid	90.2
Eriodon phosphate	0.6
Water	6.0
Emulsifying agent	2.4
	100.0

EXAMPLE IV

Approximately 400 parts of a commercial drilling fluid concentrate comprising asphalt and tene were stirred into 800 parts of light diesel fuel. The resulting drilling fluid was divided into 1500 part portions, and to each portion was added 100 parts of water, 40 parts of alkylated aryl polyether alcohol (Triton X-100) and 10 parts of the salt indicated in the following Table IV. The resistivity of each sample is indicated in the table

Table IV

Expt. No.	Salt	Resistivity, Ohm-cm./ft.	
		Initial	Ultimate
31	None	100	100
32	None	100	100
33	None	100	100
34	None	100	100
35	None	100	100
36	None	100	100
37	None	100	100
38	None	100	100
39	None	100	100
40	None	100	100

The foregoing examples illustrate the use of various electrolytes and surface active agents of the present class for imparting electrical conductivity to several different types of freshly-prepared oil-base drilling fluids. In many instances, however, it is desirable to treat drilling fluids which have previously been used in the field. Such "field fluids" are almost invariably contaminated with calcium and/or sodium compounds, and while the principle of the present invention is broadly applicable to such drilling fluids, I have found that superior results are attained when the electrolyte comprises a mixture of an alkali-metal hydroxide and water-soluble salt of strong base and weak acid, e.g., sodium chloride, sodium carbonate, sodium phosphate, etc. Such mixed electrolyte and the surface active agent may be added separately to the drilling fluid, but a more convenient procedure consists in preparing a pre-mixed composition which may be packaged and sold as such a "conductivity additive" to be added with the drilling fluid whenever desired. Such composition suitably comprises 100 parts by weight of water between about 10 and about 40 parts by weight of a mixture of an alkali-metal hydroxide and a water-soluble salt of strong base and weak acid, and between about 20 and about 80 parts by weight of one of the surface active agents of the present class. If desired, water-miscible organic solvent such as isopropyl alcohol may be included to promote solubility of the surface active agent in the water. The electrolyte mixture will comprise from about 10 to about 90 per cent by weight of the alkali-metal hydroxide and from about 90 to about 10 per cent by weight of the water-soluble salt. In employing such a "conductivity additive" composition to impart electrical conductivity to an oil-base drilling fluid the composition is simply stirred into the fluid in amount equal to between about 5 and about 20 per cent by weight of the entire composition. The use of such "conductivity additive" composition is of course not limited to contaminated field fluids but is also applicable to drilling fluids which have not previously been used.

The following example illustrates the use of mixed electrolyte in conjunction with a typical field fluid as above described.

EXAMPLE V

A steam hot field fluid was prepared by adding 12 parts of calcium chloride, 30 parts of sodium chloride and 120 parts of water to 15,000 parts of the drilling fluid prepared in Example I. The resulting composition was divided into 1500 part portions and to each portion there was added 100 parts of water, 40 parts of hydroxypropyl-oxymethylene carbonyl succinate (Tween 20) and varying amounts of electrolyte as indicated in the following Table V

Table V

Expt. No.	Electrolyte	Resistivity, Ohm-cm./ft.	
		Initial	Ultimate
41	None	100	100
42	None	100	100
43	None	100	100
44	None	100	100
45	None	100	100
46	None	100	100
47	None	100	100
48	None	100	100
49	None	100	100
50	None	100	100

3,789,190

Table VI

Expt. No.	Salt	Resistivity, Ohm-cm./ft.	
		Initial	Ultimate
51	None	100	100
52	None	100	100
53	None	100	100
54	None	100	100
55	None	100	100
56	None	100	100
57	None	100	100
58	None	100	100
59	None	100	100
60	None	100	100

The following examples are illustrative of typical "conductivity additive" compositions which may be employed as described above

EXAMPLE VI

Glycerol mono-oleate	27
Sodium hydroxide	3
Sodium chloride	10
Trisodium phosphate	10
Water	50
Isopropyl alcohol	10

EXAMPLE VII

Diethylene glycol mono-terephthalate	30
Sodium hydroxide	10
Sodium chloride	10
Water	50

EXAMPLE VIII

Sulfolane oxide-fatty acid condensate (Emulphor AO)	40
Potassium hydroxide	5
Sodium chloride	10
Water	55

As will be apparent to those skilled in the art many variations in the composition of the drilling fluid and/or the conductive additive may be made without departing from the scope of the invention. The essence of the invention lies in adding to normally non-conductive oil base drilling mud between about 0.01 and about 5 per cent by weight of a water-soluble salt and/or hydroxide between about 0.1 and about 0.18 per cent of a non-toxic surface active agent and sufficient water to adjust the total water content of the composition to between about 3 and about 10 per cent, all of said proportions being based on the weight of the entire composition.

The conductive drilling fluids provided by the invention may be employed in any of the various well logging methods which require that one or more electrodes be positioned within a well bore filled with a conductive fluid. Certain of such methods comprise the use of the electrical resistivity of the earth formations traversed by the bore. Others comprise measuring the so-called "self-potential" of such formations. Regardless of the exact nature of the logging method however, the fluid described in the drilling fluid is well adapted to use as the conductive fluid with which the bore is filled and within which an electrode is submerged.

Other modes of applying the principle of my invention may be employed instead of those explained above, being made as regards the methods or materials employed provided the composition stated by any of the following claims, or the equivalent of such stated compositions, be obtained.

I therefore, particularly point out and distinctly claim as my invention

1. An oil-base drilling fluid comprising a mineral oil carrying suspended solids and sufficient of a dispersing agent to maintain said solids dispersed in said oil, between about 3 and about 10 per cent by weight of water, between about 0.01 and about 5 per cent by weight of an electrolyte selected from the class consisting of water-soluble metal salts and alkali-metal hydroxides, and between about 0.1 and about 0.18 per cent by weight of a non-toxic surface active agent.

2. An oil-base drilling fluid according to claim 1 wherein the dispersing agent is a metal soap.

3. An oil-base drilling fluid according to claim 1 wherein the dispersing agent comprises a mixture of water-dispersible and oil-dispersible resin soaps.

