



New connection on: : 04-07-2018 : 05:47:10 - Last disconnection on: : 03-07-2018 : 01:39:03

V 4.0.0.44358(LP,U,linux) (Rev:43856 2017-04-27 09:03:29 +0200#(D201802)) (RPM D201802)

Welcome to EPOQUE Rebuild under the Production Environment

[No database/cluster active] ..fi epodoc

 Database: EPODOC

[EPODOC: SS 1] ((fatty 2d alcohol+) and hydrogen+ and ((fatty 2d acid) 2d ester))

Results in EPODOC 214

[SS 2] * and PD<2014-09-12

Results in EPODOC 172

[SS 3] ..v

[EPODOC: SS 3] 2 and ion 3d exchanger

Different expressions or operators have been used without brackets. *ERROR(-50002)*

[SS 3] 2 and (ion 3d exchanger)

Results in EPODOC 0

[SS 4] ..li 1-10

The command has been applied on a Search Statement with a zero result. *WARNING(-50856)*

[SS 4] 2

Results in EPODOC 172

[SS 5] ..li 1-10



PN - [CA2880562](#) A1 20140417

PR - GB20120018078 20121009; WO2013GB52584 20131003

AP - CA20132880562 20131003

DT - I

CCI - [C07C67/03](#) ; [C07C67/08](#)

CUI - [C07C29/17](#) ; [C07C29/128](#)

CLC - [C07C67/03](#) , [C07C69/26](#) , INV
- [C07C67/08](#) , [C07C69/24](#) , INV
- [C07C29/149](#) , [C07C31/125](#) , INV

CCA - [C07C29/149](#)

CUA - [C07C29/80](#) ; [C07C31/125](#)

PA - JOHNSON MATTHEY DAVY TECHNOLOGIES LTD [GB]

TI - PROCESS FOR THE PRODUCTION OF A **FATTY ALCOHOL** FROM A **FATTY ACID**

AB - A process for the production of **fatty alcohol** or **alcohols** comprising: subjecting a fatty acid or fatty acid mixture to esterification with a lower alkanol in an esterification reactor maintained under esterification conditions to form a stream comprising the corresponding lower alkyl **fatty acid ester** or esters; vaporising the stream from step (a); subjecting the vaporised stream of step (b) to **hydrogenation** in a first **hydrogenation** zone operated under **hydrogenation** conditions to form a stream comprising **fatty alcohol** or **alcohols** and an amount of unconverted lower alkyl **fatty acid ester** or esters; subjecting the stream from step (c) to transesterification in a wax ester reactor maintained under transesterification conditions in the presence of a transesterification catalyst thereby to convert at least a portion of the lower alkyl **fatty acid ester** or esters by ester interchange with a corresponding amount of **fatty alcohol** or **alcohols** to lower alkanol and to a wax ester or esters; separating the stream from step (d) by distillation to yield a **fatty alcohol** or **alcohols** product stream; a wax ester or esters stream; and an overhead stream comprising fatty alkanol or alkanols and alkane, and optionally one or both of water and lower alkanol; reacting said overhead stream from step (e) in a wax ester reactor maintained under transesterification conditions in the presence of a transesterification catalyst with a lower alkyl **fatty acid ester** or esters thereby to convert at least a portion of the lower alkyl **fatty acid ester** by **ester** interchange with a corresponding amount of **fatty alcohol** or **alcohols** to lower alkanol and to a wax ester or esters; and separating the wax ester or esters formed from the alkane, and any water and/or lower alkanol present.

2/172 © EPODOC / EPO

PN - [KR20140108381](#) A 20140911

PR - KR20130020035 20130225

AP - KR20130020035 20130225

DT - I

PA - GNO CO LTD [KR]

TI - METHOD FOR MANUFACTURING HIGH-PURITY VEGETABLE **FATTY ALCOHOL**

AB - The present invention relates to a method for manufacturing a high-purity isostearyl alcohol from isostearic acid, the method comprising the steps of: (A) making **fatty acid**

methyl **ester** from the compound of fatty acid compounds with carbon 16 or 18; (B) separating the **fatty acid methyl ester** compound obtained from step (A) by cooling the same between 0-30°C into isostearic acid methyl ester; and (C) manufacturing isostearic acid alcohol via **hydrogenation** process from the separated isostearic methyl ester in step (B).

