

Search history

Search 1: gas and first and second and refrigerant and (natural or GNL or LNG) (Results 11710)

Search 2: 1 and liquef* and expans* and (mixed) (Results 1591)

Search 3: 2 and phase and separator and tac=(refrigerant and gas and heat* and cool*) (Results 452)

Search 4: 3 and ((first or second) w5 refrigerant) (Results 312)

Search 5: (4) AND PD=(2006 OR 2012 OR 2003 OR 2008 OR 2009 OR 2007 OR 2004 OR 2010 OR 2011 OR 2005 OR 2001 OR 2000 OR 2002 OR 1976) (Results 199)

Search 6: (5) AND IPC=(F25) (Results 177)

Search 7: 6 and (non or free) and mixed and closed and (loop or circuit or cycle) (Results 89)

Search 8: 7 and tac=(closed and liquef*) (Results 31)

Search 9: 8 and subcool* (Results 21)

Title: APPARATUS FOR THE LIQUEFACTION OF NATURAL GAS AND METHODS RELATED TO SAME

Abstract: An apparatus and method for producing liquefied natural gas. A liquefaction plant may be coupled to a source of unpurified natural gas, such as a natural gas pipeline at a pressure letdown station. A portion of the gas is drawn off and split into a process stream and a cooling stream. The cooling stream passes through a turbo expander creating work output. A compressor is driven by the work output and compresses the process stream. The compressed process stream is cooled, such as by the expanded cooling stream. The cooled, compressed process stream is divided into first and second portions with the first portion being expanded to liquefy the natural gas. A gas-liquid separator separates the vapor from the liquid natural gas. The second portion of the cooled, compressed process stream is also expanded and used to cool the compressed process stream. Additional features and techniques may be integrated with the liquefaction process including a water clean-up cycle and a carbon dioxide (CO₂) clean-up cycle.

Classifications:

International (IPC 8-9): B01D21/26 B01D36/04 B01D53/52
B01D9/04 C01B31/20 C01B32/50 C02F1/22 C10L3/06 C10L3/10
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F28F27/02 (Advanced/Invention);
F25J1/00 F25J3/00 (Advanced/Non-invention);
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F28F27/00 (Core/Invention);
F17C F25J (Subclass/Invention);
F25J (Subclass/Non-invention)

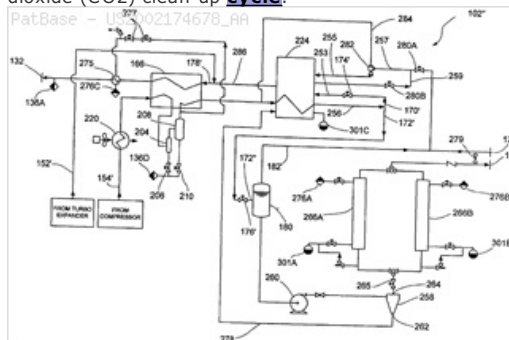
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European: F25J1/00 F25J1/00A6 F25J1/00C2F F25J1/00C2V F25J1/02 F25J1/02A F25J1/02B2 F25J1/02D F25J1/02D2
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Family:

Publication number	Publication date	Application number	Application date
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Probable Assignee: BATTELLE ENERGY ALLIANCE LLC

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Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LI LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN YU ZA ZM ZW

Abstract: Method for **liquefying** a **gas** which comprises **cooling** a feed **gas** stream successively through **first** and **second** temperature ranges to provide a **liquefied** product, wherein refrigeration for **cooling** the feed **gas** stream in the **first** temperature range is provided by a **first** vaporizing **refrigerant** and refrigeration for **cooling** the stream in the **second** temperature range is provided by a **second** vaporizing **refrigerant**, and further wherein an auxiliary **refrigerant** derived from the **second** vaporizing **refrigerant** provides additional refrigeration by vaporization at temperatures above a lowest temperature in the **first** temperature range.

International (IPC 8-9): C09K5/04 C09K5/08 F25B1/00 F25B40/00 F25B9/00 F25J1/00 F25J1/02 (Advanced/Invention); F25B1/10 F25J1/02 (Advanced/Non-invention); C09K5/00 F25J1/00 (Core/Invention)

International (IPC 1-7): F25B7/00 F25J1/00 F25J1/02
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European: C09K5/04B2 F25J1/00A6 F25J1/00C4V F25J1/00C4V2
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Probable Assignee: AIR PRODUCTS AND CHEMICALS INC

Assignee(s): (std): AIR PROD AND CHEM ; AIR PRODUCTS AND CHEMICALS INC ; EHR PRODAKTS EHND KEMIKALZ INK ; ROBERTS MARK J ; ROBERTS MARK JULIAN

Assignee(s): AIR PRODUCTS AND CHEMICALS INC ALLENTOWN ; AIR PRODUCTS AND CHEMICALS INC

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Inventor(s): ROBERTS MARK JULIAN KEMPTON

Agent(s): PIZZEYS PATENT AND TRADE MARK ATTORNEYS PTY LTD; PIZZEYS; MCFADDEN FINCHAM; OSLER HOSKIN AND HARCOURT LLP; KADOR AND PARTNER; MUIR BENJAMIN M J; DE ELZABURU ALBERTO; KIM TAE HONG; AIR PRODUCTS AND CHEMICALS INC PATENT DEPARTMENT; WILLARD

Designated states: AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GW HR HU ID IE IL IN IS IT JP KE KG KP KR KZ LC LI LK LR LS LT LU LV MA MC MD MG MK ML MN MR MW MX MZ NA NE NI NL NO NZ OM PG PH PL PT RO RU SC SD SE SG SI SK SL SN SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN YU ZA ZM ZW

Title: HYBRID **GAS LIQUEFACTION CYCLE** WITH MULTIPLE EXPANDERS

Abstract: Method for **gas liquefaction** comprising **cooling** a feed **gas** by a **first** refrigeration system in a **first heat** exchange zone and withdrawing a substantially **liquefied** stream therefrom, further **cooling** the substantially **liquefied** stream by indirect **heat** exchange with one or more work-expanded **refrigerant** streams in a **second heat** exchange zone, and withdrawing therefrom a further **cooled**, substantially **liquefied** stream. At least one of the one or more work-expanded **refrigerant** streams is provided by compressing one or more **refrigerant** gases to provide a compressed **refrigerant** stream, **cooling** all or a portion of the compressed **refrigerant** stream in a third **heat** exchange zone to provide a **cooled**, compressed **refrigerant** stream, and work expanding the **cooled**, compressed **refrigerant** stream to provide one of the one or more work-expanded **refrigerant** streams. The flow rate of a work-expanded **refrigerant** stream in the **second heat** exchange zone typically is less than the total flow rate of one or more work-expanded **refrigerant** streams in the third **heat** exchange zone.

Classifications:

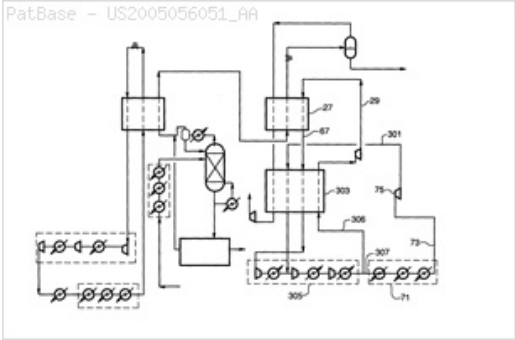
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International (IPC 1-7): F25J1/00 F25J1/02 F25J5/00

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European: F25J1/00A6 F25J1/00C4E F25J1/00C4V F25J1/00R10 F25J1/00R4N F25J1/02D6 F25J1/02D6P F25J1/02Z4H4R2 F25J1/02Z4H4R4 F25J1/02Z4R F25J1/02Z6J F25J1/02Z6L R25J220/62 R25J220/64 R25J245/02 R25J270/16

US: 62/335 62/611 62/611S 62/612 62/612P



Family:

Publication number	Publication date	Application number	Application date
AT479064 E	20100915	AT20040768455T	20040914
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TW200512429 A	20050401	TW20040127656	20040913
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US2005056051 AA	20050317	US20030664336	20030917
US7127914 BB	20061031	US20030664336	20030917
WO05028976 A1	20050331	WO2004GB03909	20040914

Priority:

US20030664336 20030917 WO2004GB03909 20040914 WO2004GB03909 20060316

Probable Assignee: AIR PRODUCTS AND CHEMICALS INC

Assignee(s): (std): AIR PROD AND CHEM ; AIR PRODUCTS AND CHEMICALS INC ; BROSTOW ADAM ADRIAN ; ROBERTS MARK JULIAN ; SPILSBURY CHRISTOPHER GEOFFREY ; EHR PRODAKTS EHND KEMIKALZ INK

Assignee(s): AIR PRODUCTS AND CHEMICALS LTD ; AIR PRODUCTS AND CHEMICALS

Inventor(s): (std): CHRISTOPHER GEOFFREY SPILSBURY ; GEOFFREY SPILSBURY CHRISTOPHER ; JULIAN ROBERTS MARK ; MARK JULIAN ROBERTS ; ROBERTS MARK ; ROBERTS MARK JULIAN ; ADAM ADRIAN BROSTOW ; ADRIAN BROSTOW ADAM ; ADRIAN ROBERTS MARK JULIAN SPI ; BROSTOW ADAM ; BROSTOW ADAM ADRIAN ; SPILSBURY CHRISTOPHER ; SPILSBURY CHRISTOPHER GEOFFREY ; SPILSBERI KRISTOFER DZHEFFRI ; ROBERTS MARK DZHULIAN ; BROSTOU ADAM ADRIAN

Inventor(s): ROBERTS MARK JULIAN SPILSBURY CHRISTOPHER... ; SPILSBURY,CHRISTOPHER GEOFFREY ; ROBERTS MARK JULIAN SPILSBURY CHRISTOPHER GEOFFREY

Agent(s): PIZZEYS; PIZZEYS PATENT AND TRADE MARK ATTORNEYS PTY LTD; MCFADDEN FINCHAM; OSLER HOSKIN AND HARCOURT LLP; BURFORD ANTHONY FREDERICK; AIR PRODUCTS AND CHEMICALS INC PATENT DEPARTMENT; WILLARD

Designated states: AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GW HR HU ID IE IL IN IS IT JP KE KG KP KR KZ LC LI LK LR LS LT LU LV MA MC MD MG MK ML MN MR MW MX MZ NA NE NI NL NO NZ OM PG PH PL PT RO RU SC SD SE SG SI SK SL SN SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN YU

Title: HYBRID **CYCLE** FOR THE PRODUCTION OF **LIQUEFIED NATURAL GAS**

Abstract: Refrigeration process for **gas liquefaction** which utilizes one or more vaporizing **refrigerant cycles** to provide refrigeration below about -40 degrees centigrade and a **gas expander cycle** to provide refrigeration below about -100 degrees centigrade. Each of these two types of **refrigerant** systems is utilized in an optimum temperature range which maximizes the efficiency of the particular system. A significant fraction of the total refrigeration power required to **liquefy** the feed **gas** (typically more than 5 percent and often more than 10 percent of the total) can be consumed by the vaporizing **refrigerant cycles**. The invention can be implemented in the design of a new **liquefaction** plant or can be utilized as a retrofit or **expansion** of an existing plant by adding **gas** expander refrigeration **circuit** to the existing plant refrigeration system.