4. An oil-base drilling fluid according to claim 1 wherein the surface active agent is selected from the class consisting of (1) partial esters of polyhydric alcohols with long-chain carboxylic acids, (2) esters of hydroxy alkyl ethers of polyhydric alcohols with long-chain carboxylic acids, and (3) polyalkylene ether alcohols.

5. An oil-base drilling fluid comprising a mineral oil having suspended therein a solid well-building agent and a finely divided inert weighing agent and sufficient of a dispersing agent to maintain said solids dispersed in said oil, between about 3 and about 10 per cent by weight of water between about 0.01 and about 5 per cent by weight of an electrolyte selected from the class consisting of water-soluble metal salts and alkali-metal hydroxides, and between about 0.1 and about 6 per cent by weight of a non-toxic surface active agent selected from the class consisting of (1) partial esters of polyhydric alcohols with long-chain carboxylic acids, (2) esters of hydroxy alkyl ethers of polyhydric alcohols with long-chain carboxylic acids and (3) polyalkylene ether alcohols.

6. An oil-base drilling fluid according to claim 5 wherein said well-building agent is a hydratable clay.

7. An oil-base drilling fluid according to claim 5 wherein the dispersing agent is a metal soap.

8. An oil-base drilling fluid according to claim 5 wherein the surface active agent is a hydricopolypolyethylene ether of a long-chain, fatty acid ester of sorbitan.

9. An oil-base drilling fluid according to claim 5 wherein the electrolyte is selected from the class consisting of alkali-metal hydroxides, alkali-metal silicates, and alkali-metal phosphates.

10. An electrically conductive oil-base drilling fluid comprising (1) normally non-conductive drilling fluid prepared by dispersing in a mineral oil between about 1 and about 10 per cent by weight of an alkali-metal alkali apportionment product of resin which has been heated at a temperature between about 250° and about 350° C. for a period of time sufficient to raise its specific rotation to a value above about +5 and apportioned resin product containing between about 1 and about 15 per cent by weight of free resin acids between about 0.1 and about 5 per cent by weight of a hydratable clay between about 0.5 and about 10 per cent by weight of water and an amount of an alkali-metal metal base corresponding approximately to that chemically equivalent to said apportioned resin product; (2) between about 0.01 and about 5 per cent, based on the weight of the entire composition, of an electrolyte selected from the class consisting of water-soluble metal salts and alkali-metal hydroxides; (3) between about 0.1 and about 6 per cent, based on the weight of the entire composition, of a non-toxic surface active agent selected from the class consisting of (a) partial esters of polyhydric alcohols with long-chain carboxylic acids, (b) esters of hydroxy alkyl ethers of polyhydric alcohols with long-chain carboxylic acids, and (c) polyalkylene ether alcohols; and (4) sufficient water to adjust the water content of the entire composition to between about 3 and about 10 per cent by weight.

11. An electrically conductive oil-base drilling fluid according to claim 10 wherein the electrolyte is provided in an amount representing between about 0.1 and about 2 per cent by weight of the entire composition, the sensitizing agent is provided in an amount representing between about 0.4 and about 4 per cent by weight of the entire composition, and sufficient water is provided to adjust the water content of the entire composition to between about 3 and about 10 per cent by weight.

12. An electrically conductive oil-base drilling fluid

according to claim 10 wherein the surface active agent is a hydricopolypolyethylene ether of a long-chain fatty acid partial ester of sorbitan.

13. An electrically conductive oil-base drilling fluid according to claim 10 wherein the alkali-metal metal base component of the normally non-conductive fluid is selected from the class consisting of calcium hydroxide and calcium oxide.

14. An electrically conductive oil-base drilling fluid according to claim 10 wherein the alkali-metal alkali apportionment product is the potassium hydroxide apportionment product of resin which has been heated at a temperature between about 250 and about 350° C. for a period of time sufficient to raise its specific rotation to a value above about +5 and comprises between about 45 and 55 per cent of potassium resin soap, between about 30 and about 35 per cent of unsaponifiable materials, between about 5 and about 10 per cent of free resin acids, and between about 5 and about 10 per cent of water.

15. An electrically conductive oil-base drilling fluid according to claim 10 wherein the alkali-metal alkali apportionment product is that obtained by heating resin at a temperature between about 225 and about 300° C. for from about 15 to about 60 minutes in the presence of a hydrogenation catalyst but in the absence of added hydrogen, distilling the resulting product and collecting a fraction distilling between about 210° and about 275° C. under 5-10 mm. pressure, and thereafter apportioning such fraction with aqueous sodium hydroxide.

16. In a well logging method wherein at least one electrode is positioned within a well bore filled with an electrically conductive fluid, the improvement which consists in employing as said fluid the conductive oil-base drilling fluid defined by claim 1.

17. In a well logging method wherein at least one electrode is positioned within a well bore filled with an electrically conductive fluid, the improvement which consists in employing as such fluid the conductive oil-base drilling fluid defined by claim 5.

18. In a well logging method wherein at least one electrode is positioned within a well bore filled with an electrically conductive fluid, the improvement which consists in employing as such fluid the conductive oil base drilling fluid defined by claim 10.

References Cited in the file of this patent

UNITED STATES PATENTS

2,542,020	Fluckner	Feb. 20, 1951
2,573,980	Fluckner	Nov. 6, 1951
2,575,561	Fluckner	Nov. 6, 1951
2,582,523	Fluckner	Jan. 15, 1952
2,605,665	Polak	July 15, 1952
2,612,471	Fluckner	Sept. 30, 1952
2,618,694	Schaeffer	Nov. 18, 1952
2,626,305	Krueger	Jan. 20, 1953
2,661,134	Lemmon	Dec. 1, 1953

FOREIGN PATENTS

467,563	Canada	Aug. 22, 1950
865,226	France	Mar. 27, 1954

OTHER REFERENCES

Barnett: The Chemical Formulary vol. VI, page 490, pub. 1943 by Chemical Pub. Co. of Brooklyn, New York.
Adm Surface Active Agents, pages 59 and 60, pamphlet pub. Oct. 1948 by Adm Powder Co. of Wilmington, Delaware.