3/172 © EPODOC / EPO

PN - [TW201425286](#) A 20140701
 PR - GB20120018078 20121009
 AP - TW20130136383 20131008
 DT - I
 CCI - [C07C67/03](#) ; [C07C67/08](#)
 CUI - [C07C29/17](#) ; [C07C29/128](#)
 CLC - [C07C67/03](#) , [C07C69/26](#) , INV
 - [C07C67/08](#) , [C07C69/24](#) , INV
 - [C07C29/149](#) , [C07C31/125](#) , INV
 CCA - [C07C29/149](#)
 CUA - [C07C29/80](#) ; [C07C31/125](#)
 PA - JOHNSON MATTHEY DAVY TECHNOLOGIES LTD [GB]
 TI - Process for production of **fatty alcohol**
 AB - A process for the production of **fatty alcohol** or **alcohols** comprising: subjecting a fatty acid or fatty acid mixture to esterification with a lower alkanol in an esterification reactor maintained under esterification conditions to form a stream comprising the corresponding lower alkyl **fatty acid ester** or esters; vaporising the stream from step (a); subjecting the vaporised stream of step (b) to **hydrogenation** in a first **hydrogenation** zone operated under **hydrogenation** conditions to form a stream comprising **fatty alcohol** or **alcohols** and an amount of unconverted lower alkyl **fatty acid ester** or esters; subjecting the stream from step (c) to transesterification in a wax ester reactor maintained under transesterification conditions in the presence of a transesterification catalyst thereby to convert at least a portion of the lower alkyl **fatty acid ester** or esters by ester interchange with a corresponding amount of **fatty alcohol** or **alcohols** to lower alkanol and to a wax ester or esters; separating the stream from step (d) by distillation to yield a **fatty alcohol** or **alcohols** product stream; a wax ester or esters stream; and an overhead stream comprising fatty alkanol or alkanols and alkane, and optionally one or both of water and lower alkanol; reacting said overhead stream from step (e) in a wax ester reactor maintained under transesterification conditions in the presence of a transesterification catalyst with a lower alkyl **fatty acid ester** or esters thereby to convert at least a portion of the lower alkyl **fatty acid ester** by **ester** interchange with a corresponding amount of **fatty alcohol** or **alcohols** to lower alkanol and to a wax ester or esters; and separating the wax ester or esters formed from the alkane, and any water and/or lower alkanol present.

4/172 © EPODOC / EPO

PN - [JP2014129292](#) A 20140710
 PNFP - JP6147002B B2 20170614



PR	- JP20120288446 20121228
AP	- JP20120288446 20121228
DT	- I
CT	- STSE (A) JP2010184885 A 20100826 [] (KAO CORP); JPH11343211 A 19991214 [] (SHISEIDO CO LTD); JP2006225347 A 20060831 [] (SHISEIDO CO LTD); JP2006169130 A 20060629 [] (SHISEIDO CO LTD); JP2007314655 A 20071206 [] (SHISEIDO CO LTD); JP2008050271 A 20080306 [] (SHISEIDO CO LTD); JPS63183511 A 19880728 [] (SHISEIDO CO LTD, et al); JP2008050273 A 20080306 [] (SHISEIDO CO LTD)
FI	- A61K8/06; A61K8/37; A61K8/81; A61K8/89; A61K8/891; A61Q1/00; A61Q1/02
FT	- 4C083/AA072; 4C083/AA112; 4C083/AB232; 4C083/AB242; 4C083/AB332; 4C083/AB352; 4C083/AB432; 4C083/AC022; 4C083/AC132; 4C083/AC172; 4C083/AC342; 4C083/AC422; 4C083/AC442; 4C083/AC482; 4C083/AD021; 4C083/AD022; 4C083/AD042; 4C083/AD092; 4C083/AD152; 4C083/AD332; 4C083/AD432; 4C083/AD452; 4C083/AD572; 4C083/CC12; 4C083/DD32; 4C083/EE06
PA	- (A) KAO CORP
TI	- (A) POWDER-CONTAINING WATER-IN- OIL TYPE EMULSION COSMETIC
AB	- (A) PROBLEM TO BE SOLVED: To provide a powder-containing water-in-oil type emulsion cosmetic which provides a light touch feeling, excels in cosmetic

durability and can obtain high storage stability. SOLUTION: There is provided a powder-containing water-in-oil type emulsion cosmetic which comprises: (A) a polyhydric **alcohol-fatty acid ester** type surfactant which has an HLB value of 6 or less and is liquid at 25°C; (B) 5 to 20 mass% of a **hydrogenated** polyisobutene based on the total amount of the powder-containing water-in-oil type emulsion cosmetic; and (C) a silicone-based film-forming agent.