Classifications:

International (IPC 8-9): F17C5/00 F25J1/00

F25J1/02 (Advanced/Invention);

F17C5/00 F25J1/00 (Advanced/Non-invention)

International (IPC 1-7): F17C5/00 F25J1/00 F25J1/02 F25J1/02 F25J3/06

CPC: F25J1/0052 F25J1/0022 F25J1/0037 F25J1/004 F25J1/0042

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F25J1/0291 F25J1/0292 F25J2220/62 F25J2220/64 F25J2245/02

European: F25J1/00A6 F25J1/00C2E2 F25J1/00C2F F25J1/00C2L

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US: 62/611 62/612

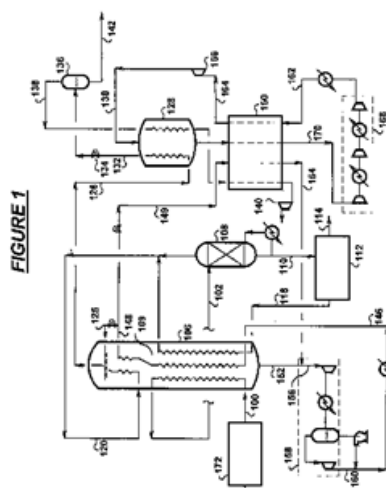
PatBase - US6308531_BA

U.S. Patent

Oct. 30, 2001

Sheet 1 of 9

US 6,308,531 B1



Family:

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Priority:

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Probable Assignee: AIR PRODUCTS AND CHEMICALS INC

Assignee(s): (std): AIR PROD AND CHEM

Assignee(s): AIR PROD AND CHEM INC ; AIR PRODUCTS AND CHEMICALS INC

Inventor(s): (std): AGRAWAL RAKESH ; ROBERTS MARK J ; ROBERTS MARK JULIAN

Inventor(s): MARK JULIAN ROBERTS ; RAKESH AGRAWAL

Agent(s): PIZZEYS; PIZZEYS PATENT AND TRADE MARK ATTORNEYS PTY LTD; SULEIMAN I AL AMMAR LAW OFFICE; NISHIYAMA MASAYA; ISHIDA TAKASHI; TSURUTA JUNICHI; HIGUCHI SOTOJI; FUKUMOTO TSUMORU; WILLARD

Designated states: AT BE CH CY DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE

Abstract: A method for **liquefaction** using a **closed loop** refrigeration system, the method comprising the steps of (a) compressing a gaseous **refrigerant** stream in at least one compressor; (b) **cooling** the compressed gaseous **refrigerant** stream in a **first heat** exchanger; (c) expanding at least a **first** portion of the **cooled**, compressed gaseous **refrigerant** stream from the **first heat** exchanger in a **first** expander to provide a **first** expanded gaseous **refrigerant** stream; and (d) **cooling** and substantially **liquefying** a feed **gas** stream to form a substantially **liquefied** feed **gas** stream in a **second heat** exchanger through indirect **heat** exchange against at least a **first** portion of the **first** expanded gaseous **refrigerant** stream from the **first** expander, wherein the **first** expanded gaseous **refrigerant** stream exiting the **first** expander is substantially vapor.

International (IPC 8-9): C10L3/00 C10L3/06 F25B9/06 F25B9/10
F25J1/00 F25J1/02 F25J5/00 (Advanced/Invention);
F25J1/00 F25J1/02 (Advanced/Non-invention);
F25J1/00 F25J1/02 F25J5/00 (Core/Invention);
F25J1/02 F25J5/00 (Core/Non-invention)

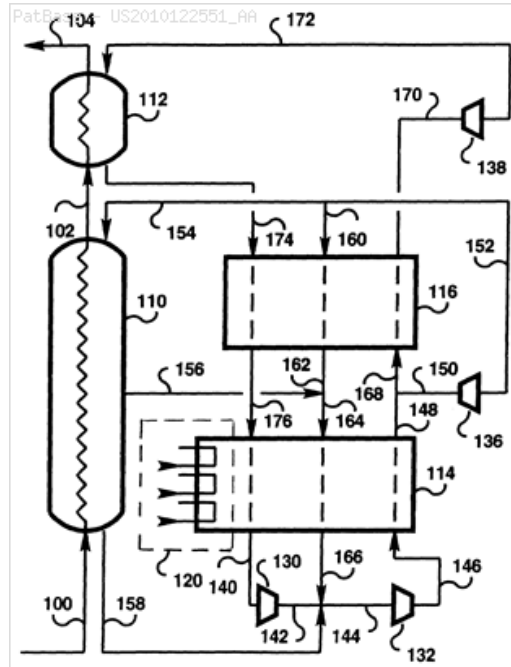
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F25J1/02Z6C4 F25J1/02Z6N R25J220/62 R25J230/08 R25J230/32
R25J230/16 R25J290/62

US: 62/606 62/611 62/612 62/613 62/613P 62/614 62/614S



Publication number	Publication date	Application number	Application date
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Priority:

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Probable Assignee: AIR PRODUCTS AND CHEMICALS INC

Assignee(s): (std): AIR PROD AND CHEM ; ROBERTS MARK JULIAN ; BROSTOW ADAM ADRIAN ; EHR PRODAKTS EHND KEMIKALZ INK

Assignee(s): AIR PRODUCTS AND CHEMICALS INC ; AIR PRODUCTS AND CHEMICALS INC US ; AIR PRODUCTS AND CHEMICALS INC 7201 HAMILTON BOULEVARD ALLENTOWN PA 18195-1501 US

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Inventor(s): ROBERTS MARK JULIANUS ; BROSTOW ADAM ADRIANUS

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Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CL CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LI LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PE PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN ST SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: **LNG** FACILITY PROVIDING ENHANCED LIQUID RECOVERY AND PRODUCT FLEXIBILITY

Abstract: A single **LNG** facility, and operating method therefor, capable of efficiently producing **LNG** products that meet the varying specifications of different **LNG** markets.

Classifications:

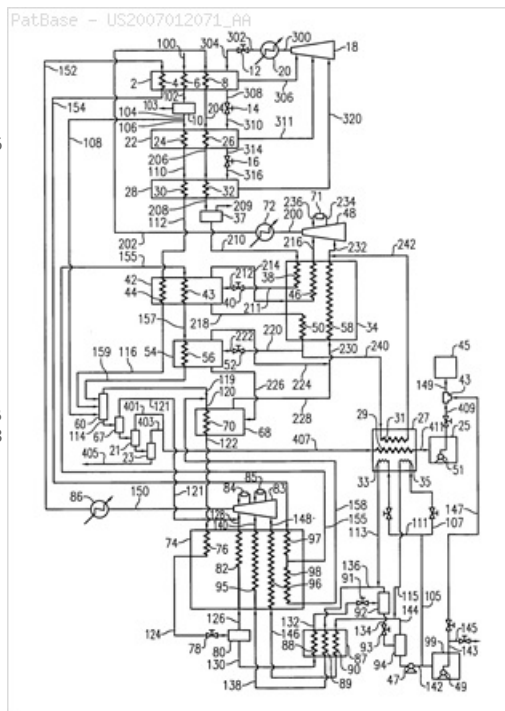
International (ipc 8-9): C10L1/04 C10L3/00 C10L3/06 F17C3/08 F25J1/00 F25J1/02 F25J3/00 F25J3/02 F25J5/00 (Advanced/Invention); F25J1/00 F25J3/00 (Advanced/Non-invention); C10L3/00 F17C3/00 F25J1/00 F25J3/00 (Core/Invention)

International (ipc 1-7): F25J1/00

CPC: F17C2221/033 F17C2223/0161 F17C2250/0456 F17C2270/0136 F25J1/0237 F25J1/0255 F25J2200/02 F25J2200/76 F25J2215/02 F25J2290/34 F25J1/0265 F25J1/0022 F25J1/0035 F25J1/004 F25J1/0045 F25J1/0052 F25J1/021 F25J1/0238 F25J3/0209 F25J3/0233 F25J3/0238 F25J3/0242 F25J3/0247 F25J2200/04 F25J2200/08 F25J2200/40 F25J2200/50 F25J2200/70 F25J2200/74 F25J2200/78 F25J2205/04 F25J2205/50 F25J2210/06 F25J2215/62 F25J2230/08 F25J2235/60 F25J2240/02 F25J2245/02 F25J2270/02 F25J2270/12 F25J2270/60 F25J2280/02 F25J2290/40 F25J2260/02 F25J1/0231

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US: 585/1 585/302 62/45.1 62/45.100S 62/611 62/611P 62/612 62/612P 62/612S 62/613 62/613P 62/620 62/620S 62/628



Family:

Publication number	Publication date	Application number	Application date
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Priority:

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Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): ELLIOT DOUGLAS G ; RANSBARGER WELDON L ; LEE RONG JWYN ; HUANG SHAWN S ; QUALLS WESLEY R ; JONES THOMAS M ; CROFTON HARRY J ; RANSBARGER WELDON ; GOUNDRY PHILIP C ; QUALLS WESLEY ; ELLIOT DOUG ; HUANG SHAWA S ; YAO JAME ; CHEN JONG J ; CHEN JONG JUH ; CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO

Assignee(s): CONOCOPHILLIPS CO SOC ORGANIZADA BAJO LAS LEYES DEL ESTADO DE DELAWARE ; CONOCOPHILLIPS COMPANY

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Inventor(s): DOUGLAS G ELLIOT ; JONG JUH CHEN ; SHAWN S HUANG ; QUALLS WESLEY R ELLIOT DOUGLAS G RANSBAGER WELDON L CHEN JONG JUH HUANG SHAWN S LEE RONG JWYN YAO JAME ; WESLEY R QUALLS ; WESLEY RQUALLS ; WELDON LRANSBARGER ; SHAWN SHUANG ; DOUGLAS GELLIOT ; CHEN JONG ; CROFTON HARRY ; ELLIOT DOUGLAS ; GOUNDRY PHILIP ; HUANG SHAWA ; HUANG SHAWM ; HUANG SHAWN ; JONES THOMAS ; RANSBAGER WELDON L

Agent(s): PHILLIPS ORMONDE FITZPATRICK; VILLASECA; SULEIMAN I AL AMMAR LAW OFFICE; CONOCOPHILIPS CO IP LEGAL; CONOCOPHILLIPS COMPANY; CONOCOPHILLIPS CO

Designated states: AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LK LR LS LT LU LV LY MA MC MD MG MK ML MN MR MW MX MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: METHODS, DEVICES AND SYSTEMS FOR EXTRACTION OF THERMAL ENERGY FROM A **HEAT** CONDUCTING METAL CONDUIT

Abstract: Provided are methods, devices and systems for controlled removal of thermal energy from a fluid within a thermally conducting metal conduit. The system allows for the in situ formation of a reversible plug that can stop the flow of fluid through the conduit, particularly without inducing thermally induced stress fractures or breaches in the conduit. The devices and systems include a thermal transfer device that can be adapted to be in thermal communication with a thermal conducting metal conduit containing a fluid, particularly a flowing fluid. The devices and systems allows for controlled re-**heating** of the conduit without inducing thermally induced stress fractures or breaches in the conduit to restore fluid flow through the conduit.