Evidence for Synergism in Nonionic Surfactant Mixtures Enhancement of Solubilization in Water in Oil Microemulsions

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It is well known that certain mixtures of surfactants can provide better performance than pure surfactants for a wide variety of applications^{1,2} and thus it is expected that enhanced solubilization of water in water in oil (w/o) microemulsions will also be achieved with certain surfactant mixtures. The formation of w/o microemulsions involves dissolving an aqueous phase into an oil phase creating a transparent and thermodynamically stable suspension of droplets with diameters in the range of 10–100 nm. It is desirable to accomplish this with a minimum amount of surfactant³ and in order to achieve this goal mixtures of surfactants can be used. We intend to address different surfactant mixtures that exhibit synergism in the solubilization of water in w/o microemulsions showing the existence of at least two different mechanisms of synergism.

Synergism in surfactants may be defined as any situation where mixtures of surfactants have superior properties when compared to the properties of any of the single components alone. Although certain mixtures of dissimilar surfactants can be expected to show synergism enhancement in properties may also occur with mixtures of similar structures. Shinoda et al.^{4,5} have demonstrated that macroemulsions made with nonionic surfactants that have been purified to a single poly(ethylene oxide) chain length are generally less able to solubilize the dispersed phase into the continuous phase when compared to macroemulsions made with surfactant having the same average length but an ethylene oxide size distribution. Ordinarily one would not expect strong synergistic effects in mixtures of nonionic surfactants as synergism in anionic/nonionic surfactant mixtures has been attributed to Coulombic ion–dipole or hydrogen bonding interactions among the polar groups. Nonionics which have minimum intermolecular interactions should have by comparison the lowest synergism of all mixtures.⁶ In light of this previous work we are able to demonstrate strong synergism in nonionic surfactant mixtures.

When formulating water in oil microemulsions one must account for several factors including the partitioning of the surfactant (or its components) between the oil water and interfacial domains (Figure 1). For maximum solubilization it is desirable to have most of the surfactant at the interface between the oil and water rather than

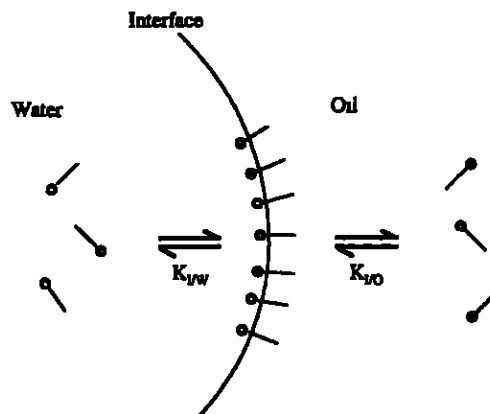


Figure 1 In microemulsions all surfactant molecules are distributed between the oil water and interface

Table 1 Surfactants Used in This Study^a

surfactant (Igepal)	abbrev	EO number	HLB	water soluble	oil soluble
CO 210	C ₈ PhE ₁₅	15	4.6	no	yes
CO-430	C ₈ PhE ₄	4	8.8	no	yes
CO 520	C ₈ PhE ₅	5	10.0	no	yes
CO 530	C ₈ PhE ₆	6	10.8	no	yes
CO 610	C ₈ PhE _{7.5}	7.5	12.2	yes	yes
CO-720	C ₈ PhE ₁₂	12	14.2	yes	yes

^a The Igepal CO family of surfactants are nonylphenyl ethoxylates (*p*-t C₈H₁₈C₆H₄(OC₂H₄)_nOH)

dissolved in the oil or water phases. Increasing the interfacial area should also increase solubilization. Synergism in microemulsion solubilization has been previously reported for a nonionic–anionic system designed for pharmaceutical applications using mixtures of AOT (sodium bis(2-ethylhexyl)sulfosuccinate) and Arlacel 20 (sorbitan laurate) in different proportions.^{7,8} The present paper reports similar improvements using nonionic–nonionic surfactant mixtures for solubilization of water in water in-oil microemulsions and provides evidence for two different synergism mechanisms.

Experimental Procedure

Microemulsion solubilization experiments were performed by titrating water into a mixture of surfactant and oil. The transition from a clear to a cloudy solution indicates that the maximum water solubilization has been exceeded. The rate of solubilization decreases as the maximum solubilization is approached. Due to these kinetic considerations the final cloudy transition was established only after several hours of stirring of a sample. All experiments were performed at 25 °C. The initial surfactant to oil ratio was 0.20 by weight with nonylphenyl ethoxylate surfactants (Igepal CO series Rhone-Poulenc Cranbury NJ) and cyclohexane (Fisher Scientific Fair Lawn NJ) as the oil phase. Similar microemulsions have been well-characterized and used for nanoparticle synthesis.⁹

The surfactants used in the solubilization experiments are commercial grade nonylphenyl ethoxylates (C₈PhE_n) with properties summarized in Table 1. This family of surfactants has the same hydrophobic domain (nonylphenol) and variation only in the length of the hydrophilic domain which consists of poly(ethylene oxide). No attempt was made to further purify these materials. These surfactants are synthesized by polymerization of ethylene oxide to nonylphenol resulting in a wide distribution of the number of ethylene oxide residues on any given molecule around an average EO number for the mixture.

(7) Johnson K. A. Shah D. O. *J Colloid Interface Sci* 1985 107 269.

(8) Johnson K. A. Shah D. O. In *Surfactants in Solution* Mittal K. L. Bothorel P. Eds. Plenum New York 1986 Vol. 8.

(9) Kumar P. Pillai V. Shah D. O. *Appl Phys Lett* 1993 62 765.

* Current address: Massachusetts Institute of Technology Department of Chemical Engineering Cambridge MA 02139 4307 E-mail: hulbers@mit.edu

(1) Scamehorn J. F. *Phenomena in Mixed Surfactant Systems*. American Chemical Society: Washington DC 1988.

(2) Rosen M. J. In *Mixed Surfactant Systems*, Holland P. M. Rubingh D. N. Eds. American Chemical Society: Washington DC 1992.