5/172 © EPODOC / EPO

PN - [CN103980090](#) A 20140813

PNFP - CN103980090B B 20160316

PR - CN20141228689 20140528

AP - CN20141228689 20140528

DT - I

CT - || STSE (A)
[CN1223169](#) A 19990721 [A] (AMMONIA CASALE SA [CH])
 [A]
[JPH11322648](#) A 19991124 [A] (DHW DEUTSCHE HYDRIERWERKE GMBH)
 [A]
[CN101633602](#) A 20100127 [A] (SHANGHAI ZHONGYUAN CHEMICAL CO)
 [A]
[US5043485](#) A 19910827 [A] (FLECKENSTEIN THEO [DE], et al)
 [A]

CTNP - || STSE (A)
 [] 石荣荣,
 "加氢制脂肪醇工艺中消除热点的措施", <<科技信息>>, (20090405), no. 10

CNOI - (A)
[C07C29/149](#)

CNOL - C07C29/149, C07C31/125, INV
 - C07C29/149, C07C33/02, INV

PA - (A)
 DENGTA BEIFANG CHEMICAL CO LTD

TI - (A)
 Production method of natural **fatty alcohol**

AB - (A)
 The invention relates to a production method of natural **fatty alcohol**. The production method comprises the following steps: purifying fatty glyceride; fractionally distilling

the generated **fatty acid methyl ester** according to length of carbon chains and then sequentially feeding into two reactors I and II connected in series; introducing a **hydrogenation** product into an evaporator to remove methanol; and finally, decompressing and rectifying to obtain a final product. The technical keypoint is as follows: the feed **hydrogen** and oil ratio of the reactor is 5800-6500, the reaction pressure is 24.5-25.5MPa, the feed preheating temperature is 200-202 DEG C, the empty tower gas velocity of the reactor I is 0.055-0.061m/s, the upper temperature of the reactor I is 203-205 DEG C, the middle temperature is 215-220 DEG C, and the lower temperature is 216-225 DEG C; the reaction pressure of the reactor II is 24.5-25.5MPa, the empty tower gas velocity is 0.079-0.092m/s, the upper temperature of the reactor II is 24.5-25.5MP, the middle temperature is 208-215 DEG C and the lower temperature is 210-220 DEG C; the height-diameter ratio of the reactor I is 12-13 and that of the reactor II is 14-15, and the effective volume ratio of the reactors I and II is 1.3-1.5. The invention solves the problems of low output and yield, high production cost, low quality gas velocity of existing production process and the like and has the advantages of low toxicity, high yield and the like.

6/172 © EPODOC / EPO

PN - [US2014219928](#) A1 20140807

PNFP - US9724324 B2 20170808

PR - US201214233198 20120719; US201161509888P 20110720; WO20121L00281 20120719

AP - US201214233198 20120719

DT - **

CT - || R141 (A1)
[US8343945](#) B2 20130101 [] (TAMARKIN DOV [IL], et al)
 - || STSE (B2)
[US8343945](#) B2 20130101 [] (TAMARKIN DOV [IL], et al)

CCI - [A61K9/0014](#) ; [A61K47/14](#) ; [A61K9/122](#) ; [A61K47/44](#)

CUI - [A61K31/351](#) ; [A61K31/59](#)

PA - (A1)
 ARNON MICHAL N [IL]; KAMENETSKY TATIANA [IL]
 - (B2)
 ARNON MICHAL N [IL]; KAMENETSKY TATIANA [IL]; PERRIGO ISRAEL PHARMACEUTICALS LTD [IL]

TI - (A1)
 TOPICAL OILY FOAM COMPOSITIONS
 - (B2)
 Topical oily foam compositions

AB - (A1)
 Topical alcohol-free thermo labile oily foam composition comprising (i) at least one active pharmaceutical ingredient or ectoparasitic active ingredient; (ii) at least about 20% w/w of at least one lipophilic component; (iii) at least about 10% w/w of at least one non-ionic surfactant; (iv) at least about 0.5% w/w of at least one **fatty alcohol** or **fatty acid** or **ester** thereof with melting point above 30° C., and; (v) at least about 7% w/w of propellant selected from propane, butane, isobutene and combinations thereof; said composition optionally comprising at least about 5% to about 70% w/w of a

hydrophilic component, optionally comprising up to about 5% w/w **hydrogenated** oil and optionally comprising a penetration enhancer