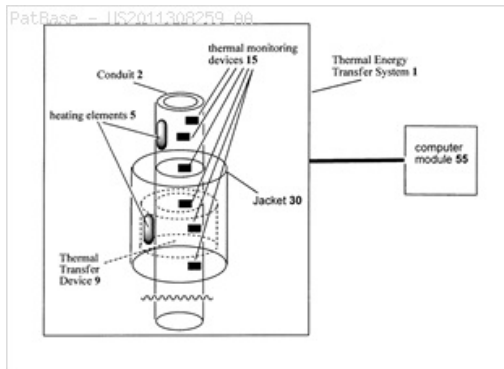
Classifications:

International (IPC 8-9): F15D1/02 F16L53/00 F16L55/00 F16L55/103 F16L55/164 F25B21/00 F25B21/02 F25B21/04 F25B29/00 F25C1/00 F25C1/18 F25D15/00 F25D3/10 F28D15/00 F28D7/10 F28F1/22 F28F11/00 F28F13/06 F28F13/10 F28F13/12 F28F27/02 F28F3/12 G05D23/00 G05D23/19 G5D23/19 H05B3/02 (Advanced/Invention); F25D15/00 (Core/Invention)

CPC: Y02B30/66 Y02B30/765 F16L55/103 G05D23/192 F28F13/06 F28D7/10 F25B21/02 F25B2321/002 F25D3/10 F25D15/00 Y10T137/0391

European: F16L55/103 G05D23/19E2

US: 137/13 137/13S 165/104.11 165/104.110S 165/109.1 165/109.100S 165/154 165/154S 165/168 165/168S 165/287 165/287S 165/61 165/61S 165/96 219/538 219/538S 62/293 62/3.1 62/3.100S 62/3.2 62/3.200S 62/3.3 62/3.300P 62/66 62/66S 62/67



Family:

Publication number	Publication date	Application number	Application date
BR112012031923 A2	20161108	BR20121131923	20110615
CA2802346 AA	20121211	CA20112802346	20110615
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CN103238019 A	20130807	CN201180039493	20110615
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EA026872 B1	20170531	EA20130000018	20110615
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US2014190663 AA	20140710	US20140208325	20140313
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US9528780 BB	20161227	US20150638177	20150304
WO11159355 A2	20111222	WO2011US01083	20110615
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Priority:

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Probable Assignee: BIOFILM IP LLC

Assignee(s): (std): BIOFILM IP LLC ; CUTBIRTH HENRY ; WRAY DANIEL X ; WRAY ROBERT J

Inventor(s): (std): CUTBIRTH HENRY ; WRAY DANIEL X ; WRAY ROBERT J

Inventor(s): DANIEL X WRAY ; HENRY CUTBIRTH ; ROBERT J WRAY

Agent(s): SMART AND BIGGAR; BALDOCK SHARON CLAIRE; STEPHANIE; MCKENNA LONG AND ALDRIDGE LLP; FRANK J; DENTONS US LLP; SEIDMAN STEPHANIE L ET AL

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CL CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LI LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PE PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN ST SV SY SZ TD TG TH TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

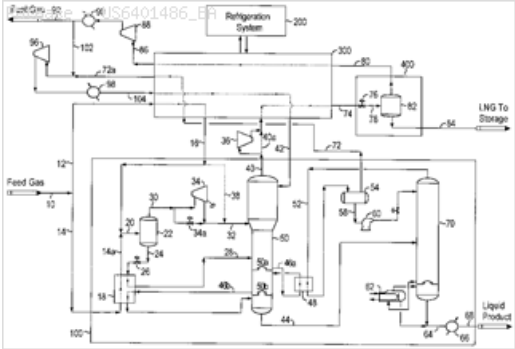
Title: ENHANCED NGL RECOVERY UTILIZING REFRIGERATION AND REFLUX FROM **LNG** PLANTS

Abstract: The present invention is directed to methods and apparatus for improving the recovery of the relatively less volatile components from a methane-rich **gas** feed under pressure to produce an NGL product while, at the same time, separately recovering the relatively more volatile components which are liquified to produce an **LNG** product. The methods of the present invention improve separation and efficiency within the NGL recovery column while maintaining column pressure to achieve efficient and economical utilization of the available mechanical refrigeration. The methods of the present invention are particularly useful for removing cyclohexane, benzene and other hazardous, heavy hydrocarbons from a **gas** feed. The benefits of the present invention are achieved by the introduction to the NGL recovery column of an enhanced liquid reflux lean on the NGL components. Further advantages can be achieved by thermally linking a side reboiler for the NGL recovery column with the overhead condenser for the NGL purifying column. Using the methods of the present invention, recoveries of propane and heavier components in excess of 95 percent are readily achievable.

Classifications:

International (IPC 8-9): F25J1/00 F25J1/02 F25J3/00 F25J3/02 (Advanced/Invention); F25J1/00 F25J3/02 (Core/Invention)
International (IPC 1-7): F25J1/00 F25J3/00
CPC: F25J1/0216 F25J1/0291 F25J1/0022 F25J1/0035 F25J1/004 F25J1/0052 F25J1/0055 F25J1/0087 F25J1/0212 F25J1/0219 F25J1/0238 F25J1/0262 F25J1/0265 F25J1/0267 F25J1/0283 F25J1/0292 F25J1/0294 F25J3/0209 F25J3/0233 F25J3/0238 F25J3/0242 F25J2200/02 F25J2200/04 F25J2200/50 F25J2200/72 F25J2200/74 F25J2200/76 F25J2200/78 F25J2205/04 F25J2210/06 F25J2215/62 F25J2220/60 F25J2230/08 F25J2230/60 F25J2240/02 F25J2270/12 F25J2270/60 F25J2270/66 F25J2270/88 F25J2280/02 F25J2290/12 F25J2290/32 F25J2260/02 F25J1/0231 F25J1/0085 F25J1/021

European: F25J1/00A6 F25J1/00C2E F25J1/00C2F F25J1/00C4V F25J1/00C4V2 F25J1/00R6E F25J1/00R6P F25J1/02 F25J1/02B10C F25J1/02D F25J1/02D10 F25J1/02D2 F25J1/02D4P F25J1/02K8D2 F25J1/02Z4H F25J1/02Z4H4R F25J1/02Z4H4R2 F25J1/02Z6A4 F25J1/02Z6J F25J1/02Z6L F25J1/02Z6N F25J3/02A2 F25J3/02C2 F25J3/02C4 F25J3/02C6 R25J200/02 R25J200/04 R25J200/50 R25J200/72 R25J200/74 R25J200/76 R25J200/78 R25J205/04 R25J210/06 R25J215/62 R25J220/60 R25J230/08 R25J230/60 R25J240/02 R25J270/12 R25J270/60 R25J270/66 R25J270/88 R25J280/02 R25J290/12 R25J290/32
US: 62/623 62/630



Family:

Publication number	Publication date	Application number	Application date
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EG23006 A	20031231	EG20010000512	20010516
MY135088 A	20080131	MY20010002361	20010517
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Priority:

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Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): CHEN JONG JUH ; LEE RONG JWYN ; PHILLIPS PETROLEUM CO ; PHILLIPS PETROLEUM COMPANY ; YAO JAME ; ELLIOT DOUGLAS G

Assignee(s): IPSI LLC ; CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO

Inventor(s): (std): ELLIOT DOUGLAS G ; JAME YAO ; JONG JUH CHEN ; LEE RONG JWYN ; RONG JWYN LEE ; YAO JAME ; JUH CHEN JONG ; CHEN JONG JUH

Inventor(s): DOUGLAS G ELLIOT

Agent(s): PHILLIPS ORMONDE FITZPATRICK

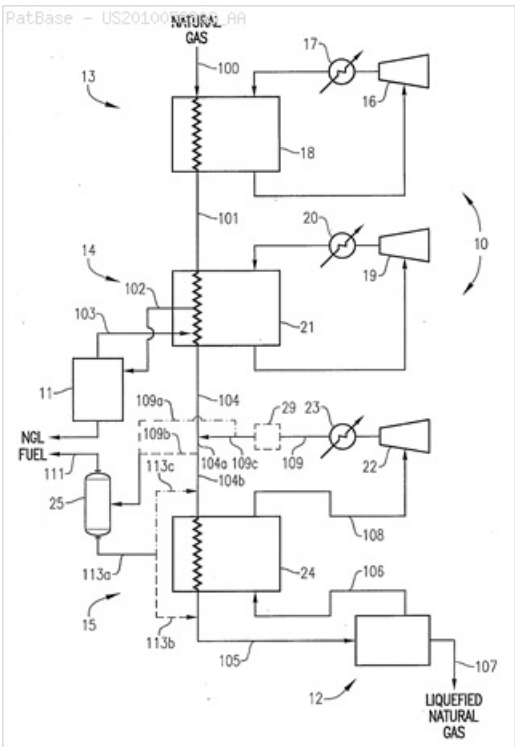
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Title: SYSTEM FOR INCONDENSABLE COMPONENT SEPARATION IN A LIQUEFIED NATURAL GAS FACILITY

Abstract: A liquefied natural gas (LNG) facility that employs a system to remove incondensable material from one or more refrigeration cycles within the facility. One or more embodiments of the present invention can be advantageously employed in an open-loop refrigeration cycle to remove at least a portion of one or more high vapor pressure components that have accumulated in the refrigerant cycle over time. In addition, several embodiments can be advantageously employed to stabilize facility operation in the event of drastic changes to the concentration of the natural gas feed stream introduced into the facility.