(3) Shinoda K. Kunieda H. In *Microemulsions: Theory and Practice*, Prince L. M. Ed. Academic Press: New York 1977 Chapter 4.

(4) Shinoda K. Saito H. Arai H. *J Colloid Interface Sci* 1971 35 624.

(5) Shinoda K. Friberg S. *Emulsions and Solubilization*. Wiley: New York 1986.

(6) Rosen M. J. *Surfactants and Interfacial Phenomena*, 2nd ed. Wiley: New York 1989.

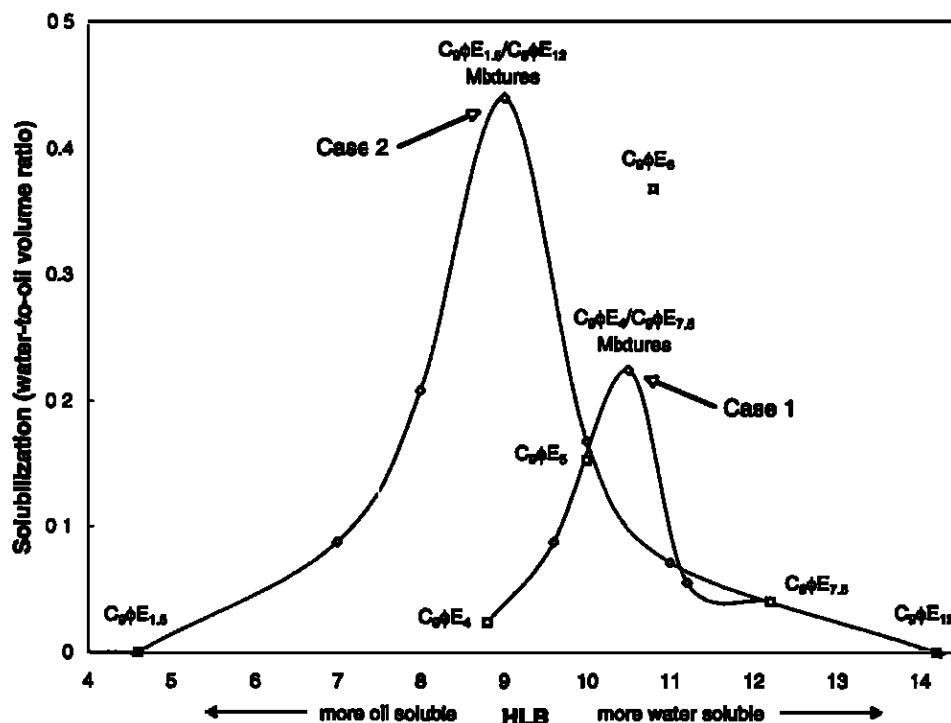


Figure 2 Maximum water solubilization (as a w/o microemulsion) vs HLB for mixtures of nonylphenyl ethoxylate surfactants in cyclohexane

The distribution of these chain lengths is often assumed to be a Poisson distribution and may also include a few percent unreacted nonylphenol or material with EO = 1 or EO = 2 in excess of that predicted by the Poisson calculation. All surfactants were soluble in cyclohexane and only the two with the largest EO number were soluble in water. It is expected that the surfactants with lower EO number are more oil soluble especially in *n*-alkane oils.

Solubilization results are presented as a maximum water-to-oil volume ratio (x) solubilized. To convert to weight fractions of water (W), oil (O), and surfactant (S), the following formulas may be used based on sample sizes of 1.2 g of surfactant and 4.8 g of oil (6.16 mL for cyclohexane):

$$W = 6.16x / (6 + 6.16x)$$

$$O = 4.8 / (6 + 6.16x)$$

$$S = 1.2 / (6 + 6.16x)$$

The maximum solubilization of 0.44 water/oil volume ratio for the optimum $C_9PhE_{1.5}/C_9PhE_{12}$ case represents a total of 31 wt % water, 55 wt % oil, and 14 wt % surfactant, or a 0.56 water/oil weight ratio.

Discussion

Figure 2 shows water solubilization in water in oil microemulsions for single nonylphenyl ethoxylates as well as binary mixtures vs HLB. The HLB can be calculated for these surfactants from the average EO content of the molecule. HLB is defined as the hydrophile-lipophile balance of a surfactant, and for ethoxylated surfactants can be calculated as 20 times the weight fraction of poly(ethylene oxide) in the molecule.^{10,11} HLB was initially intended to aid in the selection of surfactant mixtures for macroemulsion formulation.

Of the single surfactants studied, nonylphenyl ethoxylate (C_9PhE_6) with an HLB of 10.8 achieved the largest solubilization of water in cyclohexane (Figure 2). This system compares favorably with previous water in oil

microemulsion formulation results using *n*-alkanes and sorbitan ester ethoxylates¹² where it was established that optimum w/o microemulsions were created for surfactant mixtures that fell in the HLB 8.5–11 range. This range is much different from that of macroemulsions, where w/o emulsions are expected to form for surfactant mixtures in the HLB 3–6 range, while o/w emulsions generally form in the HLB 10–18 range.^{10,11}

Two different surfactant mixtures were investigated. Case 1 (Figure 2) involved two surfactants, C_9PhE_4 and $C_9PhE_{7.5}$, that were close in molecular size to C_9PhE_6 , which was the best performing single surfactant. Case 2 (Figure 2) involved $C_9PhE_{1.5}$ and C_9PhE_{12} , which were much less similar in molecular size than the previous case. Both of these mixtures showed superior solubilization results over either pure component at some mixture ratio, with case 2 clearly showing superior results over both case 1 and the best single surfactant case. The underlying reasons for these differences become more clear when we examine the composition of the mixtures.

Surfactant Size Distributions As the surfactants we consider here are not pure single component species but rather a wide distribution of homologous compounds, let us compare the actual distributions of the different surfactants and mixtures. In Figure 3 we plot the mole fraction of each EO component in each surfactant vs the HLB number of that particular fraction. These size distributions arise from the method of synthesis of the surfactant, as ethylene oxide is polymerized to nonylphenol by anionic polymerization; the resulting EO distribution is ideally a Poisson distribution. Thus for a surfactant with an EO number of N , the relative mole fraction x of any EO number component can be calculated by

$$P(x) = N^x e^{-N} / x! \quad (1)$$

For all of these components of EO = x , the HLB of the

(10) Griffin, W. C. *J. Soc. Cosmet. Chem.* **1949**, *1*, 311–326.