7/172 © EPODOC / EPO

PN - [CN103965016](#) A 20140806

PNFP - CN103965016B B 20160413

PR - CN20141209632 20140512

AP - CN20141209632 20140512

DT - I

CT - || STSE (A)
[CN102365254](#) A 20120229 [A] (SUMITOMO CHEMICAL CO)
 [A]
[CN103665369](#) A 20140326 [Y] (LANZHOU CHEM PHYS INST)
 [Y]

CTNP - || STSE (A)
 [Y] Wenwen Zhu et al, "Amphiphilic ionic liquid stabilizing palladium nanoparticles for highly efficient catalytic hydrogenation", <<Phys. Chem. Chem. Phys.>>, (20110513), vol. 13, PAGE 13492 - 13500
 [Y]
 13492-13500
 [Y] 姜蕊等,
 "温控钯-膦配合物催化油酸甲酯加氢反应的研究", <<精细化工>>, (20090430), vol. 26, no. 4, PAGE 360 - 363
 [Y]
 360-363

CNOI - (A)
[B01J23/44](#) ; [B01J31/0285](#) ; [B01J31/068](#) ; [B01J35/006](#) ; [C07C29/149](#)

PA - (A)
 UNIV QINGDAO SCIENCE & TECH

TI - (A)
 Method for preparing **fatty alcohol** through **hydrogenation** of **fatty acid methyl ester** in presence of temperature control catalytic system

AB - (A)
 The invention provides a method for preparing **fatty alcohol** through **hydrogenation** of **fatty acid methyl ester** in presence of a temperature control catalytic system. The method is characterized by adopting Pd metal nanoparticles stabilized by imidazolyl temperature control ionic liquid containing different length of polyoxyethylene ether chain segments as catalysts to catalyze **hydrogenation** of **fatty acid methyl ester** to prepare **fatty alcohol** under the conditions of 10.0g of **fatty acid methyl ester**, 0.4-1.2g of temperature control ionic liquid catalytic system (containing 0.2-10% of Pd metal nanoparticles by mass), **hydrogen** pressure of 4-8MPa, reaction temperature of 190-230 DEG C and reaction time of 2-6 hours and carrying out separation, recovery and cyclic utilization on the temperature control ionic liquid catalytic system containing the Pd metal nanoparticles. Compared with the prior art, the method has the characteristics that 1. the catalytic system can achieve high temperature homogeneous

8/172 © EPODOC / EPO

PR - CN20132717320U 20131107

AP - CN20132717320U 20131107

DT - 1

PA - DENGTA BEIFANG CHEMICAL CO LTD

TI - Grease **hydrogenation** device

9/172 © EPODOC / EPO

PN - **EA201300537** A1 20140430

PNFP - EA024091 B1 20160831

PR - GB20110019871
20111117; WO2012GB52726
20121101

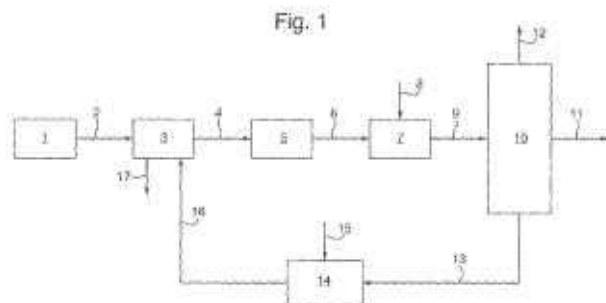
AP - EA20130000537 20121101

DT - 1

CT - || STSE (B1)
[DE102007033636](#) A1 20090122 [
] (COGNIS IP MAN GMBH [DE])

CCI - [C07C29/149](#) ; [C07C67/03](#) ;
[C07C67/08](#)

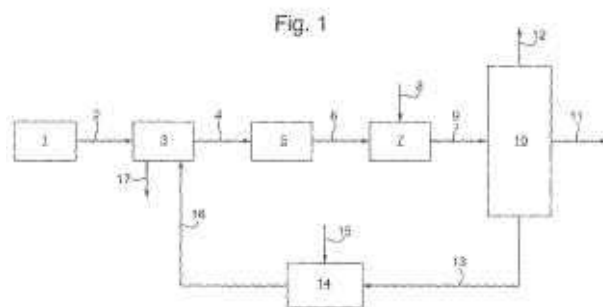
CUI - [C07C31/125](#) ; [C07C29/128](#) ;
[C07C29/1285](#)