Classifications:

International (IPC 8-9): F25J F25J1/00 F25J1/02 (Advanced/Invention); F25J1/00 (Core/Invention); F25J (Subclass/Invention)
CPC: F25J1/021 F25J1/0022 F25J1/004 F25J1/0052 F25J1/0072 F25J1/0095 F25J1/023 F25J1/0231 F25J1/0249 F25J2220/62 F25J2220/64
European: F25J1/00A6 F25J1/00C2F F25J1/00C4V F25J1/00R4N F25J1/00R8 F25J1/02B10C3 F25J1/02K2C F25J1/02K2R F25J1/02Z2M8 R25J220/62 R25J220/64
US: 62/612 62/612P



Family:

Publication number	Publication date	Application number	Application date
AU2009288561 AA	20100311	AU20090288561	20090814
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US2010058803 AA	20100311	US20090554539	20090904
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WO10027629 A3	20130613	WO2009US53837	20090814

Priority:

US20080095189P 20080908 WO2009US53837 20090814 US20090554539 20090904

Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO ; EVANS MEGAN V ; RANSBARGER WELDON L ; PRADERIO ATTILIO J ; MESSERSMITH DAVID B ; KONOKOPHILLIPS KOMPANI

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Inventor(s): EVANS MEGAN VUS ; MESSERSMITH DAVID BUS ; PRADERIO ATTILIO JUS ; RANSBARGER WELDON LUS ; ATTILIO J PRADERIO ; DAVID B MESSERSMITH ; MEGAN V EVANS ; WELDON L RANSBARGER

Agent(s): PHILLIPS ORMONDE FITZPATRICK; OSLER HOSKIN AND HARCOURT LLP; REINHOLD COHN AND PARTNERS; CONOCOPHILLIPS COMPANY - IP SERVICES GROUP,ATTENTION: DOCKETING; CONOCOPHILLIPS CO IP SERVICES GROUP ATTENTION DOCKETING; CONOCOPHILLIPS CO; HALLER LAUREN E

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CL CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PE PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN ST SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: SYSTEM FOR ENHANCED **GAS** TURBINE PERFORMANCE IN A **LIQUEFIED NATURAL GAS** FACILITY

Abstract: A system for **liquefying natural gas** that includes a process and apparatus for enhancing the performance of one or more **gas** turbines. **Gas** turbine power output can be stabilized or even enhanced using the interstage **cooling** system configured according to one or more embodiments of the present invention. In one embodiment, partially compressed air from a lower compression stage of a **gas** turbine is **cooled** via indirect **heat** exchange with a primary **coolant** before being returned to a higher compression stage of the same **gas** turbine. Optionally, the interstage **cooling** system can employ one or more secondary **coolants** to remove the rejected **heat** from the primary **coolant** system.

Classifications:

International (IPC 8-9): F01D15/00 F02C7/143 F25J F25J1/00 F25J1/02 (Advanced/Invention);

F25J1/00 (Core/Invention);

F25J (Subclass/Invention)

CPC: F25J1/0052 F01D15/005 F02C7/143 F25J1/0022 F25J1/004

F25J1/0085 F25J1/0087 F25J1/021 F25J1/0236 F25J1/0242

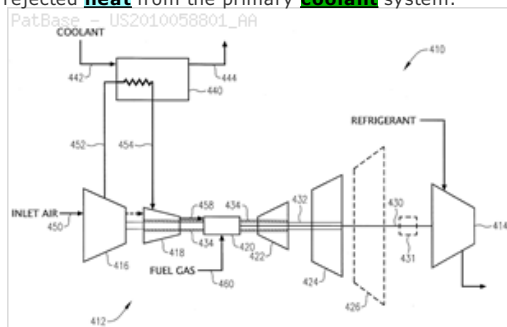
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European: F01D15/00B F02C7/143 F25J1/02 F25J1/02B10C

F25J1/02Z6A4 R25J220/64 R25J260/02 R25J270/08 R25J270/12

Y02T50/67F

US: 62/611 62/611P



Family:

Publication number	Publication date	Application number	Application date
AU2009292077 AA	20100318	AU20090292077	20090729
AU2009292077 BB	20150507	AU20090292077	20090729
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IL211007 A0	20110428	IL20090211007	20090729
IL211007 A1	20160131	IL20090211007	20090729
US2010058801 AA	20100311	US20090550098	20090828
US9841230 BB	20171212	US20090550098	20090828
WO10030441 A2	20100318	WO2009US52026	20090729
WO10030441 A3	20131121	WO2009US52026	20090729

Priority:

US20080095469P 20080909

WO2009US52026 20090729

US20090550098 20090828

Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO ; MASANI KARL D ; MEHER HOMJI CYRUS B

Assignee(s): CONOCOPHILLIPS COMPANY

Inventor(s): (std): MASANI KARL D ; MEHER HOMJI CYRUS B

Inventor(s): CYRUS B MEHER HOMJI ; KARL D MASANI

Agent(s): PHILLIPS ORMONDE FITZPATRICK; REINHOLD COHN AND PARTNERS; CONOCOPHILLIPS COMPANY - IP SERVICES GROUP,ATTENTION: DOCKETING; CONOCOPHILLIPS CO IP SERVICES GROUP ATTENTION DOCKETING; CONOCOPHILLIPS CO; HALLER LAUREN E

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CL CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PE PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN ST SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: CO₂ REFRIGERATION **CIRCUIT** WITH SUB-**COOLING** OF THE LIQUID **REFRIGERANT** AGAINST THE RECEIVER FLASH **GAS** AND METHOD FOR OPERATING THE SAME

Abstract: CO₂ refrigeration **circuit** (2) for circulating a **refrigerant** in a predetermined flow direction, comprising in flow direction a heat-rejecting **heat** exchange, (4), a receiver (10) having a liquid portion (12) and a flash **gas** portion (14), and subsequent to the receiver (10) a medium temperature **loop** (20) and a low temperature **loop** (24), wherein the medium and low temperature **loops** (24) each comprise in flow direction an **expansion** device (26, 28), an evaporator (30, 32) and a compressor (46, 38), the refrigeration **circuit** (2) further comprising a liquid line (16) connecting the liquid portion (12) of the receiver (10) with at least one of the medium and low temperature **loops** (20, 24) and having an internal **heat** exchanger (54), and a flash **gas** line (50) connecting the flash **gas** portion (14) of the receiver (10) via the internal **heat** exchanger (54) with the inlet of the low temperature compressor (46), wherein the internal **heat** exchanger (54) transfers in use **heat** from the liquid flowing through the liquid line (16) to the flash **gas** flowing through the flash **gas** line (50).

Classifications:

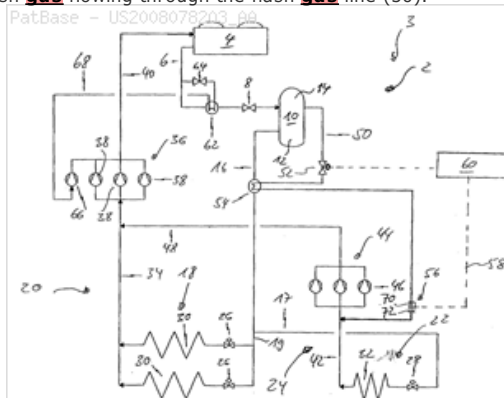
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International (IPC 1-7): F25B1/10 F25B41/04 F25B9/00

CPC: F25B40/02 F25B40/06 F25B2600/2509 F25B5/02 F25B40/04 F25B49/022 F25B2309/061 F25B2400/075 F25B2400/13 F25B2400/22 F25B2400/23 F25B9/008 F25B1/005 F25B41/04 F25B1/10

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US: 1/1 62/115 62/115P 62/117 62/117P 62/196.4 62/196.400P 62/228.3 62/335 62/498 62/498S 62/509 62/509S 62/510 62/510P



Family:

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EP2264385 A2	20101222	EP20100181303	20050729
EP2264385 A3	20111019	EP20100181303	20050729
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US2015013359 AA	20150115	US20140499852	20140929
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Priority:

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WO2005EP01724	20050218	WO2005US05413	20050218	EP20050775838	20050729
WO2005EP08255	20050729	US20070659926	20070209	US20080659926	20080102
US20110227550	20110908	US20140499826	20140929	US20140499852	20140929

Probable Assignee: CARRIER CORP

Assignee(s): (std): LINDE KALTETECHNIK GMBH AND CO ; GERNEMANN ANDREAS ; HEINBOKEL BERND ; SCHIERHORN UWE ; LINDE KALTETECHNIK GMBH ; LINDE KALTETECHNIK GMBH ; CARRIER CORP ; DURAISAMY SURESH ; KEHRRIER CORP

Assignee(s): LINDE KALTETECHNIK GMBH AND CO KG ; CARRIER FARMINGTON CORP ; CARRIER KALTETECHNIK DEUTSCHLAND GMBH ; KEHRRIER KOPOREJSHN

Inventor(s): (std): SURESH DURAISAMY ; UWE GERNEMANN ANDREAS HEINBOKE ; UWE SCHIERHORN ; SCHIERHORN UWE ; HEINBOKEL BERND ; GERNEMANN ANDREAS ; DURAISAMY SURESH ; BERND HEINBOKEL ; ANDREAS GERNEMANN

Inventor(s): GERNEMANN ANDREAS HEINBOKEL BERND SCHIERHORN UWE ; DIE ERFINDERNENNUNG LIEGT NOCH NICHT VOR ; DURAISAMY SURESH C O CARRIER FARMINGTON CORP ; DURAISAMY SURESH C O CARRIER CORPORATION

Agent(s): PHILLIPS ORMONDE FITZPATRICK; KSNH PATENTANWAELTE KLUNKER SCHMITT NILSON HIRSCH; KLUNKER SCHMITT NILSON HIRSCH; KLUNKER HANS FRIEDRICH; SCHMITT NILSON SCHRAUD WAIBEL WOHLFROM PATENTANWAELTE PARTNERSCHAFT MBB; HOEHFELD JOCHEN; BACHMAN AND LAPOINTE PC UTC; BACHMAN AND LAPOINTE PC

Designated states: AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GW HR HU ID IE IL IN IS IT JP KE KG KM KP KR KZ LC LI LK LR LS LT LU LV MA MC MD MG MK ML MN MR MW MX MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RU SC SD SE SG SI SK SL SM SN SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN YU ZA ZM ZW

Title: IMPROVED MULTI-COMPONENT REFRIGERATION PROCESS FOR LIQUEFACTION OF NATURAL GAS

Abstract: This invention relates to a process for liquefying a pressurized gas stream rich in methane in which the liquefaction of the gas stream occurs in a heat exchanger being cooled by a closed-loop multi-component refrigeration system to produce a methane-rich liquid product having a temperature above about -112 DEG C. (-170 DEG F.) and a pressure sufficient for the liquid product to be at or below its bubble point. The liquefied gas product is then introduced to a storage means at a temperature above about -112 DEG C. (-170 DEG F.).