(11) Griffin, W. C. *J. Soc. Cosmet. Chem.* **1954**, *5*, 249–256.

(12) Hulbers, P. D. T.; Shah, D. O. In *Dynamic Properties of Interfaces and Association Structures*; Pillai, V.; Shah, D. O., Eds.; AOCS Press: Champaign, IL, 1996.

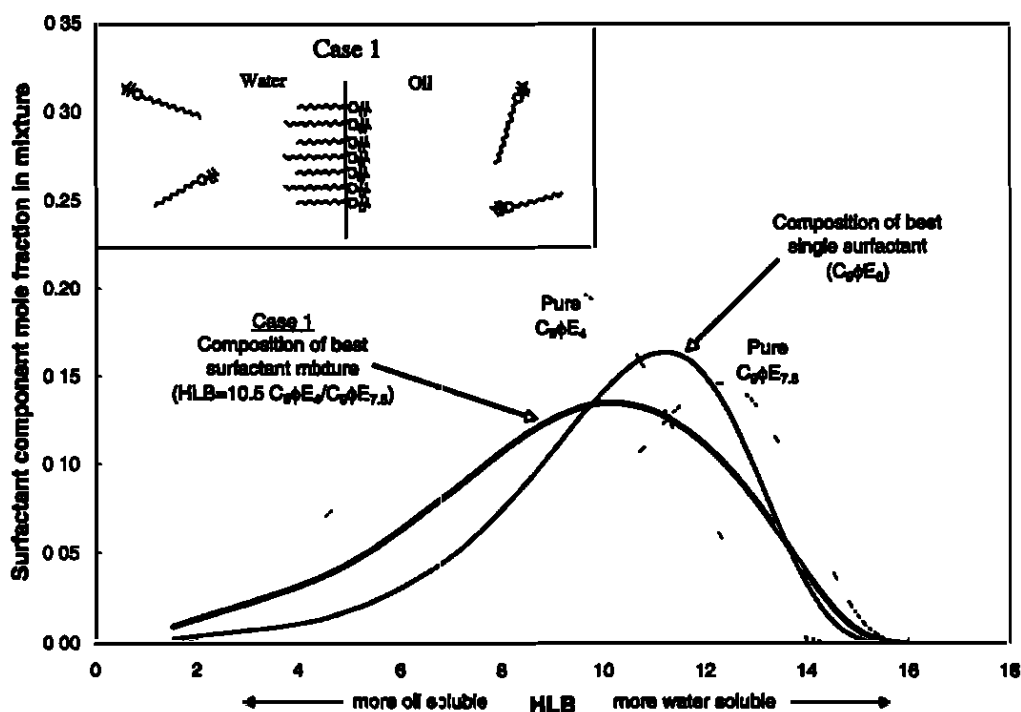


Figure 3 Distribution of components in single nonylphenyl ethoxylate surfactants as well as mixtures for case 1

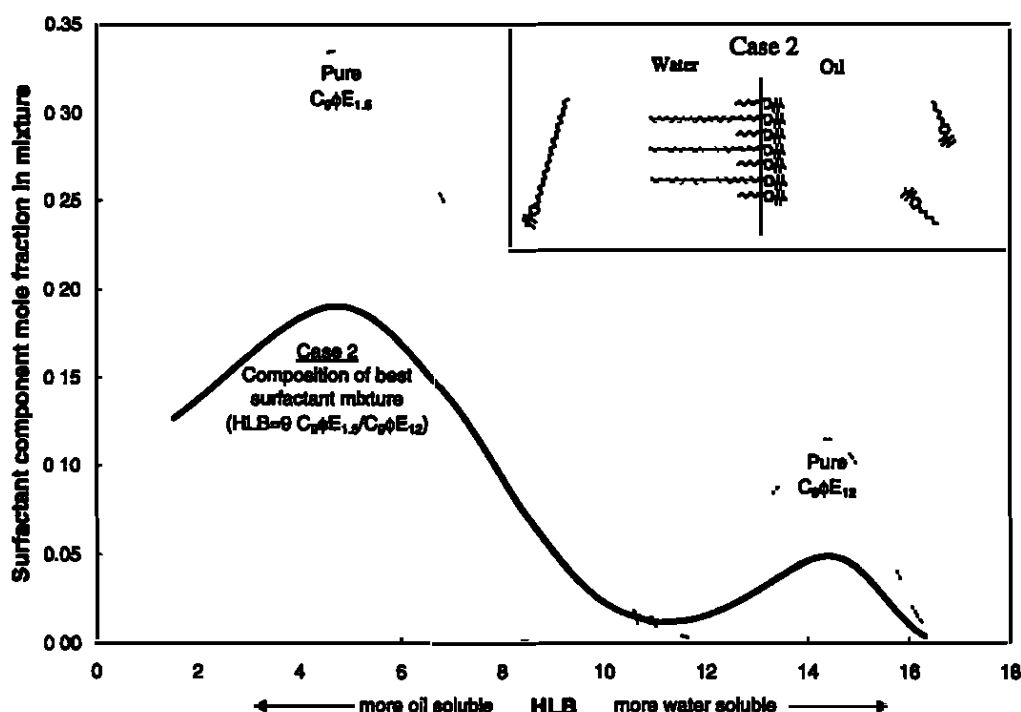


Figure 4 Distribution of components in single nonylphenyl ethoxylate surfactants as well as mixtures for case 2 showing evidence for synergism

component can be calculated for nonylphenyl ethoxylates using

$$HLB(EO = x) = 20 (17 + 44x)/(220 + 44x) \quad (2)$$

where we include the terminal hydroxyl group (MW = 17) in addition to the ethylene oxide residues (MW = 44) into the hydrophilic domain

