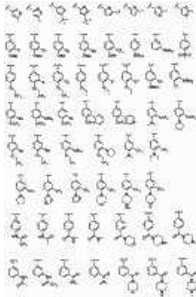
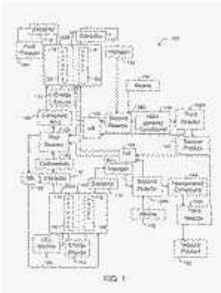
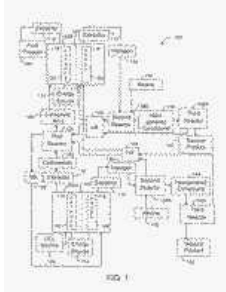
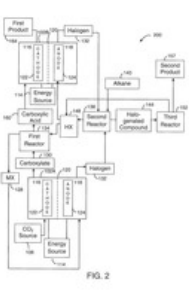
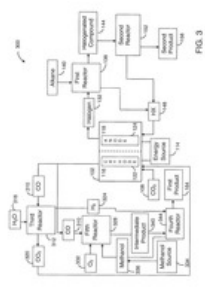
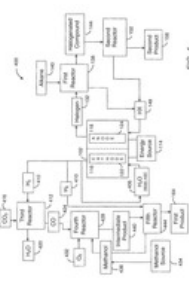


13 results for 70 AND (COOL+ OR REFRIGERAT+) - Collection: FAMPAT

#		Title	Publication number	1st app. date	Applicant/Assignee	1st publ. date	Publ. date	
1.		Process for the preparation of diol mixtures	WO200134543	2000-11-02	ASAHI CHEMICAL INDUSTRY* ASAHI KASEI ASAHI KASEI CHEMICALS	2001-05-17	2001-05-17	
Disclosed is a method for producing a diol mixture comprising 1,4-butanediol, 1,5-pentanediol and 1,6-hexanediol, which comprises: (A) providing a dicarboxylic acid mixture comprising succinic acid, glutaric acid and adipic acid and having a nitric acid content of 3 % by weight or less, based on the total weight of the succinic, glutaric and adipic acids, wherein the dicarboxylic acid mixture is prepared by denitrating an aqueous by-product solution obtained in an adipic acid production process, and (B) subjecting the dicarboxylic acid mixture to hydrogenation in the presence of water, hydrogen gas and a hydrogenation catalyst containing an active metal species comprising ruthenium and tin, to thereby obtain a hydrogenation reaction mixture comprising a diol mixture comprising 1,4-butanediol, 1,5-pentanediol and 1,6-hexanediol.								
2.		Method for producing alcohols	FR2874377	2004-08-20	COGNIS*	2006-02-24	2006-02-24	
The invention relates to a method for producing alcohols by hydrating a mixture which comprises (a) 0.1 to 99.3 % by weight of one or more alkyl esters of carboxylic acids, (b) 0 or 0.1 to 95 % by weight of one or more carboxylic acids, (c) 0 or 0.1 to 90 % by weight of one or more C<SUB>1-3</SUB>alkanols and (d) 0.5 to 25 % by weight of water, the weight percentages of components (a) to (d) relating to the respective sum of components (a) to (d), in the presence of a heterogeneous catalyst which is present in the form of pellets, with the proviso that the sum of components (a) to (d) adds up to 100 % by weight, and the amount of water (d), based on the amount of carboxylic acid ester (a), is at least 0.5 % by weight, and the additional proviso that, if both components (b) and (c) are present in an amount of 0 % by weight each, the amount of water (d) is at least 2.1 % by weight and the lower and upper limits of the amount of carboxylic acid esters (a) are identical and are only determined by the condition that the sum of components (a) to (d) adds up to 100 % by weight. The inventive method is characterized in that alcohols can be obtained by hydration in good yields and with considerably less byproducts produced, especially substantially less hydrocarbons, isooalcohols, secondary alcohols and ethers.								
3.		Electrochemical reduction of co2 with co-oxidation of an alcohol	US20130105330	2012-12-21	ARES CAPITAL AVANTIUM KNOWLEDGE CENTRE* AVATAR KNOWLEDGE CENTER LIQUID LIGHT LIQUID LIGHT LIQUID LIGHT	2013-05-02	2013-05-02	
The present disclosure is a system and method for producing a first product from a first region of an electrochemical cell having a cathode and a second product from a second region of the electrochemical cell having an anode. The method may include the step of contacting the first region of the electrochemical cell with a catholyte comprising an alcohol and carbon dioxide. Another step of the method may include contacting the second region of the electrochemical cell with an anolyte comprising the alcohol. Further, the method may include a step of applying an electrical potential between the anode and the cathode sufficient to produce a first product recoverable from the first region and a second product recoverable from the second region.								
								