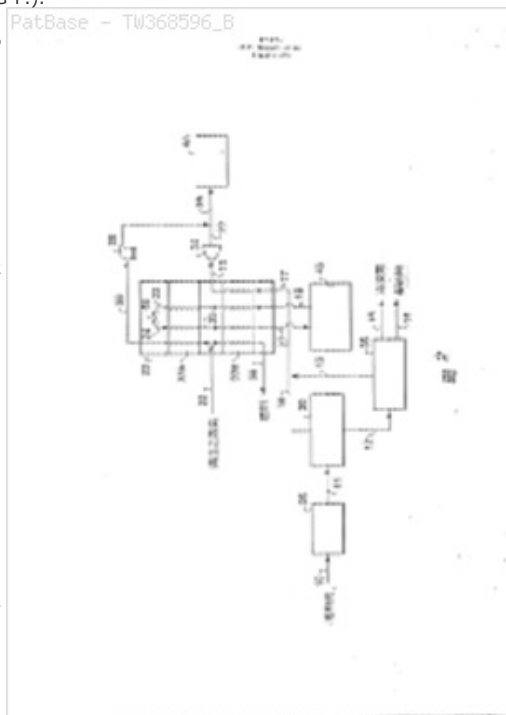
Classifications:

International (ipc 8-9): B23K35/30 B23K9/173 B60K15/03 C10L3/06 C22C38/00 C22C38/04 C22C38/06 C22C38/08 C22C38/12 C22C38/14 C22C38/16 F17C1/00 F17C1/14 F17C13/00 F17C3/00 F17C3/02 F17C7/00 F17C7/02 F17C9/00 F17D1/08 F25J1/00 F25J1/02 F25J3/02 (Advanced/Invention); F17C9/00 F25J1/00 F25J3/02 (Advanced/Non-invention); F25J1/02 (Core/Non-invention)

International (ipc 1-7): C10L3/06 F17C13/00 F17C9/00 F25J1/00 F25J1/02 F25J3/00 F25J3/02 F25J3/06

CPC: F25J1/0035 F25J1/0085 F25J1/0087 F25J1/0095 B23K9/173 B23K35/3066 B60K15/03006 C22C38/001 C22C38/04 C22C38/06 C22C38/08 C22C38/12 C22C38/14 C22C38/16 F17C1/00 F17C1/002 F17C1/14 F17C3/00 F17C3/025 F17C7/00 F17C7/02 F17C13/001 F17C2203/0648 F17C2205/0323 F17C2221/033 F17C2223/0123 F17C2223/033 F17C2223/035 F17C2225/0123 F17C2225/0161 F17C2225/033 F17C2225/035 F17C2250/03 F17C2260/046 F17C2265/017 F17C2265/022 F17C2265/033 F17C2265/034 F17C2265/035 F17C2265/036 F17C2265/037 F17C2265/066 F17C2265/068 F17C2270/0105 F17C2270/0171 F17C2270/0173 F17D1/082 F25J1/0022 F25J1/0042 F25J1/0052 F25J1/0055 F25J1/0212 F25J1/0231 F25J1/025 F25J1/0254 F25J1/0291 F25J1/0292 F25J2205/04 F25J2205/50 F25J2220/64 F25J2230/08 F25J2230/60 F25J2235/60 F25J2245/90 F25J2290/62 F25J2210/04 F25J1/004 F25J1/0215 F25J1/0219 F25J2245/02

European: B23K35/30H4 B23K9/173 B60K15/03B C22C38/00B C22C38/04 C22C38/06 C22C38/08 C22C38/12 C22C38/14 C22C38/16 F17C1/00 F17C1/00B F17C1/14 F17C13/00B F17C3/00 F17C3/02C F17C7/00 F17C7/02 F17D1/08B F25J1/00A6 F25J1/00C2L F25J1/00C4V F25J1/00C4V2 F25J1/02D F25J1/02D2 F25J1/02D4P F25J1/02K2R F25J1/02Z2M8P F25J1/02Z2T F25J1/02Z6J F25J1/02Z6L R17C203/06B1C R17C205/03L5 R17C221/03B1 R17C223/01A3 R17C223/03B R17C223/03C R17C225/01A3 R17C225/01B1B R17C225/03B R17C225/03C R17C250/03 R17C260/04C R17C265/01B1 R17C265/02A R17C265/03B1 R17C265/03B1A R17C265/03B1B R17C265/03B2 R17C265/03B3 R17C265/06D R17C265/06E R17C270/01A1 R17C270/01D1A R17C270/01D1B R25J205/04 R25J205/50 R25J220/64 R25J230/08 R25J230/60 R25J235/60 R25J245/90 R25J290/62

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AU199882598 A1	19990104	AU19980082598	19980618
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EP0988497 A1	20000329	EP19980932793	19980618
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IL133335 A0	20010430	IL19980133335	19980618
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Priority:

US19970050280P 19970620 US19980079782P 19980327 WO1998US12872 19980618

Probable Assignee: EXXON MOBIL CORP

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Assignee(s): EXXON MOBIL UPSTREAM RESEARCH COMPANY ; BOWEN RONALD R ; COLE ERIC T ; EXXON MOBIL CORP ; EXXONMOBIL UPSTREAM RESEARCH COMPANY ; EXXONMOBIL UPSTREAM RESEARCH CO ; EXXON PRODUCTION RESEARCH COMPANYUS ; KELLEY LONNY R ; EXXONMOBIL UPSTREAM RESEARCH CO HOUSTON TEXAS ; KIMBLE EDWARD L ; THOMAS EUGENE R ; EXXON PRODUCTION RESEARCH CO HOUSTON ; EXXONMOBIL UPSTREAM RESEARCH COMPANY HOUSTON TEXAS ; EXXON PRODUCTION RESEARCH COMPANY HOUSTON TEXAS

Inventor(s): (std): BOWEN RONALD R ; COLE ERIC T ; EDWARD L KIMBLE ; ERIC T COLE ; EUGENE R THOMAS ; KELLEY LONNEY R ; KELLEY LONNY R ; KELLEY LONNY RAY ; KELLY LONNY R ; KIMBLE EDWARD L ; KIMBLE EDWARD LAWRENCE ; LONNY R KELLEY ; OWEN RONALD R ; RONALD R BOWEN ; THOMAS EUGENE R

Inventor(s): R KELLEY LONNY ; LONNY RAY KELLEY

Agent(s): WATERMARK PATENT AND TRADE MARKS ATTORNEYS; WATERMARK INTELLECTUAL PROPERTY PTY LTD; BORDEN LADNER GERVAIS LLP; JOSE ANTONIO LLOREDA; REINHOLD COHN AND PARTNERS

Designated states: AM AT AZ BE BF BJ BY CF CG CH CI CM CY DE DK ES FI FR GA GB GH GR IE IT KE KG KZ LU MC MD MR NE NL PT RU SD SE SN SZ TG TJ UG ZW

Title: INTEGRATED PRE-COOLED MIXED REFRIGERANT SYSTEM AND METHOD

Abstract: A system and method for **cooling** and **liquefying** a **gas** in a **heat** exchanger that includes compressing and **cooling** a **mixed refrigerant** using **first** and last compression and **cooling cycles** so that high pressure liquid and vapor streams are formed. The high pressure liquid and vapor streams are **cooled** in the **heat** exchanger and then expanded so that a primary refrigeration stream is provided in the **heat** exchanger. The **mixed refrigerant** is **cooled** and equilibrated between the **first** and last compression and **cooling cycles** so that a pre-cool liquid stream is formed and **subcooled** in the **heat** exchanger. The stream is then expanded and passed through the **heat** exchanger as a pre-cool refrigeration stream. A stream of **gas** is passed through the **heat** exchanger in countercurrent **heat** exchange with the primary refrigeration stream and the pre-cool refrigeration stream so that the **gas** is **cooled**. A resulting vapor stream from the primary refrigeration stream passage and a two-phase stream from the pre-cool refrigeration stream passage exit the warm end of the exchanger and are combined and undergo a simultaneous **heat** and mass transfer operation prior to the **first** compression and **cooling cycle** so that a reduced temperature vapor stream is provided to the **first** stage compressor so as to lower power consumption by the system. Additionally, the warm end of the **cooling** curve is nearly **closed** further reducing power consumption. Heavy components of the **refrigerant** are also kept out of the cold end of the process, reducing the possibility of **refrigerant** freezing, as well as facilitating a **refrigerant** management scheme.

Classifications:**International (IPC 8-9):** C10L3/06 F25B1/00 F25B27/00 F25B5/02

F25J1/00 F25J1/02 F25J5/00 (Advanced/Invention);

F25B1/00 F25B27/00 F25J1/00 F25J5/00 (Core/Invention)

International (IPC 1-7): F25J1/02**CPC:** F25J1/0292 F25J2270/66 F25J1/0012 F25J1/0015 F25J1/0212

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F25J2220/62 F25J2220/64 F25J1/02 F25J5/00 F25J1/0022 F25J1/0218

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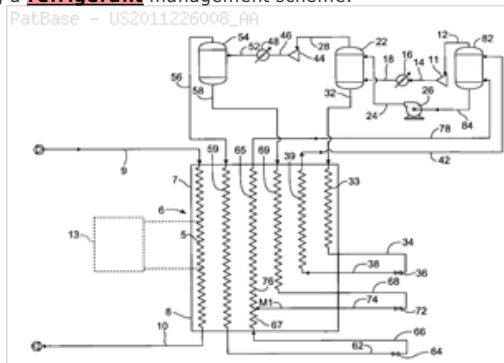
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F25J1/02D2 F25J1/02Z6 F25J1/02Z6J R25J205/90

US: 1/1 62/612 62/613 62/613P

PatBase - US2011226008_AA

**Family:**

Publication number	Publication date	Application number	Application date
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US2017051968 AA	20170223	US20160345957	20161108
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Priority:

US20100726142 20100317 CN201180023625 20110304 JP20130500070T 20110304
WO2011US27162 20110304 US20160227235 20160803 US20160345957 20161108

Probable Assignee: CHART INC

Assignee(s): (std): CHART ENERGY AND CHEMICALS INC ; CHART INC ; DUCOTE DOUG DOUGLAS JR ; GUSHANAS TIM ;
PODOLSKI JAMES ; DUCOTE JR DOUG DOUGLAS

Assignee(s): JPMORGAN CHASE BANK NA ADMINISTRATIVE AGENT AS

Inventor(s): (std): DOUGLAS A DUCOTE JR ; DUCOTE DOUG DOUGLAS ; DUCOTE DOUG DOUGLAS JR ; DUCOTE
DOUGLAS A JR ; DUCOTE JR DOUGLAS A ; GUSHANAS TIM ; GUSHANAS TIMOTHY P ; JAMES
PODOLSKI ; PODOLSKI JAMES ; TIMOTHY P GUSHANAS ; TIM GUSHANAS ; DOUG DOUGLAS DUCOTE
JR ; DUCOTE JR DOUG DOUGLAS

Agent(s): SPRUSON AND FERGUSON; BLAKE CASSELS AND GRAYDON LLP; Dauncey Mark Peter; HOSHINO
OSAMU; ONO SHINJIRO; TOMITA HIROYUKI; KOBAYASHI YASUSHI; MIYAMAE TORU; YAMAMOTO
OSAMU; TAKEUCHI SHIGEO; COOK ALEX LTD; JOHNSTON BLAKE R

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CL CM CN CO CR CU
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SV SY SZ TD TG TH TJ TM TN TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: NITROGEN REJECTION SYSTEM FOR LIQUIFIED **NATURAL GAS**

Abstract: This invention concerns a method and an apparatus for removing nitrogen and other low boiling point inorganic components from pressurized **LNG**-bearing streams and streams produced therefrom. The removal of such components is accomplished via a novel pressure reduction/stripping methodology thereby producing at least one low BTU nitrogen-rich **gas** stream and at least one high BTU methane-rich stream which is suitable for recycle to an open methane **cycle liquefaction** process and/or employment as a high quality fuel **gas**.