CLC	- C07C67/03, C07C69/26 , INV - C07C67/08, C07C69/24 , INV - C07C29/149, C07C31/125 , INV
PA	- (B1) JOHNSON MATTHEY DAVY TECHNOLOGIES LTD [GB]
TI	- (B1) PROCESS FOR PRODUCING FATTY ALCOHOLS
AB	- (B1) A process for the production of fatty alcohol or alcohols comprising: (a) subjecting a fatty acid or fatty acid mixture to esterification with a lower alkanol in an esterification reactor maintained under esterification conditions to form a stream comprising the corresponding lower alkyl ester or esters; (b) vaporising the stream from step (a); (c) subjecting the vaporised stream of step (b) to hydrogenation in a first hydrogenation zone operated under hydrogenation conditions to form a stream comprising fatty alcohol or alcohols and an amount of unconverted lower alkyl ester or esters; (d) subjecting the stream from step (c) to transesterification in a wax ester reactor maintained under transesterification conditions in the presence of a solid transesterification catalyst thereby to convert at least a portion of the lower alkyl fatty acid ester by ester interchange with a corresponding amount of fatty alcohol or alcohols to lower alkanol and to a wax ester or esters derived from a fatty alcohol and a fatty acid; (e) separating fatty alcohol or fatty alcohols and wax ester or wax esters of step (d) by distillation

to yield a **fatty alcohol** or **alcohols** product and a stream comprising wax ester or esters;
 (f) passing said stream comprising wax ester or esters to a second **hydrogenation** zone operating under conditions to effect **hydrogenation** in the liquid phase to revert the wax ester or esters to **fatty alcohol** or **alcohols**; and (g) returning the **fatty alcohol** or **alcohols** to the separation step (e).

10/172 © EPODOC / EPO
 PN - [GB2507687](#) A 20140507
 PR - WO2012GB52726
 20121101; GB20110019871
 20111117
 AP - GB20140002408 20121101
 DT - **
 CT - || STSE (A)
[DE102007033636](#) A1 20090122 [
] (COGNIS IP MAN GMBH [DE])
 CCI - [C07C29/149](#) ; [C07C67/03](#) ;
[C07C67/08](#)
 CUI - [C07C31/125](#) ; [C07C29/128](#) ;
[C07C29/1285](#)
 CNOI - [C07C29/149](#) ; [C07C67/03](#) ;
[C07C67/08](#) ; [C07C31/125](#) ;
[C11C3/00](#) ; [C11C3/003](#) ;
[C11C3/10](#) ; [C11C3/12](#)
 CLC - [C07C67/03](#) , [C07C69/26](#) , INV
- [C07C67/08](#) , [C07C69/24](#) , INV
- [C07C29/149](#) , [C07C31/125](#) , INV
 PA - JOHNSON MATTHEY DAVY
 TECHNOLOGIES LTD [GB]
 TI - Process for producing **fatty**
alcohols from **fatty** acids
 AB - A process for the production
 of **fatty alcohol** or **alcohols**
 comprising: subjecting a fatty
 acid or fatty acid mixture to
 esterification with a lower
 alkanol in an esterification
 reactor maintained under



esterification conditions to form a stream comprising the corresponding lower alkyl ester or esters; vaporising the stream from step (a); subjecting the vaporised stream of step (b) to **hydrogenation** in a first **hydrogenation** zone operated under **hydrogenation** conditions to form a stream comprising **fatty alcohol** or **alcohols** and an amount of unconverted lower alkyl ester or esters; subjecting the stream from step (c) to transesterification in a wax ester reactor maintained under transesterification conditions in the presence of a solid transesterification catalyst thereby to convert at least a portion of the lower alkyl **fatty acid ester** by **ester** interchange with a corresponding amount of **fatty alcohol** or **alcohols** to lower alkanol and to a wax ester or esters derived from a **fatty alcohol** and a **fatty acid**; separating **fatty alcohol** or **fatty alcohols** and wax ester or wax esters of step (d) by distillation to yield a **fatty alcohol** or **alcohols** product and a stream comprising wax ester or esters; passing said stream comprising wax ester or esters to a second **hydrogenation** zone operating under conditions to effect **hydrogenation** in the liquid phase to revert the wax ester or esters to **fatty alcohol** or **alcohols**; and returning the **fatty alcohol** or **alcohols** to the separation step (e).