								
								
								
								

4.

Water gas shift catalyst and fuel cell system including the same

KR100728124

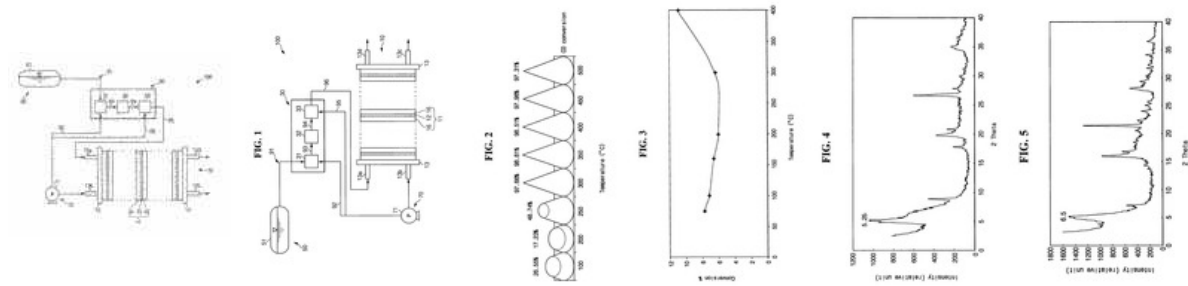
2006-02-10

SAMSUNG SDI*

2007-06-07

2007-06-07

A water gas shift catalyst for a reformer of a fuel cell system where a supporter includes a clay and ZnO; and an active material including CuO supported on the supporter. In a preferred embodiment the ZnO is filled between layers of the clay.



5.

Catalyst for oxidizing carbon monoxide in a reformer, and fuel cell plant including said reformer

EP1818096

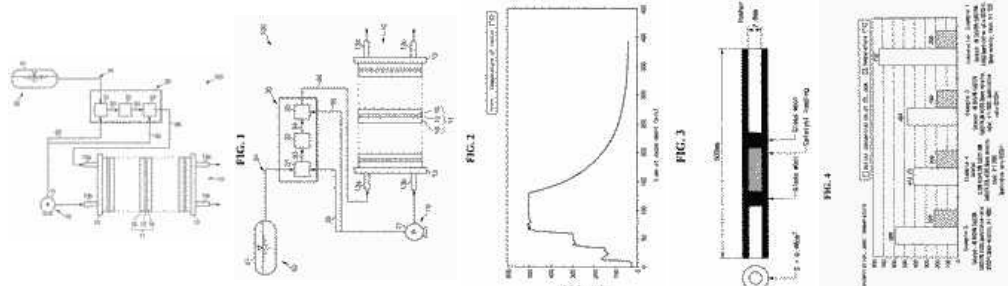
2006-02-14

SAMSUNG SDI*

2007-08-15

2007-08-15

In a fuel cell, a fuel cell system, and a method of preparing the same, a carbon monoxide oxidizing catalyst for a reformer of the fuel cell system includes: a carrier selected from the group consisting of alumina, cordierite, and combinations thereof; and an active material including CeO₂, MO, and CuO, where M is a transition element which is supported on the carrier. M can be selected from the group consisting of Ni, Co, Fe and combinations thereof.



6.