Classifications:**International (IPC 8-9):** F25J1/02 F25J3/00

F25J3/02 (Advanced/Invention);

F25J1/00 F25J3/02 (Core/Invention)

International (IPC 1-7): F25J3/00**CPC:** F25J1/023 F25J2200/40 F25J2210/06 F25J3/029 F25J1/0022

F25J1/004 F25J1/0052 F25J1/021 F25J1/0265 F25J1/0284 F25J3/0209

F25J3/0233 F25J3/0257 F25J2200/08 F25J2200/70 F25J2200/78

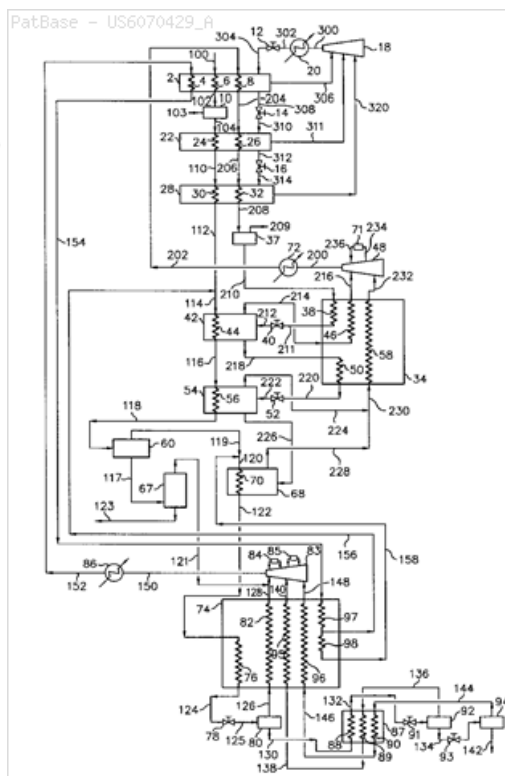
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F25J2245/02

European: F25J1/00A6 F25J1/00C2F F25J1/00C4V F25J1/02B10C3

F25J1/02Z6A6 F25J3/02 F25J3/02A2 F25J3/02C12 F25J3/02C2

F25J3/02C30H F25J3/06

US: 62/612 62/619**Family:**

Publication number	Publication date	Application number	Application date
AU200040356 A1	20001016	AU20000040356	20000328
AU200040356 A5	20001016	AU20000040356	20000328
AU755215 B2	20021205	AU20000040356	20000328
BRPI0009478 A	20020219	BR2000PI09478	20000328
CA2367347 AA	20010907	CA20002367347	20000328
CA2367347 C	20040817	CA20002367347	20000328
NO20014744 A	20011123	NO20010004744	20010928
NO20014744 A0	20010928	NO20010004744	20010928
NO334275 B1	20140127	NO20010004744	20010928
US6070429 A	20000606	US19990281024	19990330
WO0058674 A1	20001005	WO2000US08144	20000328

Priority:

US19990281024 19990330 WO2000US08144 20000328

Probable Assignee: CONOCO PHILLIPS CO**Assignee(s):** (std): CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO ; LOW WILLIAM R ; PHILLIPS PETROLEUM CO ; YAO JAME**Assignee(s):** PHILLIPS PETROLEUM COMPANY**Inventor(s):** (std): JAME YAO ; LOW WILLIAM R ; WILLIAM R LOW ; YAO JAME**Agent(s):** PHILLIPS ORMONDE FITZPATRICK; OSLER HOSKIN AND HARCOURT LLP**Designated states:** AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BY CA CF CG CH CI CM CN CR CU CY CZ DE DK DM DZ EE ES FI FR GA GB GD GE GH GM GN GR GW HR HU ID IE IL IN IS IT JP KE KG KP KR KZ LC LK LR LS LT LU LV MA MC MD MG MK ML MN MR MW MX NE NL NO NZ PL PT RO RU SD SE SG SI SK SL SN SZ TD TG TJ TM TR TT TZ UA UG US UZ VN YU ZA ZW

Title: DOMESTIC **gas** PRODUCT FROM AN **LNG** FACILITY

Abstract: An **LNG** facility capable of producing a domestic **gas** product from an intermediate stream in the **LNG** facility. Withdrawing the domestic **gas** product from a location within the **LNG** facility can minimize operational disturbances typically caused by extracting a domestic **gas** product stream upstream of the **liquefaction** portion of the **LNG** facility. In addition, withdrawing the domestic **gas** product from this location can provide increased control of light contaminants (e.g., nitrogen) in open-**loop** refrigeration **cycles** and can ultimately result in incremental **LNG** and/or NGL production.

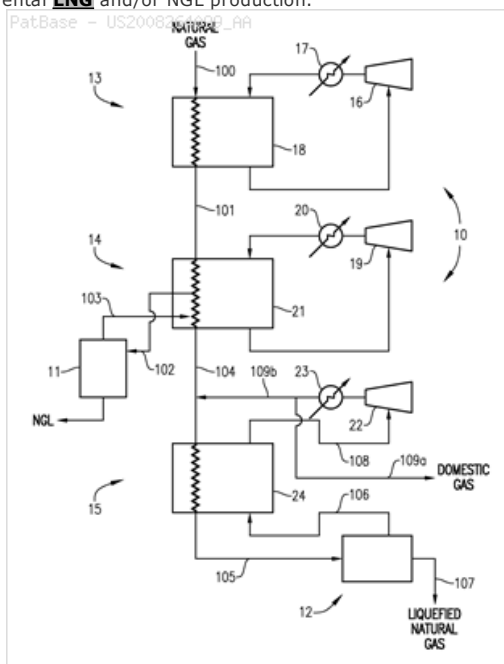
Classifications:

International (IPC 8-9): F25J1/00 (Advanced/Invention); F25J1/00 (Core/Invention)

CPC: F25J1/0022 F25J1/004 F25J1/0052 F25J1/021 F25J1/023 F25J1/0283 F25J2220/64 F25J2245/02

European: F25J1/00A6 F25J1/00C2F F25J1/00C4V F25J1/02B10C3 F25J1/02K2C F25J1/02Z6A4 R25J220/64 R25J245/02

US: 62/611 62/611P



Family:

Publication number	Publication date	Application number	Application date
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AU2008246020 BB	20120426	AU20080246020	20080319
EG25499 A	20120122	EG20090101559	20091021
US2008264099 AA	20081030	US20070739488	20070424
WO08134136 A1	20081106	WO2008US57479	20080319

Priority:

US20070739488 20070424 WO2008US57479 20080319

Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): EVANS MEGAN V ; STRASSLE LISA M ; RANSBARGER WELDON L ; MOCK JON M ; ORTEGO JAMES D ; FAJARDO ELICIA ; CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO

Assignee(s): CONOCOPHILLIPS COMPANY

Inventor(s): (std): STRASSLE LISA M ; RANSBARGER WELDON L ; ORTEGO JAMES D ; MOCK JON M ; FAJARDO ELICIA ; EVANS MEGAN V

Inventor(s): ELICIA FAJARDO ; JAMES D ORTEGO ; JON M MOCK ; LISA M STRASSLE ; MEGAN V EVANS ; WELDON L RANSBARGER

Agent(s): PHILLIPS ORMONDE FITZPATRICK; CONOCOPHILLIPS COMPANY - IP SERVICES GROUP, ATTENTION: DOCKETING; CONOCOPHILLIPS CO IP SERVICES GROUP ATTENTION DOCKETING; KELLY KAMERON D

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: FEED **GAS** DRIER PRECOOLING IN **MIXED REFRIGERANT NATURAL GAS LIQUEFACTION** PROCESSES

Abstract: A **closed loop** (100, 106, 108, 112, 116, 118) single component, e.g. propane or Freon **refrigerant**, refrigeration **cycle** is added to a single or dual **mixed refrigerant natural gas liquefaction** process to precool (in 100) the **natural gas** prior to adsorptive drying. By means of pressure control (104), the single component **refrigerant** temperature can be accurately controlled to ensure against hydrate formation in the **natural gas** feed and to maximize the precooling of the **natural gas** feed prior to drying. The addition of the single component refrigeration **cycle** overcomes the difficulty of controlling the precooling temperature which occurs when **cooling** by a multicomponent **refrigerant**, and thus improves plant reliability and minimizes the equipment sizes associated with the drying operation.

Classifications:

International (IPC 8-9): B01D53/26 F25J1/00 F25J1/02

F25J3/06 (Advanced/Invention);

F25J1/00 (Advanced/Non-invention);

B01D53/26 F25J1/00 (Core/Invention)

International (IPC 1-7): B01D53/26 F25J1/00 F25J1/02 F25J3/00 F25J3/06

CPC: F25J1/0022 F25J1/0055 F25J1/0087 F25J1/0216 F25J1/0263

F25J1/0279 B01D53/265 F25J1/0215 F25J1/0267 F25J1/0268

F25J1/0291 F25J1/0295 F25J2220/62 F25J2220/64 F25J2270/90

F25J2290/62

European: B01D53/26D F25J1/02D F25J1/02D4P F25J1/02D6P

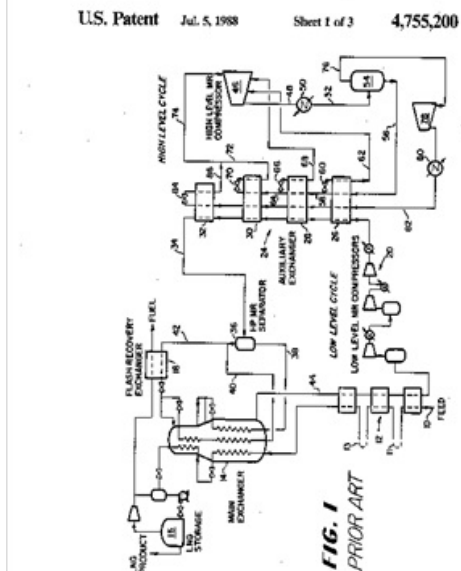
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R25J205/02 R25J220/62 R25J220/64 R25J270/12 R25J270/18

R25J270/60 R25J270/90 R25J280/02 R25J290/62

US: 62/11 62/335 62/434 62/612

PatBase - US4755200_R



Family:

Publication number	Publication date	Application number	Application date
AU198811995 A1	19880915	AU19880011995	19880219
AU586136 B2	19890629	AU19880011995	19880219
CA1300490 A1	19920512	CA19880559502	19880222
DE3860715 D1	19901108	DE19883860715	19880219
DZ1183 A1	20040913	DZ19880000019	19880224
EP0281821 A1	19880914	EP19880102474	19880219
EP0281821 B1	19901003	EP19880102474	19880219
FR2611386 A1	19880902	FR19880002393	19880226
FR2611386 B1	19890713	FR19880002393	19880226
JP1219488 A2	19890901	JP19880040546	19880223
JP1936308 C3	19950526	JP19880040546	19880223
JP6068431 B4	19940831	JP19880040546	19880223
KR19880010302 A	19881008	KR19880002054	19880227
KR910004397 B1	19910627	KR19880002054	19880227
NO165613 B	19901126	NO19880000842	19880226
NO165613 C	19910306	NO19880000842	19880226
NO880842 A	19880829	NO19880000842	19880226
NO880842 A0	19880226	NO19880000842	19880226
US4755200 A	19880705	US19870020286	19870227