Case 1 For the first case Figure 3 shows the distribution of components for the best single surfactant C_9PhE_6 along with the two components of the mixture C_9PhE_4 and $C_9PhE_{7.5}$. The curves represent the actual HLB values of the components within each of the

surfactants or surfactant mixtures with the distribution of components calculated from eq 1 and the HLB values for each EO component from eq 2. From Figure 3 it can be seen that C_9PhE_4 has the bulk of its material in the HLB 9–13 region which can be expected for good water-in-oil microemulsion solubilization. For the mixtures the peak solubilization case (a 50/50 mixture of C_9PhE_4 and $C_9PhE_{7.5}$ with an $HLB_{mix} = 10.5$) is plotted. This EO distribution of the mixture has a shape similar to the distribution curve for the best single surfactant (C_9PhE_6) although somewhat wider. Again it appears that the best solubilization for the mixture occurs where the mixture

has most of its components in the HLB 9–13 region. This supports the concept that good solubilization occurs when most of the surfactant falls in a certain HLB region being neither very water soluble nor very oil soluble. This should cause conditions where it is most favorable for the surfactant to partition at the interface. In such a case solubilization for the mixtures is better than that of either component. The best mixture does not solubilize more than the best single surfactant C_9PhE_6 with a similar EO number distribution (Figure 2). Thus the solubilization ability in this case appears to be related only to simple additive contributions of the surfactant material in the HLB 9–13 region with no apparent additional benefit from synergism between the two surfactants.

Case 2 Figure 4 shows a second much different scenario. The two components in this mixture C_9PhE_{15} and C_9PhE_{12} are very oil soluble and very water soluble respectively. Both surfactants have little of their material in the HLB 9–13 region. The plot of the distribution for the optimum mixture (43 wt % C_9PhE_{12} , $HLB_{mix} = 9$) does not have a single maximum. Given the composition of individual components the optimum mixture actually has a minimum of material in the HLB 9–13 region. In this case the high level of solubilization has nothing to do with the amount of this material which is completely opposite to the previous case in Figure 3. Given the conclusions of the first case one would expect less surfactant to partition to the interface as the two surfactant components are highly soluble in the oil (C_9

PhE_{15}) or the water (C_9PhE_{12}) phases. This must not be the case though as mixtures of these two surfactants clearly show the highest water solubilization even greater than the best single surfactant (C_9PhE_6). Some true synergistic effect must cause these components to preferentially partition to the interface for only if the majority of surfactant partitions to the interface can such a high level of solubilization be achieved.

Conclusions

Two different approaches for surfactant selection can be considered in order to achieve a high level of water solubilization in water in-oil microemulsion formulations. The first approach is to maximize the amount of surfactant in the HLB 9–13 region where it is intermediate between high oil solubility and high water solubility. Achieving more surfactant partitioning to the interface as opposed to partitioning into the bulk phases will allow for stabilization of a larger interfacial area and thus a high level of solubilization. Even greater solubilization can result if some synergism between surfactant components can be achieved. As a second approach mixtures of a highly oil soluble surfactant and a highly water soluble surfactant achieved the maximum water solubilization evidently overcoming the expected partitioning of the two surfactant components into the oil and water phases and enhancing their partitioning to the interface.

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**SUPERINTENDENCIA DE INDUSTRIA Y COMERCIO
DIVISION DE NUEVAS CREACIONES
SOLICITUD VIA PCT**

2020

Bogota, D C , 26 de julio de 2007

Abogado

HUMBERTO RUBIO CAMACHO

Apoderado

Solicitante **Halliburton Energy Services, Inc**

ASUNTO

Radicacion **04-10426**

Trámite 002

Evento 001

Actuación 430

Oficio 9353

Folios 014

Como resultado del examen de fondo, realizado con fundamento en el artículo 45 de la Decisión 486 de la Comisión de la Comunidad Andina, se le comunica

1 Documentos estudiados

1 1 Descripción Folios 7 a 22

1 2 Reivindicaciones Folios 23 a 25

1 3 Proridad Folio 29, Solicitud de Estados Unidos No 09/939,990 del 27 de agosto de 2001

2 Objeto de la invención

- El título de la solicitud es **"LODO CONDUCTOR BASADO ELECTRICAMENTE EN ACEITE"** (Folio 1)
- La presente invención se refiere a lodos o fluidos basados en aceite para uso en la perforación de pozos en formaciones subterráneas. Mas en particular, la invención se refiere a lodos basados en aceite, aptos o compatibles para uso con imágenes de resistividad del pozo o de la formación

En la **reivindicación independiente 1** se plantea un método para obtener imágenes de resistividad de una formación durante la perforación de un pozo en dicha formación con un fluido de perforación conductivo basado en aceite, dicho fluido comprende un aceite de base de éster polar, un surfactante derivado de éster sorbitan y un surfactante derivado de éster sorbitan etoxilado, en donde dichos surfactantes son en cantidades suficientes para crear micelas que tienen una mayor concentración en la capa de la palizada

En la **reivindicación independiente 10** se plantea un método para perforar un pozo mientras se obtienen imágenes de resistividad de la formación en la que se perfora el pozo, dicho método comprende utilizar un fluido de perforación eléctricamente conductivo basado en aceite, dicho fluido comprende surfactantes de ácido graso complementarios y un aceite base polar

En la **reivindicación independiente 13** se define un fluido de perforación que comprende un aceite base polar y surfactantes complementarios, de modo que dichos surfactantes formen micelas que tienen una concentración más densa en la capa de la palizada de dicho fluido que cualquier surfactante pudiera tener por sí solo

- Existe la necesidad de nuevos fluidos de perforación basados en aceite de emulsión invertida con propiedades conductivas adecuadas para uso con registros de resistividad
- El objeto de la invención definido se catalogó como **C09K 7/06**, según la Clasificación Internacional de Patentes (IPC)

3 De la solicitud de Patente

3.1 Título

- El título de la invención según se encuentra en el folio 1 es "LODO CONDUCTOR BASADO ELECTRICAMENTE EN ACEITE". No obstante, esta traducción resulta deficiente y confusa. Se recomienda que el título sea modificado del siguiente modo: **"LODO ELECTRICAMENTE CONDUCTOR BASADO EN ACEITE"**

3.2 Descripción (artículo 28 D 486)

- El capítulo descriptivo contiene cantidades expresadas en el sistema inglés de unidades. Se recomienda realizar la conversión al Sistema Internacional de Unidades.
- En conclusión, la descripción no cumpliría con el requisito de acuerdo con el art 28 de la Decisión 486.