Method for producing 1,6-hexandiol

CN101265158

2007-03-12

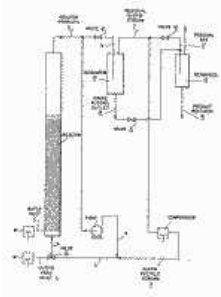
PETROCHINA*

2008-09-17

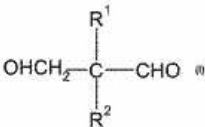
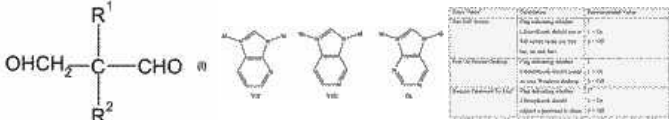
2008-09-17

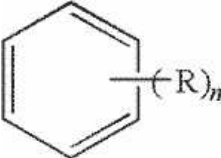
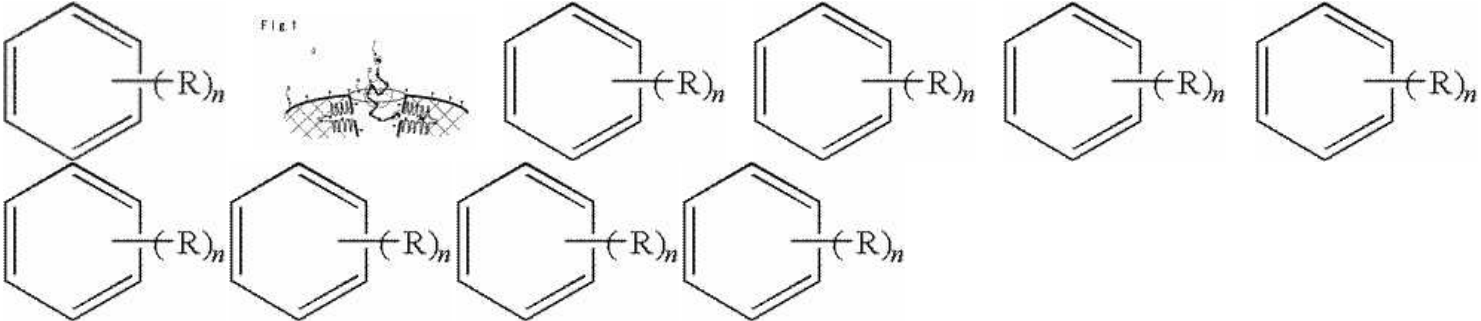
The invention relates to a method of producing 1, 6-hexanediol, which is that solid acid catalysts that are adipate and methanol are pre-esterified at atmospheric pressure; the supernatant fluid of reaction products after pre-esterifying is delivered to a continuous esterifying tower to act the continuous esterifying reaction with methanol vapor under the action of a catalyst, and the temperature for the continuous esterifying reaction ranges from 70 DEG C to 15 DEG C; based on the quality of the adipate, the addition amount of a solid catalyst ranges from 1 to 10 percent; the molar ratio of the methanol and the adipate is 1 to 10:1, and a solid acid catalyst is strong acidic ion exchange resin; reactants act the hydrogenation reaction after purification by rectification, wherein, the molar ratio of the hydrogen and ester is 50 to 350:1, the temperature ranges from 150 to 250 DEG C, the pressure ranges from 2.5 to 10.0MPa, and the catalysts are copper oxide ranging from 25 to 60 percent, zinc oxide ranging from 25 to 60 percent and alumina ranging from 10 to 30 percent; the obtained crude methanol is performed through the purification by rectification to gain the 1, 6-hexanediol the purity quotient of which is 99.0 percent, and the waste methanol can be recycled after the rectification.