Priority:

US19870020286 19870227 CA19880559502 19880222

Probable Assignee: AIR PRODUCTS AND CHEMICALS INC

Assignee(s): (std): AIR PROD AND CHEM

Assignee(s): AIR PROD AND CHEM INC ; AIR PRODUCTS AND CHEMICALS INC ; AIR PRODUCTS AND CHEMICALS INC A CORP OF DE ; AIR PRODUCTS AND CHEMICALS INC ALLENTOWN PA US ; AIR PRODUCTS CHEMICAL INC ; LIU YU NAN ; NEWTON CHARLES LEO

Inventor(s): (std): NEWTON CHARLES L ; NEWTON CHARLES LEO ; CHIYAARUSU REO NIYUUTON ; LIU YU NAN ; YUUNAN RIYUU

Inventor(s): CHARLES LEO NEWTON ; LIU YU NAN WHITEHALL PA 18052 US ; NEWTON CHARLES LEO PANAMA CITY FL 32407 US ; YU NAN LIU

Agent(s): PIZZEYS; PIZZEYS PATENT AND TRADE MARK ATTORNEYS PTY LTD; MCFADDEN FINCHAM; OSLER HOSKIN AND HARCOURT LLP

Designated states: BE DE GB IT NL

Title: SYSTEM FOR ENHANCED FUEL **GAS** COMPOSITION CONTROL IN AN **LNG** FACILITY

Abstract: An **LNG** facility employing an enhanced fuel **gas** control system. The enhanced fuel **gas** control system is operable to produce fuel **gas** having a substantially constant Modified Wobbe Index (MWI) during start-up and steady-state operation of the **LNG** facility by processing one or more intermediate process streams in a fuel **gas separator**. In one embodiment, the fuel **gas separator** employs a hydrocarbon-separating membrane, which can remove heavy hydrocarbons and/or concentrate nitrogen from the incoming process streams.

Classifications:

International (IPC 8-9): F02C7/26 F25J1/00 F25J1/02

F25J3/00 (Advanced/Invention);

F25J1/00 F25J3/00 (Core/Invention)

CPC: F25J1/0022 F25J1/004 F25J1/0052 F25J1/021 F25J1/023

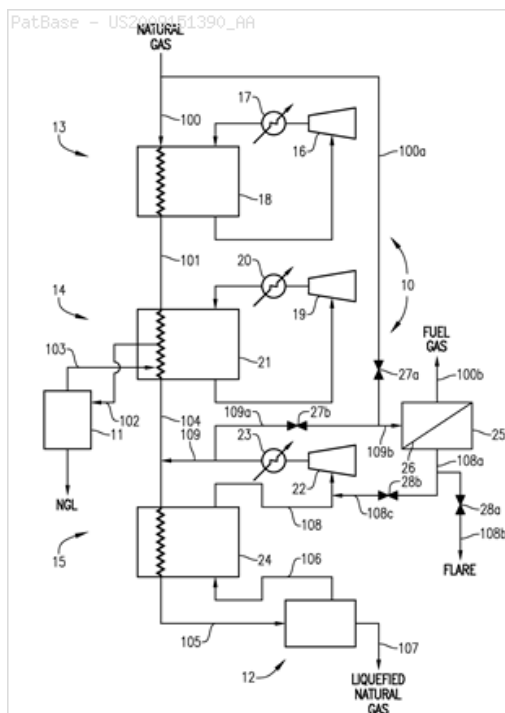
F25J1/0283 F25J2205/40 F25J2205/80 F25J2210/06 F25J2220/62

F25J2220/64 F25J2245/02 F25J2280/10

European: F25J1/00A6 F25J1/00C2F F25J1/00C4V F25J1/02B10C3

F25J1/02K2C F25J1/02Z6A4

US: 60/776 62/611 62/611P 62/612 62/618 62/618S



Family:

Publication number	Publication date	Application number	Application date
US2009151390 AA	20090618	US20070955141	20071212
US8381543 BB	20130226	US20070955141	20071212
WO09076501 A2	20090618	WO2008US86369	20081211
WO09076501 A3	20091126	WO2008US86369	20081211

Priority:

US20070955141 20071212

Probable Assignee: CONOCO PHILLIPS CO

Assignee(s): (std): CONOCO PHILLIPS CO ; CONOCOPHILLIPS CO ; MOCK JON M ; RANSBARGER WELDON L

Assignee(s): CONOCOPHILLIPS COMPANY

Inventor(s): (std): MOCK JON M ; RANSBARGER WELDON L

Agent(s): CONOCOPHILLIPS COMPANY - IP SERVICES GROUP,ATTENTION: DOCKETING; CONOCOPHILLIPS CO
IP SERVICES GROUP ATTENTION DOCKETING; CONOCOPHILLIPS COMPANY; CONOCOPHILLIPS CO;
BALL JOHN W

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU
CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL
IN IS IT JP KE KG KM KN KP KR KZ LA LC LK LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW
MX MY MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN ST SV SY
SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: METHOD AND SYSTEM FOR PRODUCING **LNG**

Abstract: A method is described for production of **LNG** from an incoming feed **gas** (1) on an onshore or offshore installation, and it is characterised by the following steps: 1) the feed **gas** is led through a fractionation column (150) where it is **cooled** a separated in an overhead fraction with a reduced content of pentane (C5) and heavier components, and a bottom fraction enriched with heavier hydrocarbons, 2) the overhead fraction from the fractionation column is fed to a **heat** exchanger system (110) and is subjected to a partial condensation to form a two-**phase** fluid, and the two-**phase** fluid is separated in a suitable **separator** (160) a liquid (5) rich in LPG and pentane (C3-C5) which is re-circulated as cold reflux to the fractionation column (150), while the **gas** (6) containing lower amounts of C5 hydrocarbons and hydrocarbons heavier than C5 is exported for further processing in the **heat** exchanger system (110) for **liquefaction** to **LNG** with a maximum content of ethane and LPG 3) the **cooling circuit** for **liquefaction** of **gas** in the **heat** exchanger system comprises an open or **closed gas expansion** process with at least one **gas expansion** step. A system for carrying out the method is also described.

Classifications:

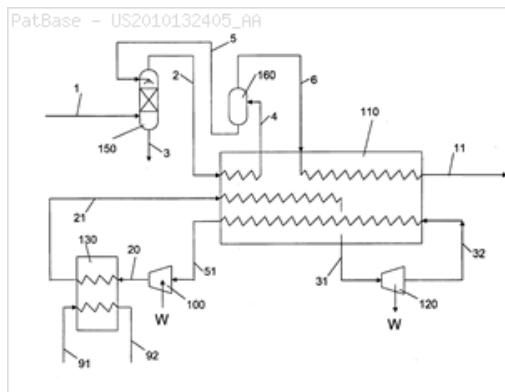
International (IPC 8-9): B01D3/14 C10L3/08 F25J1/00 F25J1/02 F25J3/02 (Advanced/Invention); B01D3/14 C10L3/08 F25J1/02 F25J3/02 (Advanced/Non-invention); B01D3/14 C10L3/00 F25J1/00 F25J3/02 (Core/Invention)

International (IPC 1-7): F25J3/02

CPC: F25J1/0288 F25J1/0022 F25J1/005 F25J1/0052 F25J1/0057 F25J1/0072 F25J1/0204 F25J1/0205 F25J1/0212 F25J1/0215 F25J1/0232 F25J1/0238 F25J1/0241 F25J1/0278 F25J1/0281 F25J1/0294 F25J2220/64 F25J2270/16 F25J2270/90 F25J1/0037 F25J1/0082 F25J1/0092 F25J1/0097 F25J1/0201 F25J1/0202 F25J1/0216 F25J2210/06 F25J1/02 B01D3/14 C10L3/08 F25J3/02

European: F25J1/00A6 F25J1/00C4E F25J1/00C4V F25J1/00C4V4 F25J1/00R4N F25J1/02 F25J1/02B2 F25J1/02B4 F25J1/02D F25J1/02D2 F25J1/02D4P F25J1/02F F25J1/02K4 F25J1/02K8D2 F25J1/02K8D4R F25J1/02Z4U4F F25J1/02Z6A F25J1/02Z6C4 F25J1/02Z6N R25J210/60 R25J220/64 R25J270/16 R25J270/90

US: 62/611 62/611P 62/618 62/618S

**Family:**

Publication number	Publication date	Application number	Application date
AU2008283102 AA	20090205	AU20080283102	20080620
AU2008283102 BB	20130207	AU20080283102	20080620
BRPI0813297 A2	20141230	BR2008PI13297	20080620
CA2692213 AA	20090205	CA20082692213	20080620
CN101711335 A	20100519	CN200880021514	20080620
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IN08508DN2009 A	20100716	IN2009DN08508	20091224
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MY163902 A	20171115	MY20090005466	20080620
NO20073245 A	20081223	NO20070003245	20070622
NO20073245 L	20081223	NO20070003245	20070622
NO329177 B1	20100906	NO20070003245	20070622
US2010132405 AA	20100603	US20080665329	20080620
WO09017414 A1	20090205	WO2008NO00229	20080620

Priority:

NO20070003245 20070622 WO2008NO00229 20080620

Probable Assignee: ARAGON AS

Assignee(s): (std): KANFA ARAGON AS ; LUND NILSEN INGE SVERRE

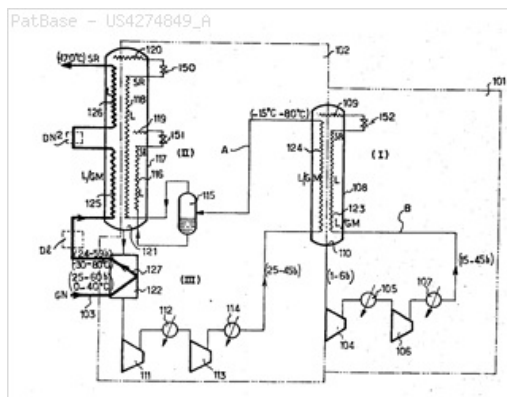
Assignee(s): ARAGON AS

Inventor(s): (std): LUND NILSEN INGE SVERRE ; NILSEN INGE SVERRE LUND ; SVERRE LUND NILSEN INGE ; NILSEN LUND

Inventor(s): LUND NILSEN ; INGE SVERRE LUND NILSEN

Agent(s): WRAYS; ONSAGERS LTD; CHRISTIAN D ABEL; ACAPO AS

Designated states: AE AG AL AM AO AT AU AZ BA BB BE BF BG BH BJ BR BW BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DO DZ EC EE EG ES FI FR GA GB GD GE GH GM GN GQ GR GT GW HN HR HU ID IE IL IN IS IT JP KE KG KM KN KP KR KZ LA LC LI LR LS LT LU LV LY MA MC MD ME MG MK ML MN MR MT MW MX MY MZ NA NE NG NI NL NO NZ OM PG PH PL PT RO RS RU SC SD SE SG SI SK SL SM SN SV SY SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN ZA ZM ZW