3.3 Reivindicaciones (artículo 30 D 486)

- La reivindicación independiente 1 se plantea como 'Un método para obtener imágenes de resistividad de una formación durante la perforación de un pozo en dicha formación con un fluido de perforación conductivo basado en aceite'. Sin embargo, se hace una caracterización de la naturaleza química del fluido base aceite. No es coherente definir un método de monitoreo de formaciones subterráneas como lo es el de imágenes de resistividad, tan solo mencionando la naturaleza del fluido de perforación pues dicho método es una tecnología que implica otras operaciones.

Según la materia de la invención descrita con la solicitud, el objeto central de esta corresponde al fluido de perforación, su naturaleza y composición, por ello, se recomienda que el preámbulo de la reivindicación independiente 1 sea coherente con la materia de la invención, es decir, se plantee en términos del fluido de perforación.

- En la reivindicación independiente 1 se menciona que 'dichos surfactantes son en **cantidades suficientes para crear micelas que tienen una mayor concentración en la capa de la palizada**'. No obstante, la expresión 'cantidades suficientes' no es clara pues genera dudas sobre las magnitudes precisas relacionadas con las cantidades de cada surfactante. Además cuando menciona que es 'para crear micelas que tienen una mayor concentración en la capa de la palizada' esta información corresponde a un resultado a alcanzar y no a una característica propia de la formulación del fluido de perforación. Dado lo anterior, se recomienda considerar que si es importante la cantidad de surfactantes, se incluyan numéricamente en la reivindicación 1 de modo que se elimine la

expresión 'cantidades suficientes' De otra parte, se recomienda que la información que se incluya en la reivindicación independiente 1 corresponda a la solución técnica y no a los efectos o resultados que esta pueda tener, entonces se recomienda eliminar la información que corresponde a resultados a alcanzar

- La reivindicación dependiente 3 se relaciona con la reivindicación 1 pero incluye características de la preparación del fluido de perforación, lo cual es incoherente pues en la reivindicación 1 no se ha mencionado el método de preparación del fluido. Dado lo anterior, si el señor solicitante considera que su propuesta también abarca el método de preparación del fluido de perforación, se recomienda que plantee una reivindicación independiente para este y defina las características novedosas que constituyen el aporte con la propuesta de la solicitud. Si así lo hace, también debe modificar el título de la invención.
- En las reivindicaciones dependientes 4 y 16 no se hizo una traducción adecuada. En dichas reivindicaciones se menciona que la 'emulsión comprende entre 85 y 95 **volumen porcentaje** de éster y entre 5 y 15 **volumen porcentaje** de salmuera. Se recomienda que la expresión resaltada en negrita sea **porcentaje en volumen o %V/V**.
- Las reivindicaciones dependientes 6 y 7 incluyen fórmulas del éster sorbitan y del éster sorbitan etoxilado pero no son legibles. Se recomienda mejorar la legibilidad de las estructuras para facilitar la comprensión y para efectos de digitalización.
- En la reivindicación 11 se hace mención de que los surfactantes son complementarios pero no está clara dicha propiedad porque se especifica que al menos uno de dichos surfactantes de ácido graso complementarios es **más soluble en agua** que los demás, y al menos uno de los demás surfactantes de ácido graso complementarios es **más soluble en agua** que los demás', mientras que en la descripción se explica que "Los surfactantes son complementarios, es decir uno es más soluble en agua que el otro y uno es más soluble en aceite que el otro" (Negrita Personal) (Folio 10, resumen de la invención). Se recomienda rectificar la información que se especifica en la reivindicación 11.
- En la reivindicación independiente 13 se plantea un fluido de perforación pero se caracteriza por los resultados a alcanzar diciendo 'que dichos surfactantes formen micelas que tienen una concentración más densa en la capa de la palizada de dicho fluido que cualquier surfactante pudiera tener por sí solo. Esto no constituye una definición de la materia de la invención sino de un resultado, por ello se recomienda que en el capítulo reivindicatorio se plantee una sola reivindicación independiente para el fluido de perforación y que su parte caracterizante incluya la naturaleza química y proporciones de los componentes del fluido, eliminando la información correspondiente a los resultados a alcanzar.
- En la reivindicación dependiente 16 se incluye la expresión "aproximadamente" que no confiere precisión a la invención. Se recomienda eliminar dicha expresión.
- En conclusión, el capítulo reivindicatorio no cumpliría con el requisito de claridad como se requiere según el art. 30 de la Decisión 486.

4 Determinación del Estado de la Técnica

Considerando que la fecha de presentación de la primera solicitud de patente de la cual se reivindica prioridad es **27 de agosto de 2001**, se buscaron documentos del estado de la técnica relacionados con fecha de publicación anterior a esta y se encontraron los siguientes

N°	Documento	Título	Publicación
D1	US2739120	"ELECTRICALLY CONDUCTIVE DRILLING FLUIDS"	20 de marzo de 1956
D2	"EVIDENCE OF SYNERGISM IN NONIONIC SURFACTANT MIXTURES ENHANCEMENT OF SOLUBILIZATION IN WATER-IN-OIL MICROEMULSIONS"		<i>Langmuir</i> 1997, 13, 5762 – 5765

Se anexan copias en el documento adjunto

5 Analisis de patentabilidad (segun requisito) (articulo 14 D486)

5.1 Nivel inventivo (artículo 18 D486)

- Comentarios sobre el estado de la técnica

La investigación del estado de la técnica relacionado con lodos de perforación permitió identificar la evolución en este campo, observándose una tendencia inicial (1920) al empleo de lodos base aceite y a la incorporación de petróleo (1930) para aumentar velocidades de perforación. En décadas posteriores (1960 a 1980) se avanzó en el empleo de emulsiones base aceite o emulsiones inversas con los consiguientes desarrollos en materia de aditivos, sin embargo, los problemas ambientales fueron identificados, motivando al desarrollo de fluidos sintéticos biodegradables. En 1990 y 1991 los ésteres y las polialfaolefinas respectivamente, fueron los primeros fluidos sintéticos conocidos y desde ese momento, los avances se han dado con base en fluidos no tóxicos.