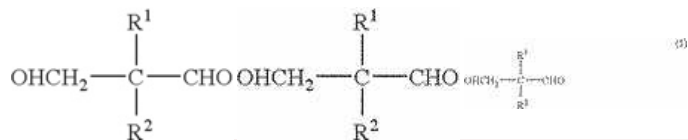


7.	Process for the production of lower alcohols by direct catalytic hydration of lower olefins	AR202990	1974-06-21	DEUTSCHE TEXACO 2000 HAMBURG RWE DEA FUR MINERALOEL & CHEMIE* TEXACO	1975-07-31	1975-07-31
A process for the production of C.sub.2 to C.sub.6 alcohols via the direct hydration of olefins in the presence of water, and acid or a strongly acidic solid with the separation of aqueous crude alcohols from the reaction product.						
						
8.	Hydroformylation process	WO9715543	1996-10-16	SHELL SHELL CANADA SHELL INTERNATIONALE RESEARCH*	1997-05-01	1997-05-01

Accordingly, a process is provided for the hydroformylation of ethylenically unsaturated compounds having at least 4 carbon atoms by reaction thereof with carbon monoxide and hydrogen in the presence of a solvent and a catalyst system obtainable by combining: a) a source of Group VIII metal cations; b) a source of anions; and c) a source of phosphine ligands, wherein the solvent is a C1 to C10 alkane or alkene having two or more cyano groups attached.

9.	Method for hydrogenation of methylolalkanal to give polyvalent alcohols with low acetal content	DE102006009839	2006-03-01	BASF*	2007-09-06	2007-09-06
The invention relates to a method for production of polyvalent alcohols with low acetal content by catalytic hydrogenation of methylolalkanal of general formula (I), where R<SUP>1</SUP> and R<SUP>2</SUP> independently = a further methylol or C<SUB>1</SUB>-C<SUB>22</SUB> alkyl group or C<SUB>6</SUB>-C<SUB>33</SUB> aryl or aralkyl group in the liquid phase on a hydrogenation catalyst, characterised in that at least one tertiary amine, inorganic base or inorganic or organic acid is added to the hydrogenation feed to adjust the pH value of the hydrogenation product to 7.0 to 9.0.						
						
						

10.	Gas adsorbent	WO2007018266	2006-08-10	MITSUBISHI CHEMICAL* MITSUBISHI RAYON	2007-02-15	2007-02-15
To provide a gas adsorbent which has sufficient gas adsorptivity for noxious gas components in a cigarette when brought into contact with a gas stream having a high flow rate as that when it passes through a cigarette filter, and which releases a small amount of bad odor components such as amine impurities and free noxious components which adversely affect health such as aromatic compounds derived from the gas adsorbent itself. A gas adsorbent which satisfies the following conditions (I), (II), (IV) and (V) or the following conditions (I), (III), (IV) and (V): (I) the mean pore radius of the gas adsorbent is at least 330 Å and at most 3,000 Å as measured by a mercury porosimeter; (II) the amine elution amount from the gas adsorbent per unit mass is at most 10 µeq/g; (III) the content of a monocyclic aromatic compound represented by the following formula 1 in the gas adsorbent per unit mass is at most 4 mg/g; wherein R is a substituent selected from the group consisting of a hydroxyl group, a C 1-3 alkyl group and a C 2-3 alkenyl group, and n is an integer of from 1 to 6 and represents the number of the substituent R, provided that when there are a plurality of R's, the respective R's may be the same or different; (IV) the neutral salt decomposition capacity is at most 0.43 meq/g; and (V) the acid adsorption capacity of the gas adsorbent per unit mass is at least 1.5 meq/g.						
						
						

$$\begin{array}{c} \text{R}^1 \\ | \\ \text{OHCH}_2 - \text{C} - \text{CHO} \\ | \\ \text{R}^2 \end{array}$$


2002-08-14	2002-08-14
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1995-01-25 1995-01-25

评价内容		评价方法	评价结果	评价依据	评价结论
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	环境现状评价	现状评价	现状评价	现状评价	现状评价
环境影响评价	环境影响评价	环境影响评价	环境影响评价	环境影响评价	环境影响评价
	环境影响评价	环境影响评价	环境影响评价	环境影响评价	环境影响评价

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