Title: CONDUCTOR COMPOSITIONS**Abstract:** Conductor compositions of finely divided Ni₃B_{1-x}P_x wherein x is the approximate range 0.05-0.6, dispersed in a vehicle, useful for producing sintered conductor patterns on a substrate. Glass powder may optionally be present. Also the resultant fired conductors.**Classifications:****International (ipc 8-9):** C04B41/50 C04B41/51 C04B41/87 C04B41/88 C09D5/24 F25J1/00 F25J1/02 H01B1/06 H01B1/14 H01B1/16 H01J17/49 H05K1/09 (Advanced/Invention); F25J1/00 (Advanced/Non-invention); C04B41/45 C04B41/87 C04B41/88 C09D5/24 F25J1/00 H01B1/06 H01B1/14 H01J17/49 H05K1/09 (Core/Invention)**International (ipc 1-7):** B22F7/00 C09D5/24 F25J1/00 F25J1/02 H01B1/00 H01B1/02 H01B1/06 H01B1/14 H01J17/49 H01B5/16**CPC:** Y10S428/901 C04B41/88 C04B41/009 C04B41/5025 C04B41/5053 C04B41/5144 C04B41/87 C04B2111/00844 C04B2111/94 H01B1/06 H01B1/14 H01J17/492 H05K1/092 F25J1/0262 F25J1/0265 F25J1/0022 F25J1/0055 F25J1/0212 F25J1/0264 F25J1/0268 F25J1/0292 F25J2220/64 F25J2210/06**European:** C04B41/00V C04B41/50P C04B41/50R C04B41/51P C04B41/87 C04B41/88 F25J1/00A6 F25J1/00C4V2 F25J1/02D F25J1/02D2 F25J1/02Z4H4 F25J1/02Z4H4R F25J1/02Z4H4R4 F25J1/02Z6L H01B1/06 H01B1/14 H01J17/49D H05K1/09D M04B111/00T56 M04B111/94 R25J220/64**US:** 106/1.27 252/513 428/427 428/433 428/901 62/335 62/612 62/9

Title: METHOD FOR LIQUEFYING METHANE-RICH GAS

Abstract: A method for liquefying methane-rich gas in the form of a feed gas comprising the steps of cooling the gas and partially liquefying the gas by expansion within an expansion device. The pressure of the gas at the inlet of the expansion device is in the range from 40 bar to 100 bar and pressure of the gas at the outlet of the expansion device is in the range from 2 bar to 10 bar.

Classifications:

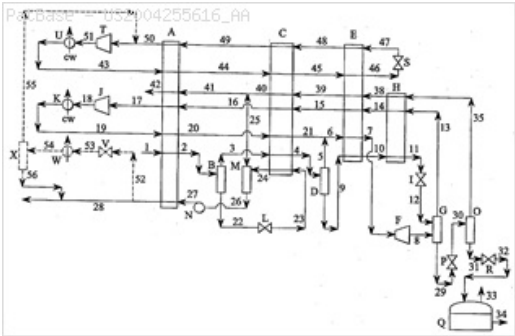
International (IPC 8-9): F25J1/00 F25J1/02 (Advanced/Invention); F25J1/00 (Core/Invention)

International (IPC 1-7): F25J1/00 F25J1/02

CPC: F25J1/0022 F25J1/0035 F25J1/0037 F25J1/004 F25J1/0042 F25J1/0045 F25J1/0052 F25J1/0219 F25J1/025 F25J1/0255 F25J1/0278 F25J2205/02 F25J2205/04 F25J2220/62 F25J2220/64 F25J2235/60 F25J2240/40 F25J2245/02

European: F25J1/00A6 F25J1/00C2E F25J1/00C2E2 F25J1/00C2F F25J1/00C2L F25J1/00C2V F25J1/00C4V F25J1/02D10 F25J1/02Z2M8P F25J1/02Z2T8 F25J1/02Z4U4F R25J205/02 R25J205/04 R25J220/62 R25J220/64 R25J235/60 R25J240/40 R25J245/02

US: 62/611 62/611P 62/612 62/612S 62/613



Family:

Publication number	Publication date	Application number	Application date
GB200120272 A0	20011010	GB20010020272	20010821
GB200402650 A0	20040310	GB20040002650	20020820
GB2393504 A1	20040331	GB20040002650	20020820
GB2393504 B2	20050518	GB20040002650	20020820
US2004255616 AA	20041223	US20040487501	20040809
US7234321 BB	20070626	US20020487501	20020820
WO03019095 A1	20030306	WO2002GB03844	20020820

Priority:

GB20010020272 20010821 WO2002GB03844 20020820

Probable Assignee: GASCONSULT LTD

Assignee(s): (std): GASCONSULT LTD ; MAUNDER ANTHONY DWIGHT ; SKINNER GEOFFREY FREDERICK

Assignee(s): SKINNER GEFFREY F ; MAUNDER ANTHONY D ; GASCONSULT LIMITED

Inventor(s): (std): MAUNDER ANTHONY DWIGHT ; SKINNER GEOFFREY F ; SKINNER GEOFFREY FREDERICK ; SKINNER GEFFREY F ; MAUNDER ANTHONY D

Inventor(s): ANTHONY DWIGHT MAUNDER ; GEOFFREY FREDERICK SKINNER

Agent(s): MARSHALL GERSTEIN AND BORUN LLP

Designated states: AE AG AL AM AT AU AZ BA BB BE BF BG BJ BR BY BZ CA CF CG CH CI CM CN CO CR CU CY CZ DE DK DM DZ EC EE ES FI FR GA GB GD GE GH GM GN GQ GR GW HR HU ID IE IL IN IS IT JP KE KG KP KR KZ LC LK LR LS LT LU LV MA MC MD MG MK ML MN MR MW MX MZ NE NL NO NZ OM PH PL PT RO RU SD SE SG SI SK SL SN SZ TD TG TJ TM TN TR TT TZ UA UG US UZ VC VN YU ZA ZM ZW

Title: PROCESS FOR LIQUEFYING NATURAL GAS CONTAINING NITROGEN

Abstract: 1,181,049. Natural gas liquefaction process. MESSER GRIESHEIM G.m.b.H. 5 Dec., 1968 [20 Dec., 1967]. No. 57848/68. Heading F4P. Cooling, followed by liquefaction and subcooling of compressed natural hydrocarbon gas in feed line 101 is effected in heat-exchangers 102, 103, respectively, and the sub-cooled liquid is then further cooled at 104 and expanded at a valve 107 into a separator 105; exchanger 102 being cooled by passage therethrough of a first multicomponent refrigerant, e.g. a mixture of C 1 to C 4 saturated hydrocarbons in a closed cycle, exchanger 103 being cooled by a second multicomponent refrigerant, e.g. a mixture of nitrogen, methane and ethane also in a closed cycle and in cascade arrangement with the first refrigeration cycle and the refrigerant of each cycle undergoes only one compression stage and is expanded to above atmospheric pressure. Exchanger 104 is cooled by flash gas from separator 105 which gas also cools exchangers 102, 103. In operation, the first refrigerant is compressed at 109 to about 40 atmosphere liquefied in a water-cooled exchanger 110, further cooled in exchanger 102 in countercurrent heat exchange with itself after expansion at 112 to about 3 atmosphere, and the refrigerant after leaving the warm end of exchanger 102 is returned to the compressor inlet. The second refrigerant is compressed at 114, cooled by water at 115, liquefied in exchanger 102, further cooled in exchanger 103, expanded at a valve 117 and returned through exchangers 103, 102 to the inlet of compressor 114.

Classifications:

International (IPC 8-9): F25J1/00 F25J1/02

F25J3/02 (Advanced/Invention);

F25J1/00 F25J3/02 (Core/Invention)

International (IPC 1-7): F25J1/00 F25J1/02 F25J3/02 F25J3/06

CPC: Y10S62/927 F25J1/0218 F25J1/0022 F25J1/004 F25J1/0045

F25J1/0052 F25J1/0072 F25J1/0214 F25J1/0219 F25J3/0209

F25J3/0233 F25J3/0257 F25J2200/02 F25J2200/50 F25J2200/74

F25J2200/94 F25J2270/12 F25J2270/42 F25J2270/60 F25J2290/34

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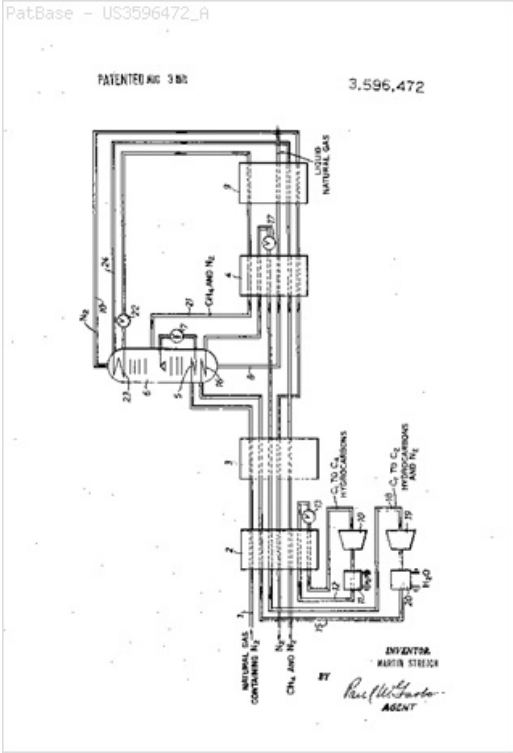
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R25J200/74 R25J200/94 R25J270/12 R25J270/42 R25J270/60

R25J290/34

US: 62/28 62/623 62/927



Family:

Publication number	Publication date	Application number	Application date
DE1551611 A1	19700416	DE19671551611	19671220
DE1551611 B2	19750821	DE19671551611	19671220
DE1551611 C3	19760401	DE1967M076657	19671220
FR1596088 A	19700615		19681213
GB1181049 A	19700211	GB19680057848	19681205
GB1208196 A	19701007	GB19680057849	19681205
NL160078 B	19790417	NL19680018394	19681220
NL160078 C	19790917	NL19680018394	19681220
NL6818394 A	19690624	NL19680018394	19681220
SU476766 D	19750705	SU19681290780	19681218
US3596472 A	19710803	US19680784124	19681216

Priority:

DE19671551611 19671220 DE19671551611 19671220 DE1967M076657 19671220

Probable Assignee: MESSER GRIESHEIM GMBH

Assignee(s): (std): LINDE AG ; MESSER GRIESHEIM GMBH

Assignee(s): LINDE 6200 WIESBADEN AG ; LINDE AG 6200 WIESBADEN ; LINDE AKTIENGESSELLSCHAFT WIESBADEN BONDSREPUBLIC ; LINDE AKTIENGESSELLSCHAFT WIESBADEN BONDSREPUBLIC DUTSLAND ; LINDE WIESBADEN BONDSREPUBLIC DUTSLAND AG ; MESSER GRIESHEIM G M B H

Inventor(s): (std): MARTIN STREICH DIPL PHYS ; STREICH MARTIN ; STREICH MARTIN DIPL PHYS

Inventor(s): MARTIN STREICH