El documento **US2739120** (D1) forma parte del estado de la técnica y enseña fluidos de perforación eléctricamente conductivos empleados en la investigación y determinación de la naturaleza de las formaciones subterráneas (Columna 1, líneas 62 – 66), que consisten en emulsiones agua en aceite y que incluyen agentes surfactantes particulares no iónicos como por ejemplo, monooleato sorbitan, monopalmitato sorbitol, trioleato sorbitan, (se hace mención de SPAN®) condensados de polioxietileno de monooleato de sorbitan, condensados de polioxietileno de monopalmitato de sorbitan (se hace mención de TWEEN®).

En D1 también se particulariza la incorporación de agentes de superficie como monolaurato hidroxipolioxietileno sorbitan, monopalmitato hidroxipolioxietileno sorbitan, trioleato hidroxipolioxietileno sorbitan, sin embargo, aún se sitúa dicha información en la generación de los lodos base aceite (aceite mineral por ejemplo).

El documento **"EVIDENCE OF SYNERGISM IN NONIONIC SURFACTANT MIXTURES ENHANCEMENT OF SOLUBILIZATION IN WATER-IN-OIL MICROEMULSIONS"** (D2) forma parte del estado de la técnica y en una etapa más avanzada de desarrollo (década de los 90's) enseña que en las microemulsiones agua en aceite (w/o) se puede aumentar la solubilización mediante la incorporación de mezclas de surfactantes no iónicos dado que se demuestra un **efecto sinérgico** importante.

D2 contiene información sobre lo conocido que es el desarrollo de ciertas mezclas de surfactantes porque proveen un desempeño mejor que al adicionar surfactantes puros. De hecho, se logra sinergia en la solubilización de agua en emulsiones w/o.

En D2 se explica que para maximizar la solubilización es deseable tener más surfactantes en la interfase entre el aceite y el agua que disueltos en la fase agua y en la fase aceite, pues el incremento del área interfacial permite incrementar la solubilización.

En D2 se demuestra que mezclas de un surfactante altamente soluble en aceite y un surfactante altamente soluble en agua alcanzan máxima solubilización

- Comentarlos sobre la propuesta y la información del estado de la técnica

El señor solicitante realiza una propuesta (año 2001) de un fluido de perforación base aceite y eléctricamente conductor que se define en las reivindicaciones del caso en estudio. Al analizar el planteamiento de la propuesta, se entiende que el principio técnico sobre el cual se fundamenta consiste en fluidos de perforación basados en aceite con propiedades conductivas, que incluyen **composiciones sinérgicas** de surfactantes derivados de éster sorbitan y de éster sorbitan etoxilado.

Es claro que para el señor solicitante es muy importante incorporar la composición sinérgica de los surfactantes derivados de éster sorbitan y éster sorbitan etoxilado como bien lo sustenta en la descripción. No obstante, al analizar el estado de la técnica es posible afirmar que un técnico de nivel medio versado en la materia, como puede ser un ingeniero químico con experiencia en emulsiones y que también realiza mejoramientos en su campo de trabajo, tiene acceso a información como la reportada en D1 y D2.

Basándose en D1 el técnico puede motivarse a desarrollar lodos eléctricamente conductivos que consistan en una emulsión agua en aceite (w/o) en la que se empleen surfactantes con la misma naturaleza química que tienen los propuestos en la solicitud. De hecho, hasta en D1 se hace referencia a las mismas denominaciones comerciales de la composición citada en la descripción de la solicitud en estudio (SPAN® y TWEEN®).

Con D1 un técnico optaría por incluir un solo surfactante pues en ningún momento se hace mención de los efectos sinérgicos. No obstante, con D2 se demuestra que un técnico conoce la posibilidad de mejorar la estabilidad de las emulsiones mediante incorporar varios surfactantes. Así las cosas, con la información contenida en D1 y D2, el técnico se vería motivado a desarrollar ensayos de rutina para determinar combinaciones de surfactantes sugeridos en D1 donde uno de los surfactantes sea soluble en agua y el otro sea soluble en aceite para obtener un desempeño sinérgico en el sistema w/o.

Lo anterior permite afirmar que proponer lodos base aceite eléctricamente conductivos con la composición sinérgica propuesta en las reivindicaciones, no parece ser una solución técnica que genere un efecto sorprendente que evidencie un salto tecnológico respecto al arte previo. Por el contrario parece un mejoramiento que puede realizar un técnico de nivel medio y que cae dentro de la línea normal de avance de la tecnología.

Así, la propuesta definida en las reivindicaciones de la solicitud no parece cumplir con el requisito de nivel inventivo como se requiere según el artículo 18 de la Decisión 486.

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6 Conclusi n

Los requisitos de patentabilidad de la presente solicitud se encuentran afectados así

N°	Documento N°	Reivindicaciones Afectadas	Requisito que Afecta
D1	US2739120	1 - 20	Nivel Inventivo
D2	"EVIDENCE OF SYNERGISM IN NONIONIC SURFACTANT MIXTURES ENHANCEMENT OF SOLUBILIZATION IN WATER-IN-OIL MICROEMULSIONS"		

En cumplimiento del artículo 45 de la Decisión 486 de la Comisión de la Comunidad Andina, se le indica que debe dar respuesta dentro del término de **sesenta** días contados a partir de la fecha de notificación de la presente comunicación. En caso de no dar respuesta al presente requerimiento, o si a pesar de la respuesta subsistieran los impedimentos para la concesión, se denegará la patente.

Notifíquese el presente oficio conforme a lo dispuesto en el numeral 5.2, literal e), del capítulo quinto del título primero de la circular única No. 10 de 2001.


ALIX CARMENZA CESPEDES DE VERGEL
Jefe de División de Nuevas Creaciones

03 AGO 2007

El anterior requerimiento fue notificado por fijación en lista, de fecha _____

CONCEPTO TECNICO No 1149	EXAMINADOR TECNICO Codigo No 202042
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